

1 **Title**

2 Evaluation of the suitability of different calorimetric methods to determine the enthalpy-
3 temperature curve of granular PCM composites

4 **Authors**

5 Javier Mazo*, Mónica Delgado, Conchita Peñalosa, Pablo Dolado, Inés Miranda, Ana
6 Lázaro, José María Marín, Belén Zalba

7 Aragón Institute for Engineering Research (I3A), Thermal Engineering and Energy
8 Systems Group, University of Zaragoza

9 Agustín Betancourt Building, C/María de Luna 3, 50018 Zaragoza, Spain

10 Phone: (+34) 876 555 584

11

12 * Corresponding Author, jmazo@unizar.es

13

14

15

16

17

18

19

20

21

22

23

24

25 **Abstract**

26 The present research has analysed the complementarity of different measuring methodologies when
27 characterizing the phase changing behaviour of a granular PCM composite (GPCC) through a
28 comparison of their results. Specifically, the enthalpy variation of the GR31 product manufactured
29 by Rubitherm has been measured by using: 1) An energy balance calculation of an air stream flowing
30 through a GPCC packed bed; 2) Differential Scanning Calorimetry; 3) the T-history method. The
31 main purpose of this study was to evaluate the suitability of these methods for the enthalpy-
32 temperature curve determination of GPCC. The energy balance setup gave an accurate measurement
33 of the enthalpy variation within a sufficiently high temperature interval. Obtaining a representative
34 sample was not a problem using this method, in contrast to the DSC which requires a greater number
35 of tests to obtain an average value representative of the packed bed. However, the energy balance
36 method does not enable the direct determination of the enthalpy-temperature curve. The T-history
37 methodology allows the enthalpy to be determined based on temperature while the representativeness
38 problem of the DSC is avoided due to the higher sample volume. Nevertheless, the sample must be
39 altered, crushed and subsequently compacted to reduce the effects of the thermal resistances provoked
40 by the void spaces being filled by air. This comparison has shown that there is no single valid
41 methodology for characterizing the phase changing behaviour of PCM granules.

42 **Keywords**

43 Thermal Energy Storage; PCM granules; Packed bed; DSC; T-history

44 **Nomenclature**

45 A Surface [m^2]

46 a_b Compactness of the packed bed [m^{-1}]

47	Bi	Biot number $Bi=h\cdot r/(2\cdot\lambda)$ [-]
48	c	Specific heat capacity [kJ/(kg·K)]
49	C	Constant
50	D	Diameter [m]
51	E	Energy [kJ]
52	e	Thickness [m]
53	f	Liquid mass fraction [-]
54	h	Heat transfer coefficient [W/(m ² ·K)], Specific enthalpy [kJ/kg]
55	H	Enthalpy [kJ]
56	L	Thermal losses [kJ]
57	L _b	Length of the packed bed [m]
58	\dot{m}	Mass flow [kg/s]
59	m	Mass [kg]
60	Nu	Nusselt number [-]
61	Ra	Rayleigh number [-]
62	T	Temperature [°C]
63	T _m	Phase change temperature [°C]
64	t	Time [s]
65	\dot{V}	Air volumetric flow rate [l/min]

66 x Position [m]

67 **Abbreviations**

68 EB Relative to the energy balance setup

69 DSC Differential Scanning Calorimeter

70 GPCC Granular PCM composites

71 PCM Phase Change Materials

72 **Subscripts**

73 ∞ Ambient conditions, final stationary situation

74 a Air

75 b Packed bed

76 c Relative to convection

77 c,b Convection in the packed bed

78 eq Equivalent

79 ext External

80 i Inlet

81 int Internal

82 l Liquid

83 o Outlet

84 p Relative to a particle of the packed bed

85 r-c Combined radiation and convection

86 s Solid

87 sur Surface

88 t Tube

89 **Greek symbols**

90 δ Deviation

91 Δ Increase

92 ϵ Emissivity [-]

93 μ Mean value

94 ρ Density [kg/m³]

95 σ Standard deviation

96 **1. Introduction**

97 Granular PCM composites (GPCC) are of considerable interest for thermal energy storage systems
98 due to the possibility of direct contact between the heat transfer fluid and the GPCC, which can also
99 lead to better heat transfer rates while taking advantage of small particle diameters. These composites
100 provide a flexible solution that can be used in several applications. On the one hand, they can be
101 integrated with air heat exchangers. Several configurations have been experimentally analyzed.
102 Packed bed air heat exchangers have been studied by Nagano et al. [1] and Rady [2,3] whereas
103 various fluidized bed configurations have been exhaustively tested by Izquierdo-Barrientos et al. [4]
104 and Izquierdo-Barrientos et al. [5]. For building applications, Nagano et al. [6] proposed and tested
105 at small scale a floor supply air conditioning system where a packed bed was installed in order to

106 shift cooling energy consumption to the night period. On the other hand, PCM granules can be
107 integrated into building composite materials. Hawes [7] proposed this technique for incorporating
108 PCM into concrete. Since then, a substantial number of works has been published on the preparation
109 and analysis of light weight concretes [8-10] and mortars [11-13] with PCM contained in porous
110 particles.

111 Characterization of the phase changing behaviour of granular materials is an important issue for the
112 design and optimization of latent thermal energy storage systems. However, PCM embedded into
113 granular porous solids may present difficulties when measuring enthalpy-temperature curves.
114 Differential scanning calorimeter (DSC) is a popular method of determining phase change enthalpy
115 and phase change temperature. In general, the representativeness of the sample has to be ensured, but
116 this can be compromised in DSC measurements as the sample frequently has a similar magnitude as
117 the GPCC granules. Since the PCM absorption is expected to be unequal between different granules,
118 a specific analysis of the heterogeneity of the composite material should be made before presenting a
119 result.

120 The DSC technique has been widely used for the characterization of GPCC. For instance, it was used
121 in the works of Kheramad et al. [14] and Sharifi and Sakulich [15], dealing with the preparation of
122 GPCC for incorporating PCM into lightweight aggregates that can be integrated into construction
123 materials, in order to determine the thermal energy storage capacity. Izquierdo-Barrientos et al. [16]
124 evaluated the stability through melting and solidifying cycles of the storage capacity of these particles
125 for their application in a fluidized bed heat exchanger. Rady [17] and Kheradmand et al. [14] showed
126 the significant influence of the temperature variation rate used in their experiments on the phase
127 change temperature interval determination, while its effect on the associated enthalpy variation was
128 of secondary importance. Taking this fact into account, Rady [17] and Rady and Arquis [18] proposed
129 a method, based on the adjustment of a thermal model representing the DSC device, in order to correct
130 the error associated with a non-thermal equilibrium temperature variation rate. However, a wide range

131 of heating and cooling rates (0.5-10K/min) has been used in the evaluation of the storage capacity of
132 GPCC. Although the suitability of this relevant testing parameter depends on additional aspects such
133 as the thermal conductivity of the porous matrix or the sample preparation, the effect of this heating
134 and cooling rate is not frequently evaluated when the experimental data obtained from this technique
135 are presented.

136 Rady [17] recognized that special attention has to be paid to the sample preparation when measuring
137 GPCC in order to ensure the representativeness of DSC samples. However, little detailed information
138 is usually provided about this feature. Some exceptions include Zhang et al. [19], Zhang et al. [20],
139 Li et al. [21] and Li et al. [22] who specified that crushed samples were used. Additionally, Zhang et
140 al. [19] and Zhang et al. [20] investigated the influence of this modification of the composite structure
141 on the phase transition temperature. Concerning the number of samples, Izquierdo-Barrientos et al.
142 [16] used five sets of two samples in order to analyse the storage capacity stability through melting
143 and solidifying cycles.

144 In contrast to DSC, by using the T-history method [23], the sample representativeness problem is
145 solved. The sample volume is at least one order of magnitude higher than the particle size. However,
146 it is difficult to verify if the theoretical limit imposed on the Biot number of the PCM is satisfied,
147 since the resulting thermal conductivity of the sample contained in the sample is not frequently
148 known. Additionally, as has been numerically analyzed in Mazo et al. [24], measuring solids with the
149 highest Biot number values permitted by this methodology ($Bi=0.1$) can lead to significant deviations
150 in the enthalpy-temperature curve.

151 Compared to DSC, fewer works dealing with PCM granules and the T-history methodology have
152 been found in literature. Rady et al. [25] and Rady and Arquís [18] performed cooling T-history tests
153 on GR27 and GR42 samples (Rubitherm [26]). They proposed a modification to the original method
154 [30] in order to identify the beginning and end of the solidifying process. Additionally, they applied

155 the method proposed by Marín et al. [27] in order to integrate empirical data into the enthalpy-
156 temperature curve.

157 On the other hand, with an air heat balance installation, whose methodology is based on the same
158 physical principle as that of the energy balance experimental installations developed by Zalba et al.
159 [28] or Günther et al. [29], the enthalpy variation of PCM granules in a packed bed can be quantified.
160 Although this proposed methodology cannot evaluate the enthalpy-temperature curve, it can provide
161 a direct and accurate measurement of the thermal energy variation of a GPCC packed bed between
162 the final and initial temperatures of the experimental test.

163 Finally, it has to be taken into account that the changes in the PCM supporting structure associated to
164 sample preparation (e.g. when crushed samples are used) can modify the phase change behaviour of
165 the composite material. In fact, the interaction between the PCM and the supporting porous structure
166 can lead to certain changes in phase change temperature and enthalpy [30]. Concerning its influence
167 on melting and solidifying temperature, Zhang et al. [20] identified two main effects. On the one
168 hand, the confinement inside a porous structure induces pressure variations in the PCM which are
169 associated with the volume expansion during the phase change process that modifies the melting
170 temperature. This effect can be evaluated by the Clapeyron equation. As a result of this phenomenon,
171 the confinement (or the reduction of mean pore size) produces an increase in the melting temperature
172 for most PCM ($\rho_s > \rho_l$). On the other hand, the interaction between the PCM and the inside porous
173 surface modifies the phase change temperature. This effect can be explained with the Gibbs-Thomson
174 equation. For attractive interaction between the pore surface and the liquid, the melting temperature
175 increases, whereas it decreases if the interaction is weak or repulsive. Zhang et al. [20] found that
176 capric acid showed a remarkable increase in the melting temperature when confined in pores, which
177 was explained in terms of the confinement effect and the attractive interaction of the PCM. However,
178 they did not observe any significant variation in phase change temperature in paraffin. The authors
179 explained that in the latter cases, both phenomena produced an opposite effect. Furthermore, Zhang

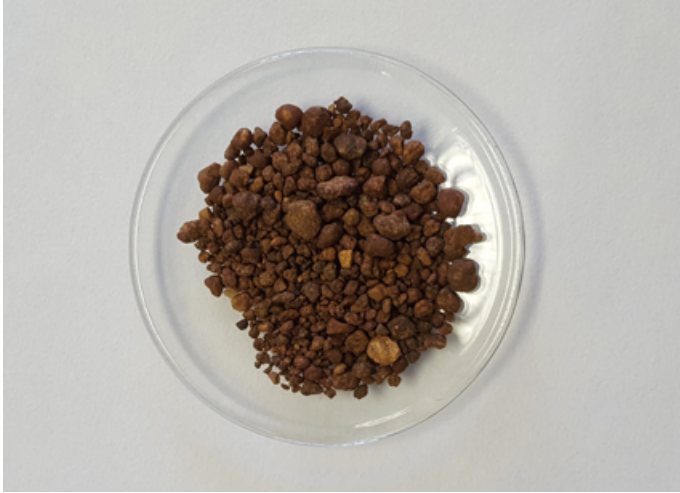
180 et al. [19] observed that the phase change temperature range was affected by the porous material and
181 also by the PCM volume fraction in composites. Zhang et al. [31] also studied different porous media
182 as the matrix for organic PCMs. They observed that there was a wider phase change temperature
183 range when relatively pure organic PCMs were confined. In the case of phase change enthalpy, a
184 reduction of its value –if it is compared to the bulk PCM material– can generally be expected as a
185 result of the confinement [30]. Nevertheless, the intensity of this reduction depends both on the PCM
186 and on the porous structure. Fu et al. [32] investigated the effect of the incorporation to a SiO₂ matrix
187 of different organic materials. They observed a slight reduction of about 5% in the phase change
188 enthalpy of paraffin composites.

189 The present study aims to evaluate the suitability of these three measuring methodologies –DSC , T-
190 history and air energy balance– for the enthalpy-temperature curve determination of GPCC. A similar
191 approach was used by Günther et al. [33] for the thermal characterization of pure PCM and PCM
192 macrocapsules. In their work, the results from DSC –obtained with both the dynamic and isothermal
193 step modes–, T-history and an air flow energy balance installation were compared. They discussed
194 the suitability of DSC methods and found good agreement between the macrocapsule experimentation
195 in the air balance set up and the T-history results for a PCM with a significant sub-cooling
196 phenomenon. In the present work, the experimental results of these methods for the thermal
197 characterization of a granular material have been analyzed and compared.

198 **2. Materials**

199 The product GR31, supplied by the manufacturer Rubitherm [26], has been characterized. These
200 granules have a particle size between the range of 1-3 mm, where paraffin is absorbed, representing
201 a mass fraction of approximately 35%, inside a porous mineral structure which contains diatom
202 (according to patent EP1628110A1, 2006 [34]). Figure 1 shows a picture of the analysed commercial

203 GPCC. According to manufacturer information, the composite undergoes an enthalpy variation of
204 60kJ/kg ($\pm 7.5\%$) within the temperature range from 20 to 35°C [26].



205

206 **Figure 1.** Image of the analysed GPCC (GR31 [26]).

207 **3. DSC measurements**

208 **3.1 Methodology adopted**

209 The present work adopts the methodology for characterizing phase change materials with a DSC
210 proposed by Lázaro et al. [35] after a set of Round Robin Tests. Firstly, heating and cooling rates
211 were applied to the PCM, starting from fast rates (10 K/min) and slowing down by halving the
212 previous rate. When the changes in peak temperature between two consecutive tests were lower than
213 0.2 K, thermal equilibrium in the sample and crucible could be assumed. The highest heating rate
214 once this condition of thermal equilibrium was achieved has been taken as the equilibrium rate. The
215 calibration was performed by using seven different standards (mercury, water, gallium, indium, tin,
216 bismuth and cesium chloride) at the equilibrium heating rate, as well as the baseline measurement
217 (empty crucible). Once these measurements were accomplished, the same or a lower sample mass
218 was measured at the equilibrium rate to ensure thermal equilibrium. Three samples and three cycles
219 were applied and the baseline subtracted from the results obtained.

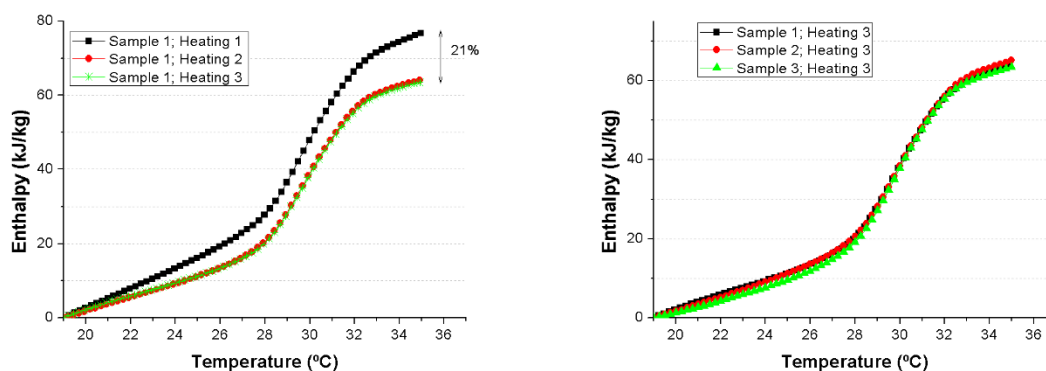
220 As previously mentioned, the characterization of GPCC using DSC requires special care to ensure
221 that the measured sample is representative of the bulk material used in practical solutions. Due to the
222 heterogeneity of the sample and to the crucible volume, achieving a representative sample can be a
223 problem. Also the morphological structure of the granules can have an influence on the heat transfer
224 process depending on the contact resistance with the crucible. In order to analyse this
225 representativeness problem, two different approaches have been followed with regard to the sample
226 preparation. On the one hand, granules with a flat surface were taken as samples to be measured,
227 placing the flat face on the crucible base to avoid an elevated thermal contact resistance. On the other
228 hand, PCM granules were crushed and subsequently compacted in the aluminium crucible, the
229 quantity being equivalent to that of one whole granule. Three samples of each preparation
230 methodology were tested.

231 The equilibrium condition was reached between the heating rate of 0.125 and 0.0625 K/min for both
232 types of sample (crushed and granule), having a sample mass of 27.93 mg for the crushed sample and
233 28.23 mg for the individual PCM granules. As a result of these equilibrium tests, measurements have
234 been executed at 0.125 K/min. Figure 2 shows the results for the crushed sample and figure 3 for the
235 granule sample.

236 Additionally, complementary measurements of the specific heat capacity have been made following
237 the procedure defined in [36], using sapphire as the reference material. Two samples of, respectively,
238 granulated and crushed GPCC were tested at a speed of 1K/min. Finally, the methodology proposed
239 in the *Guide for the expression of the uncertainty in measurement* [37] has been used to analyse the
240 uncertainty propagation through DSC results. Rudtsch [38] and Wilthan [39] applied this procedure
241 to the evaluation of the resulting uncertainty interval of specific heat capacity and temperature
242 measurements, whereas Sarge et al. [40] presented an example where that range associated with phase
243 change enthalpy was calculated. As in these previous works, repeatability of DSC signals and
244 temperature measurements have been the principal contributions to the overall uncertainty.

245 **3.2 DSC results**

246 In figure 2 a different result can be observed for the first crushed sample between the first heating
247 and the two following ones. This effect is principally associated with a deviation in the measurement
248 of specific capacity. It has to be noted that at the thermal equilibrium speed the intensity of the signal
249 corresponding to the sensible contribution to the overall thermal energy variation of the sample is
250 low. A similar behaviour was observed for the other two samples tested. The second and third heating
251 processes for all the samples have similar results. The enthalpy variation measured in the third test of
252 each crushed sample is presented in Table 1, showing maximum differences of around 4%. This can
253 also be observed in figure 2 (right). On the other hand, a possible leak of the paraffin soaked by the
254 silica supporting material could be observed with the naked eye. After the bulk material was cycled,
255 the sample turned darker due to the paraffin leak.

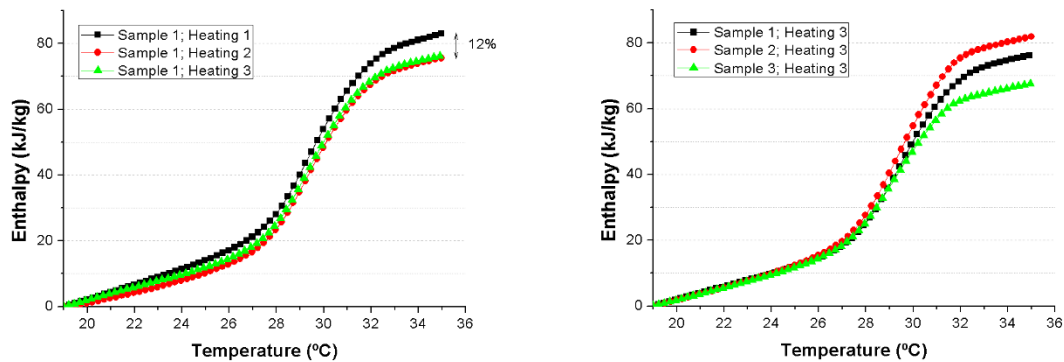


256 **Figure 2.** DSC results when GR31 is crushed. Left: Enthalpy-Temperature curve for sample 1 for 3
257 consecutive heating tests. Right: Enthalpy-Temperature curve for samples 1, 2 and 3 during the third
258 heating.
259 heating.

260 The same behaviour is observed in figure 3 in the case of testing with a granule of GR31 with a flat
261 surface set on the crucible base. The second and the third heating gave rise to a different result than
262 that of the first heating. However, in contrast to the crushed sample, it is observed that the results vary
263 depending on the granule (figure 3 left), so the samples do not seem to be representative. Differences

264 up to 20% were measured between the analysed samples (table 1). More samples would be necessary
265 to reduce the dispersion of the results of this measurement of the enthalpy variation of the granulated
266 material. In addition, due to the possible different absorption of PCM in each granule, a thermal
267 equilibrium test should be run for each sample to be measured, instead of measuring just one sample
268 and then applying the resulting equilibrium rate to the rest of the samples.

269 The significant reduction in the variability of the results using crushed samples can be associated with
270 a lower effect of the heterogeneity of the composite material on DSC results. Therefore, taking into
271 account this statistical indicator, measuring crushed GR31 samples can be recommended. However,
272 it has to be taken into account that the crushing process can modify the confinement of PCM.



273

274 **Figure 3.** DSC results for GR31 granules. Left: Enthalpy-Temperature curve for sample 1 for 3
275 consecutive heating tests. Right: Enthalpy-Temperature curve for samples 1, 2 and 3 during the
276 third heating.

277 In figure 4, the third heating of each crushed and granule sample has been compared. It is observed
278 that for the crushed samples, similar results in terms of phase change enthalpy and phase change
279 temperature are obtained, as previously mentioned. In the case of the granule samples, deviations in
280 terms of phase change enthalpy are observed, probably due to the different mass fraction of paraffin
281 absorbed by the silica matrix.

282 Concerning the phase change temperature, an additional quantification has been made. The main
 283 purpose of this analysis is to compare the DSC results to those obtained from T-history method. It
 284 has to be noted that in the latter, due to relevant effect of the noise and the precision of temperature
 285 measurements, the evaluation of the specific heat capacity at a given temperature level has a
 286 significant uncertainty range [41]. Consequently, the determination of peak temperature with this
 287 method is uncertain. The proposed additional analysis is based on the evaluation of the evolution of
 288 the liquid mass fraction curve $f(T)$. This dimensionless function is defined by the following model
 289 describing the variation of enthalpy with temperature (Eq. 1). Palomo del Barrio and Dauvergne [42]
 290 used this approach in order to describe the enthalpy-temperature curve of a PCM composite material
 291 which was determined by means of an inverse method.

$$292 \quad \frac{dh}{dT} = c_{eq}(T) = c_s + (c_l - c_s) \cdot f + h_m \cdot \frac{df}{dT} \quad (1)$$

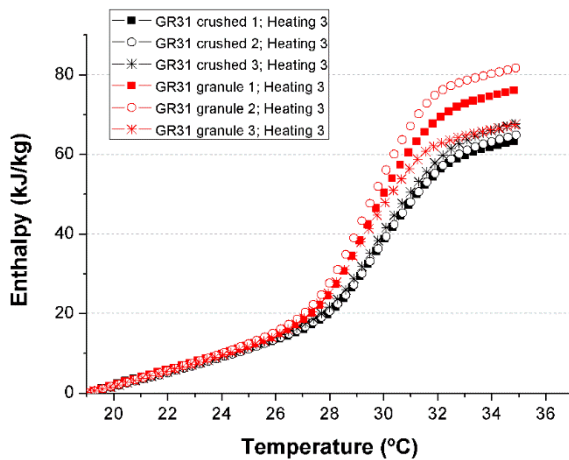
293 Where c_s and c_l are the specific heat capacity values corresponding to the solid and liquid states are
 294 measured at 22°C and 35°C respectively. Therefore, for a given enthalpy-temperature curve, the
 295 temperature dependence of the liquid fraction ($f(T)$) can be calculated by solving the previous first
 296 order differential equation (Eq. 1, imposing the initial condition $f(T_s) = 0$) thus resulting in the
 297 following expression (Eq. 2).

$$298 \quad f(T) = \frac{h(T)}{h_m} - \frac{c_s}{c_l - c_s} \cdot \left[1 - e^{\frac{c_l - c_s}{h_m} \cdot (T - T_l)} \right] - \frac{c_l - c_s}{h_m^2} \cdot e^{-\frac{c_l - c_s}{h_m} \cdot T} \cdot \int_{T_l}^T e^{\frac{c_l - c_s}{h_m} \cdot \tau} \cdot h(\tau) \cdot d\tau \quad (2)$$

299 The definite integral in equation 2 has been numerically calculated at each temperature level by means
 300 of the trapezoidal rule. Additionally, the parameter h_m , which is the one that verifies the condition f
 301 (T_l) = 1, has been calculated using an iterative scheme. Finally, an average phase change temperature
 302 (\bar{T}_m) is quantified from experimental results with the following equation (Eq. 3).

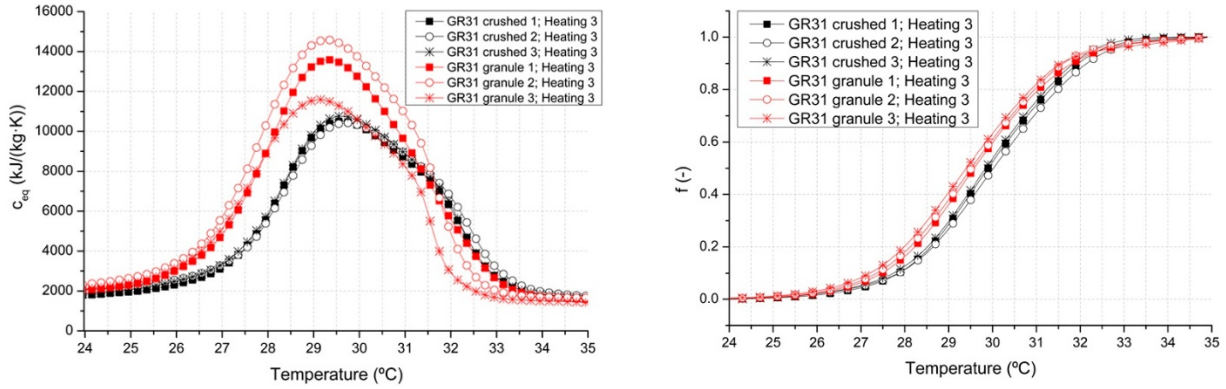
303
$$\bar{T}_m = \frac{\int_{0.05}^{0.95} T \cdot df}{0.9} \quad (3)$$

304 The measured values of peak temperatures (T_p) and average phase change temperature (\bar{T}_m) are
 305 presented in table 1, whereas the temperature evolutions of equivalent heat capacity ($c_{eq}(T) = \frac{dh}{dT}$) and
 306 the liquid fraction are shown in figure 5. It is interesting to highlight the difference in the melting
 307 temperature (approximately 0.5K, see table 1) between the crushed and the granule sample. In
 308 principle, this could be explained by a lack of thermal equilibrium, since this thermal equilibrium test
 309 was done with one only sample and the resulting heating rate directly applied to the other three
 310 samples which could be different. However, this would lead to a shift toward higher temperatures
 311 instead of lower temperatures. The crushed sample preparation could have led to this variation in the
 312 phase change temperature. Conversely, due to the high dispersion of the results of the granule
 313 samples, the effect of the modification of the porous structure on the phase change enthalpy cannot
 314 be analysed. A specific study should be carried out in order to evaluate these effects in the analysed
 315 composite material, which is beyond the scope of this work. Nevertheless, when measuring the
 316 enthalpy-temperature curve of these composites, it is recommendable to verify that the sample
 317 preparation does not significantly modify the phase change process.



318

319 **Figure 4.** Comparison of the DSC curves for the third heating for all the samples, in crushed form
 320 and in granule form.



321
 322 **Figure 5.** Analysis of the measured phase change temperature interval. Left: temperature
 323 dependence of equivalent specific heat capacity. Right: temperature dependence of the liquid
 324 fraction dimensionless parameter (f , Eq. 1).

	Crushed sample				Granule sample			
	Sample 1	Sample 2	Sample 3	μ (σ)	Sample 1	Sample 2	Sample 3	μ (σ)
Mass (mg)	12.12	20.69	21.53	-	15.6	23.41	21.91	-
T_p [°C]	29.6±0.3	29.7±0.3	29.6±0.3	29.6±0.3 (0.06)	29.3±0.3	29.3±0.3	29.1±0.3	29.3±0.3 (0.13)
\bar{T}_m [°C]	29.9±0.3	29.9±0.3	29.9±0.3	29.9±0.3 (0.06)	29.5±0.3	29.4±0.3	29.2±0.3	29.4±0.3 (0.13)
Enthalpy variation (25-35°C) [kJ/kg]	52.4±3.1	53.9±3.2	54.4±3.3	54±2 (1.0)	64.3±3.9	69.5±4.2	55.9±3.4	63.6±17.9 (6.9)
	Sample 1'	Sample 2'		μ (σ)	Sample 1'	Sample 2'		μ (σ)
Specific heat (20-22°C) [kJ/(kg·K)]	1.59±0.08	1.58±0.08		1.60±0.05 (0.01)	1.86±0.09	1.71±0.09		1.8±0.3 (0.11)
Specific heat (35-40°C) [kJ/(kg·K)]	1.37±0.10	1.38±0.10		1.37±0.07 (0.01)	1.55±0.11	1.42±0.10		1.5±0.2 (0.09)

325 **Table 1.** Mass, melting temperature and enthalpy variation (25-35°C) according to the DSC.

326 **4. T-history measurements**

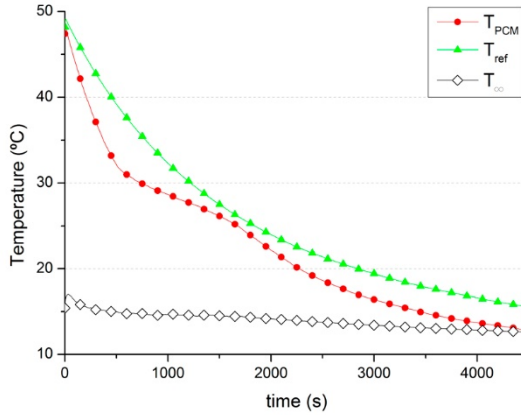
327 The material analyzed in the present study, GR31, has been measured in a T-history installation,
328 whose technical details are described in the Ph.D. dissertation by Lazaro [43]. The method proposed
329 by Marín et al. [27] has been used in order to obtain the enthalpy-temperature curve. Due to the
330 limitations of the chamber for high temperatures, only the results of cooling tests are presented in this
331 work.

332 Samples were prepared by crushing the GR31 granules in a lab mortar. The material was subsequently
333 compacted in the sample holder of the T-history set-up. Special attention must be paid in this
334 compacting process to reduce the effects related to thermal resistances resulting from the intergranular
335 space filled by air, to avoid radial thermal gradients inside the sample. These thermal gradients could
336 lead to significant deviations in the enthalpy-temperature curve determination by the T-history
337 methodology [44, 45]. Furthermore, when testing solid PCM, this effect is expected to be more
338 significant due to the fact that heat transfer takes place only by conduction.

339 According to the results of Mazo et al. [24], who theoretically analyzed the conduction transfer
340 process inside T-history samples, when the temperature is measured in the centreline, phase change
341 enthalpy can be overestimated in 10% if the tests are carried out at limit Biot numbers ($Bi \approx 0.1$). On
342 the other hand, when the temperature is measured at the surface of the sample holder, the deviation
343 in phase change enthalpy is negligible and is not expected to depend on the thermal properties of the
344 PCM sample. Therefore, in these experiments this last configuration was selected for temperature
345 measurements.

346 Type T thermocouples were used for measuring the temperature at the sample surfaces. The
347 uncertainty of the temperature measurement ($\pm 0.5^\circ\text{C}$) has been considered in the presentation of the
348 results. For this purpose, the methodology proposed by Mazo [41] for evaluating the uncertainty
349 propagation across the enthalpy-temperature curve integration process [27] has been used. In figure
350 6 the temperature evolution during the third experiment is shown whereas the results of three T-
351 history tests are gathered in table 2. The enthalpy-temperature curve obtained is presented in section

352 6, where the outcomes of the different measuring methods are compared (fig. 10). The results show
 353 a reasonable repeatability which is lower than the calculated measurement uncertainty range.



354

355 **Figure 6.** Registered time evolutions during T-history test 3 (heat capacity of T-history components:

356 $C_{ref} = m_{ref} \cdot c_{ref} = 154 \text{ J/K}$, $C_t = m_t \cdot c_t = 51 \text{ J/K}$).

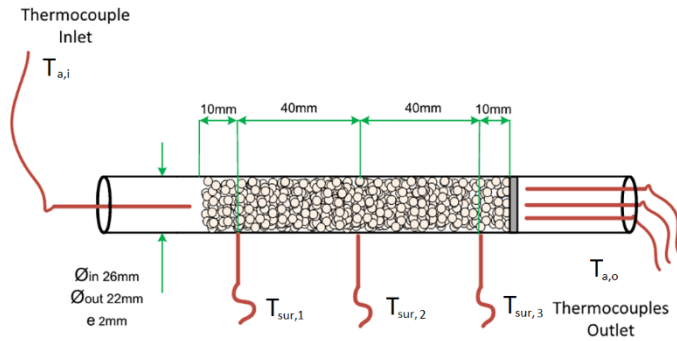
Test	m_{PCM} [g]	$c_{p,s}$ [J/(kg·K)]	$c_{p,l}$ [J/(kg·K)]	Δh [kJ/(kg·K)] (25-35°C)	T_m [°C]
T1	34.81	1.3 ± 0.4	1.6 ± 0.4	52 ± 3	29 ± 0.5
T2	34.81	1.4 ± 0.4	1.6 ± 0.4	51 ± 3	29 ± 0.5
T3	34.81	1.3 ± 0.4	1.5 ± 0.4	53 ± 3	29 ± 0.5
Repeatability (σ)	-	0.03	0.06	1.00	0.10

357 **Table 2.** Summary of the results of T-history cooling tests.

358 5. Air energy balance installation

359 The experimental installation previously developed by Dolado et al. [46] has been used for these
 360 measurements as it allows the measurement of the enthalpy variation of a packed bed of granular
 361 PCM. In figure 7 a sketch of the experimental set up is provided. The air flow temperature is measured
 362 at the air inlet and outlet sections. Additionally, the surface temperature of the glass container is
 363 measured at three points. Type T thermocouples are used for these measurements. The air volumetric

364 flow is measured by a thermal mass flow controller (Bronkhorst, EL-FLOW [47]). The uncertainty
 365 associated with each measurement is presented in table 3 and discussed in section 5.1. The GPCC
 366 packed bed is contained inside a glass tube ($D_{int}=22$ mm, $D_{out}=26$ mm, $e=2$ mm).



367

368 **Figure 7.** Sketch of the experimental set up.

369 Equation 4 represents the energy balance equation giving the enthalpy change between the beginning
 370 and the end (t_∞) of the experiment. Four main contributions are considered: energy balance to the air
 371 flow (ΔH_a), heat losses (L), and the thermal energy variations corresponding to the PCM packed bed
 372 (ΔH_{PCM}) and to the tube (ΔH_t). In this energy balance equation, thermal gains and losses due to the
 373 axial conduction heat transfer through the tube at the inlet and outlet sections and the time variation
 374 of the air flow thermal energy are neglected.

$$375 \quad m_{PCM} \cdot \Delta h_{PCM} = \int_{t=0}^{t_\infty} (T_{a,i} - T_{a,o}) \cdot \dot{m}_a \cdot c_{p,a} \cdot dt - \int_{x=0}^{L_b} (T_t|_{t_\infty} - T_\infty) \cdot \frac{m_t}{L_b} \cdot c_{p,t} \cdot dx -$$

$$376 \quad - \int_{t=0}^{t_\infty} (T_\infty - \bar{T}_t) \cdot h_{r-c} \cdot A_t \cdot dt = \Delta H_a - \Delta H_t - L \quad (4)$$

377 The equivalent radiative and convective thermal coefficient (h_{r-c}) is obtained from the final stationary
 378 situation (Eq. 5). Its radiative and convective components have been corrected at each time step of
 379 the experiment from the value calculated at the stationary situation. For this purpose, radiation heat
 380 exchange has been modelled considering the tube as small object with a grey surface ($\epsilon_f=0.9$) enclosed
 381 in a small cavity [48] (Eq. 6). On the other hand, free convection coefficient has been represented by

382 an expression of the form $Nu=C \cdot Ra^n$. If the variation of air thermophysical properties during the
 383 thermal test is neglected, the free convection heat transfer coefficient can be approximated by the
 384 following expression ($h_c \approx C' \cdot (\bar{T}_t - T_\infty)^n$) (Eq. 6). According to the correlation of Churchill and Chu
 385 [49], an exponent of 0.33 for the Raleigh number has been used.

$$386 \quad h_{c-r}|_{t_\infty} = \frac{\dot{m}_a \cdot c_{p,a} \cdot (T_{a,i} - T_{a,o})|_{t_\infty}}{A_T \cdot (\bar{T}_t|_{t_\infty} - T_\infty)} \quad (5)$$

$$387 \quad h_{c-r}|_{t_\infty} = \varepsilon_t \cdot \sigma \cdot (\bar{T}_t|_{t_\infty}^2 + T_\infty^2) \cdot (\bar{T}_t|_{t_\infty} + T_\infty) + C' \cdot (\bar{T}_t|_{t_\infty} + T_\infty)^{0.33} \quad (6)$$

388 **5.1 Uncertainty propagation analysis**

389 The uncertainty propagation of the measurements through the energy balance equation (Eq. 4) has
 390 been taken into account in order to select the most favourable conditions (air inlet temperature, length
 391 of the packed bed and air volumetric flow rate) in which to carry out these experiments. Equation 7
 392 represents this uncertainty propagation law [37] including the uncertainty of each term contributing
 393 to the energy balance equation. The accuracy of the method depends on the relation between the
 394 contributions to the energy balance equation. Due to the uncertainty propagation law, one important
 395 effect on the overall error is the amplification effect of the factor $\Delta H_a / \Delta H_{PCM}$. Considering this fact,
 396 it is more advisable to work at low values of this relation (lower heat losses and thermal inertia of the
 397 tube) than to have a very accurate measurement of these secondary terms.

$$398 \quad \frac{\delta(\Delta H_{PCM})}{\Delta H_{PCM}} = \sqrt{\left(\frac{\Delta H_a}{\Delta H_{PCM}}\right)^2 \cdot \left(\frac{\delta(\Delta H_a)}{\Delta H_a}\right)^2 + \left(\frac{\Delta H_t}{\Delta H_{PCM}}\right)^2 \cdot \left(\frac{\delta(\Delta H_t)}{\Delta H_t}\right)^2 + \left(\frac{L}{\Delta H_{PCM}}\right)^2 \cdot \left(\frac{\delta(L)}{L}\right)^2} =$$

$$399 \quad = \sqrt{\left(1 + \frac{\Delta H_t}{\Delta H_{PCM}} + \frac{L}{\Delta H_{PCM}}\right)^2 \cdot \left(\frac{\delta(\Delta H_a)}{\Delta H_a}\right)^2 + \left(\frac{\Delta H_t}{\Delta H_{PCM}}\right)^2 \cdot \left(\frac{\delta(\Delta H_t)}{\Delta H_t}\right)^2 + \left(\frac{L}{\Delta H_{PCM}}\right)^2 \cdot \left(\frac{\delta(L)}{L}\right)^2} \quad (7)$$

400 The influence of the controllable experimental conditions (air inlet temperature, length of the packed
 401 bed and volumetric air flow) in this uncertainty propagation is not simple a priori, and some opposing

402 effects can be expected. For example, if a high air inlet temperature is selected, although the relative
 403 error in the energy balance estimation to the air flow (ΔH_a) decreases (lower ratio $\delta T/\Delta T_{a,i-o}$), heat
 404 losses and energy variation of the glass tube ratios ($\Delta H_t/\Delta H_{PCM}$, $L/\Delta H_a$) are expected to increase, thus
 405 amplifying this error. Consequently, a preliminary numerical analysis has been made in order to
 406 obtain a prediction of these contributions to the energy balance equation at different testing
 407 conditions. In this way, an estimation of the resulting measurement uncertainty interval in a variety
 408 of situations can be calculated. In section 5.1.1 the numerical model is briefly described, whereas the
 409 parametric analysis that has been carried out with the purpose of determining a range of favourable
 410 testing conditions is presented in section 5.1.2.

411 Table 3 gathers the information about the sensors used in the experimental setup and their associated
 412 uncertainty. The uncertainty of each contribution to the energy balance equation (Eq. 4) has been
 413 calculated using the uncertainty propagation law with equations 8, 9 and 10. Their values will be
 414 shown in section 5.4.

$$415 \quad \frac{\delta EB_a}{EB_a} = \sqrt{\left(\frac{\delta \dot{m}_a}{\dot{m}_a}\right)^2 + \left(\frac{\delta(\Delta T_a)}{\Delta T_a}\right)^2}; \quad \frac{\delta H_t}{H_t} = \sqrt{\left(\frac{\delta c_t}{c_{p,t}}\right)^2 + \left(\frac{\delta(\Delta T_{sur,\infty})}{\Delta T_{sur,\infty}|_{t_\infty}}\right)^2} \quad (8-9)$$

$$416 \quad \frac{\delta L}{L} = \sqrt{\left(\frac{\delta h_{c-r}}{h_{c-r}}\right)^2 + \left(\frac{\delta(\Delta T_{sur,\infty})}{\Delta T_{sur,\infty}}\right)^2} = \sqrt{\left(\frac{\delta \dot{m}_a}{\dot{m}_a}\right)^2 + \left(\frac{\delta(\Delta T_a)}{\Delta T_a|_{t_\infty}}\right)^2 + \left(\frac{\delta(\Delta T_{sur,\infty})}{\Delta T_{sur,\infty}}\right)^2} \quad (10)$$

Magnitude	Sensor	Uncertainty
Air temperature	Thermocouple type T	$\pm 0.5^\circ\text{C}$
Surface temperature	Thermocouple type T	$\pm 0.5^\circ\text{C}$
Volumetric flow rate	Flow controller	$\pm 0.6\%$

417 **Table 3.** Uncertainty of the magnitudes measured.

418 **5.1.1 Numerical model**

419 The numerical model which has been developed in order to simulate the heat transfer inside the PCM
 420 packed bed is briefly described in this section. The model is based on the following assumptions:
 421 uniform temperature inside the PCM granules; uniform temperature across the packed bed section
 422 and uniform air flow; heat transfer between the granules and the inside surface of the tube is neglected;
 423 time variation of the thermal energy of the air is not considered; and, finally, the tube containing the
 424 packed bed is considered as a lumped heat capacity system in radial direction where axial heat
 425 conduction inside the tube has been neglected. According to these simplifications, the problem can
 426 be represented by the following equations (eq. 11-12), corresponding, respectively, to the energy
 427 balance –formulated in its differential form– of the air stream (eq. 11), packed bed particles (eq. 12)
 428 and the wall of the tube (eq. 13).

$$429 \quad \dot{m}_a \cdot c_{p,a} \cdot \frac{\partial T_a}{\partial x} = \frac{\pi \cdot D_b^2}{4} \cdot a_b \cdot h_{c,b} \cdot (T_b - T_a) + \pi \cdot D_b \cdot h_{c,b} \cdot (T_t - T_a) \quad (11)$$

$$430 \quad 6 \cdot h_{c,b} \cdot (T_a - T_b) = D_p \cdot \rho_p \cdot \frac{\partial h_{PCM}}{\partial t} \quad (12)$$

$$431 \quad (D_b + e) \cdot h_{r-c} \cdot (T_\infty - T_t) + D_b \cdot h_{c,b} \cdot (T_a - T_t) = \frac{(D_b + e)^2 - D_b^2}{4} \cdot \frac{m_t}{L_b} \cdot c_t \cdot \frac{\partial T_t}{\partial t} \quad (13)$$

432 It should be noted that the main assumptions of the model (one-dimensional analysis, uniform
 433 temperature inside PCM granules) are identical to those adopted by Rady [2, 3], Izquierdo-Barrientos
 434 [50] and Izquierdo-Barrientos et al. [51]. The prediction of these models has been demonstrated to be
 435 accurate enough for the purpose of this work. For the external convective component of the equivalent
 436 heat transfer coefficient (h_{r-c}), the correlation from Churchill and Chu [49] has been used, whereas
 437 that formulated by Wakao [52] has been utilized for calculating the heat exchange coefficient inside
 438 the packed bed ($h_{c,b}$).

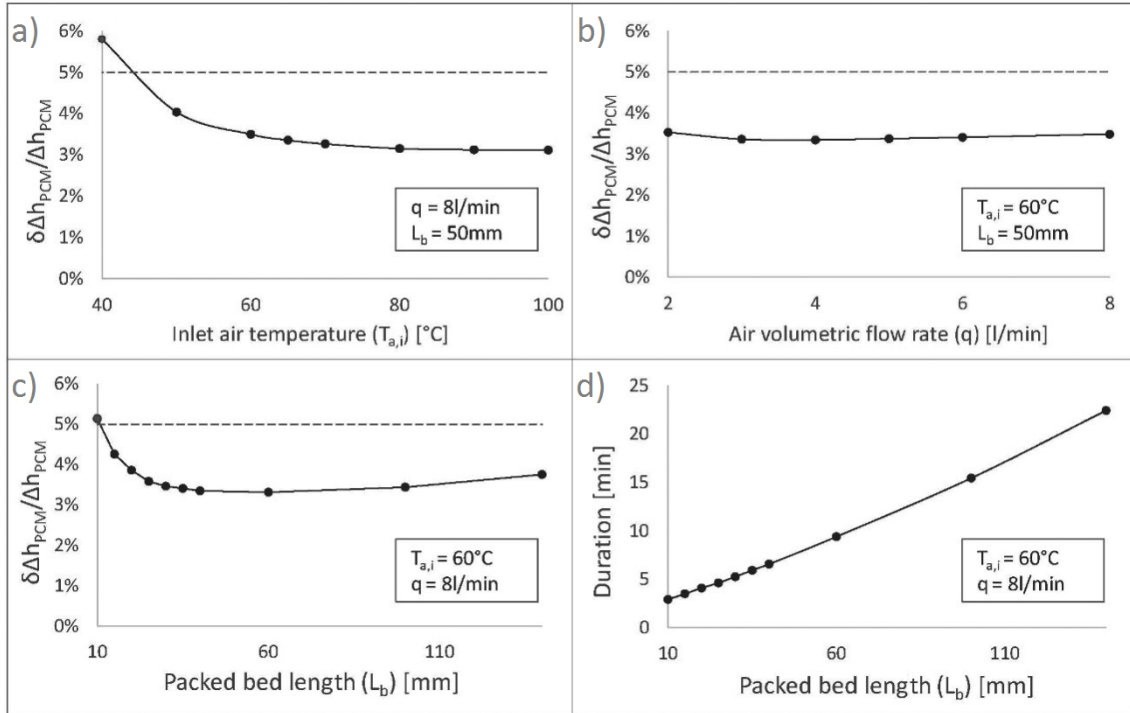
439 An enthalpy method has been used in order to handle the phase change. A fully implicit method has
 440 been utilized for time discretization and a central difference scheme has been chosen for the spatial

441 discretization since, due to the high contact surface, the Peclet number associated to the numerical
442 scheme is 0.6 [53].

443 **5.1.2 Determination of temperature levels and lengths for the packed bed**

444 The previously described numerical model has been used to evaluate the influence of the experimental
445 conditions on the uncertainty propagation of sensor errors during the measurement of the enthalpy
446 variation of the PCM packed bed. The effect of the length of the tube (L_b [mm]), the air inlet
447 temperature ($T_{a,i}$ [°C]) and the air flow (q [l/min]) has been analyzed. The objective is to determine
448 an acceptable range for these conditions where an uncertainty of $\pm 5\%$ is ensured.

449 In figure 8, the influence of the previously mentioned experimental conditions on the uncertainty of
450 the results is plotted ($\delta h_{PCM}/\Delta h_{PCM}$ [%]). Looking at the effect of the inlet temperature (fig. 8 (a)), it
451 can be seen that the error decreases when the air inlet temperature rises in the temperature range
452 analyzed. In this case, the most important effect on the uncertainty propagation through the energy
453 balance equation is the temperature difference between the air inlet and outlet. Additionally, the
454 influence of the air volumetric flow rate is negligible for this combination of uncertainties of the
455 measured variables. According to these results, the inlet temperature should be selected above 50°C.
456 Concerning the packed bed length (fig. 8 (c, d)), the main influence on the overall uncertainty is the
457 increase in the ratio between heat losses and the enthalpy variation of the PCM ($L/\Delta H_{PCM}$). According
458 to this, packed bed lengths from 40 to 100 mm can be chosen, since they produce an acceptable error
459 in the solution ($\pm 5\%$, fig. 8 (c)) and a reasonable duration for the experiment (5 to 15min, fig. 8 (d)).

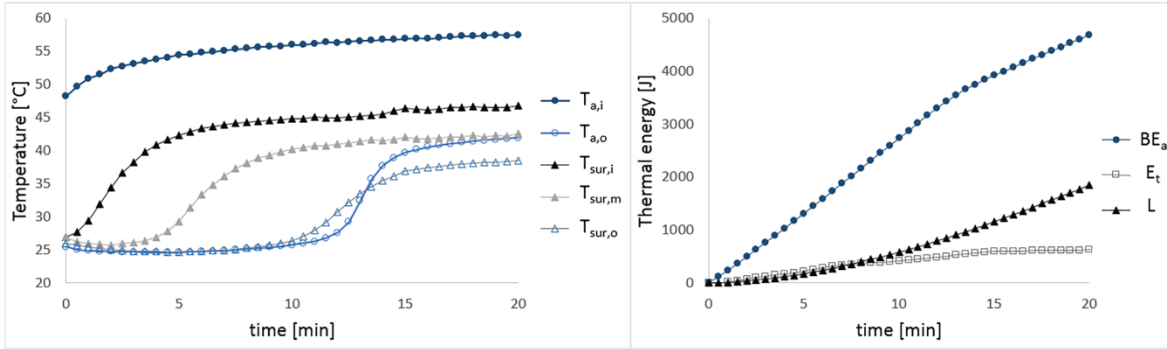


460

461 **Figure 8.** Influence of the experimental conditions (air inlet temperature (a), air volumetric flow
 462 rate (b) and packed bed length (c,d)) on the uncertainty propagation of the results and the duration
 463 of the experiment.

464 **5.2 Results**

465 Figure 9 shows an example of the temperature evolution of the air and the packed bed container
 466 during the test. Table 4 gathers the results from the measurements of GR31. The calculated
 467 uncertainty associated with each thermal energy variation is also presented. A good repeatability, less
 468 than 5%, has been observed in these experiments.



469

470 **Figure 9.** Temperature evolution and thermal energy contributions to the overall energy balance
 471 (GR31-T3).

	m_{PCM} [g]	Δh_{PCM} [kJ/kg]	ΔT_{PCM} [°C]	$T_{a,i}$ [°C]	$T_{a-o} _{t_\infty}$ [°C]	T_∞ [°C]	\dot{V} [l/min]	$h_{c-r} _{t_\infty}$ [W/(m ² ·K)]
T1	27.65	70.9±3.3	[24.8-46.7]	57.3	41.1	25.5	7.2	14±1
T2	27.63	71.5±3.5	[24.4-48.5]	55.3	40.0	24.5	7.3	13±1
T3	27.65	71.7±3.5	[24.8-49.1]	57.5	43.5	24.7	8	12±1

Repeatability Δh_{PCM} ($\sigma_{\text{GR31}}=1.2\text{kJ/kg}$)

472 **Table 4.** Results of the experimental tests (GR31).

473 It should be noted that the measurement model used in this method is based on a simpler hypothesis
 474 than that of the T-history method. Whereas in the energy balance methodology the main contribution
 475 to the energy variation of the PCM packed bed can be quantified from the thermal energy transferred
 476 to the air stream, in the T-history method a uniform temperature inside the samples and an identical
 477 equivalent heat transfer coefficient at the surface of both samples (reference and PCM) have to be
 478 assumed.

479 Nevertheless, this complementary method is not able to evaluate the enthalpy-temperature curve since
 480 the temperature of the packed bed is not uniform during the experiment. Additionally, as discussed
 481 in the previous section, the accuracy depends heavily on the experimental conditions. The most
 482 relevant variable in the resulting accuracy is the inlet temperature. This effect leads to a lower limit

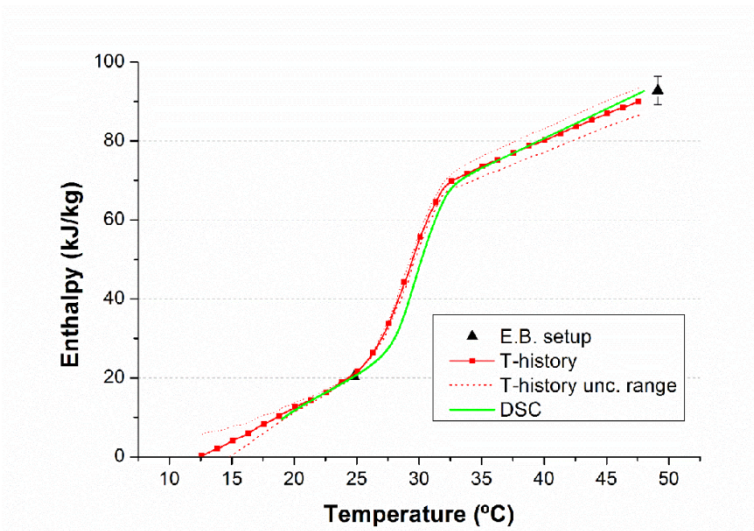
483 for the temperature interval in which the enthalpy variation can be measured with acceptable
 484 accuracy.

485 **6. Discussion**

486 The results obtained from the application of the different experimental methodologies can be
 487 compared in table 5 and figure 10. As can be seen, there is a good agreement between the measured
 488 enthalpy variation values. The DSC results obtained with crushed samples are included within the
 489 estimated uncertainty range of the T-history and energy balance experimental methods.

Method	c_s [g]	c_l [kJ/kg]	\bar{T}_m [°C]	Δh_{PCM} [kJ/kg] (25-35°C)	Δh_{PCM} [kJ/kg] (24.8-49°C)
DSC <u>granule</u>	1.8±0.3	1.4±0.2	29.4±0.3	64±18	80±21
DSC crushed	1.60±0.05	1.4±0.1	29.9±0.3	54±2	74±5
T-history crushed	1.6±0.4	1.3±0.4	29.0±0.5	52±3	71±4
E. B. set up <u>granule</u>	-	-	-	-	73±4

490 **Table 5.** Comparison of the results obtained with the different experimental methodologies.



491

492 **Figure 10.** Comparison of the results obtained with the different experimental methodologies.

493 On the other hand, there is an appreciable difference between the phase change temperature of the
494 DSC and T-history measurements (0.9°C). This is not only due to a slight hysteresis phenomenon of
495 the material, but also to a deviation in T-history associated with the thermal gradient inside the PCM
496 sample. According to Mazo et al. [24], the theoretically expected deviation in the measurement of
497 phase change temperature can be bounded by linear functions which are proportional to the Biot
498 number and the temperature difference between the ambient and phase change temperatures (Eq. 14).

$$499 \quad 0.44 \cdot Bi_{PCM} \cdot |T_{\infty} - \bar{T}_m| \leq |\delta T_m| \leq 0.70 \cdot Bi_{PCM} \cdot |T_{\infty} - \bar{T}_m| \quad (14)$$

500 The Biot number is conditioned by the experimental configuration and cannot be modified.
501 Furthermore, in the case of crushed samples, it is difficult to estimate the equivalent conductivity and
502 consequently the Biot number. Therefore, if a higher accuracy of the phase change temperature
503 measurement is required, an expansion of the experimental methodology should be developed in
504 order to reduce the effect of this phenomenon. This procedure would involve carrying out thermal
505 tests at reduced ambient temperature differences ($T_{\infty} - T_m$) in order to reduce the deviation in the
506 phase change temperature measurements associated to the thermal gradients inside the sample. On
507 the other hand, it has to be taken into account that the reduction of this temperature interval ($T_{\infty} - T_m$)
508 increases the uncertainty of the phase change enthalpy measurement, according to the results of Zhang
509 et al. [23] and Mazo [41].

510 **7. Conclusions**

511 This work has analyzed some problematic issues associated with the determination of the enthalpy-
512 temperature curves of GPCC by comparing different experimental methodologies. The principal
513 characteristics of these procedures are summarized in the following table (table 6).

514

515

Methodology	h-T curve	Sample mass [g]	Sample form		Advantages	Disadvantages
			Granules	Crushed granules		
DSC	Yes	0.02	Yes	Yes	h-T curve is obtained Crushed samples can be measured to reduce the dispersion of the results	If the granule is measured without being crushed, an appropriate sampling must be done. This will lead to a long experiment to get representative results. The crushed sample preparation can modify phase change temperature
T-history	Yes	8-25	No	Yes	Bigger sample sizes, which means a more representative sample.	Sample must be crushed and compacted to avoid temperature gradients inside the sample. It is difficult to estimate the equivalent conductivity and consequently the Biot number of crushed samples
E.B. setup	No	30	Yes	No	Sample representativeness The model from which the energy variation of PCM is measured is based on a simpler hypothesis than the DSC and T-history methods.	h-T curve cannot be measured. Only the enthalpy variation in a temperature interval. Experimental conditions, especially temperature levels, have a high influence on the accuracy of measurements. Thus, the quality of the measurement limits the temperature interval

516 **Table 6.** Main characteristics of experimental methodologies for evaluating enthalpy variations in
517 granular PCM composites.

518 First of all, the evaluation of the energy balance in the heat exchange between an air stream and a
519 granular PCM packed bed provides a measurement of the enthalpy variation of this composite
520 material. With a suitable design, considerably accurate measurements of the enthalpy variation of
521 representative samples of granular PCM can be obtained. In this case, a repeatable measurement has
522 been obtained that can be used in the comparison with other experimental methodologies.

523 The results of the DSC analysis have shown a significant deviation in the measurement of the phase
524 change enthalpy variation of three granule samples ($\sigma_{\Delta h}/\Delta h \approx 11\%$). Since these differences can be
525 attributed to the heterogeneity of the composite material, a specific methodology should be developed
526 in order to improve the accuracy of this measurement. Additionally, the equilibrium condition
527 proposed by Lázaro et al. [35] should be verified in each granular PCM composite sample. Therefore,
528 this methodology is very time-consuming.

529 On the other hand, when crushed samples are used the dispersion in phase change enthalpy
530 measurements is considerably reduced ($\sigma_{\Delta h}/\Delta h \approx 2\%$). Furthermore, these values are consistent with
531 those obtained with the T-history methodology and the energy balance experimental set up.
532 Nevertheless, a slight difference in melting temperature (0.5°C) between the granule sample and the
533 crushed sample was detected. This deviation can be explained in terms of a change of the PCM
534 confinement in the porous material related to the preparation of the crushed sample. Therefore, in a
535 general case, if this sample preparation technique is used, it is recommendable to verify if the resulting
536 modifications of the phase change process are acceptable for a specific application.

537 Compared to the DSC results, the T-history tests provided a reasonable approximation of the
538 enthalpy-temperature curve. Nevertheless, when the temperature is measured at the surface of the
539 sample, the hysteresis phenomenon is expected to be overestimated [24]. Therefore, it would be of
540 interest to develop a procedure in order to adapt the temperature interval of the T-history test to the
541 required accuracy in phase change temperature measurements.

542 **Acknowledgments**

543 The authors thank the Spanish Ministry of Economy and Competitiveness for the funding of this work
544 within the framework of projects ENE2011-28269-C03-01, ENE2011-22722 and ENE2014- 57262-
545 R, partially funded by the Spanish Government (Energy Program), the Government of Aragon (Spain)
546 and the Social Fund of the European Union (FEDER Program). The authors would like to

547 acknowledge the use of the Servicio General de Apoyo a la Investigación-SAI, Universidad de
548 Zaragoza.

549 **References**

550 [1] K. Nagano, S. Takeda, T. Mochida, K. Shimakura, Thermal characteristics of a direct heat
551 exchange system between granules with phase change material and air, *Applied Thermal*
552 *Engineering* 24 (14-15) (2004) 2131-2144.

553 [2] M. Rady, Granular phase change materials for thermal energy storage: Experiments and
554 numerical simulations, *Applied Thermal Engineering* 29 (14-15) (2009) 3149-3159.

555 [3] M. Rady, Thermal performance of packed bed thermal energy storage units using multiple
556 granular phase change composites, *Applied Energy* 86 (12) (2009) 2704-2720.

557 [4] M. A. Izquierdo-Barrientos, C. Sobrino, J. A. Almedros-Ibáñez, Thermal energy storage in a
558 fluidized bed of PCM, *Chemical Engineering Journal* 230 (2013) 573-583.

559 [5] M. A. Izquierdo-Barrientos, M. Fernández-Torrijos, J. A. Almedros-Ibáñez, C. Sobrino,
560 Experimental study of fixed and fluidized beds of PCM with an internal heat exchanger, *Applied*
561 *Thermal Engineering* 106 (2016) 1042-1051.

562 [6] K. Nagano, S. Takeda, T. Mochida, K. Shimakura, T. Nakamura, Study of a floor air
563 conditioning phase change material to augment building mass thermal storage. Heat response in
564 small scale experiments, *Energy and Buildings* 38 (5) (2006) 436-446.

565 [7] D.W. Hawes, *Latent Heat Storage in Concrete*, (PhD Thesis) Concordia University (1991)
566 Montreal, Quebec (Canada).

567 [8] D. Zhang, Z. Li, J. Zhou, K. Wu, Development of thermal energy storage concrete, *Cement and*
568 *Concrete Research* 34 (6) (2004) 927-934.

- 569 [9] A. R. Sakulich, D. P. Bentz, Incorporation of phase change materials in cementitious systems
570 via fine lightweight aggregate, *Construction and Building Materials* 35 (2012) 483-490.
- 571 [10] H. Cui, S. A. Memon, R. Liu, Development, mechanical properties and numerical simulation
572 of macro encapsulated thermal energy storage concrete, *Energy and Buildings* 96 (2015) 162-174.
- 573 [11] M. Li, Z. Wu, J. Tan, Heat storage properties of the cement mortar incorporated with
574 composite phase change material, *Applied Energy* 103 (2013) 393-399.
- 575 [12] Z. Zhang, G. Shi, S. Wang, X. Fang, X. Liu, Thermal energy storage cement mortar containing
576 n-octadecane/expanded graphite composite phase change material, *Renewable Energy* 50 (2013)
577 670-675.
- 578 [13] S. Kim, S. J. Chang, E. Chung, S. G. Jeong, S. Kim, Thermal characteristics of mortar
579 containing hexadecane/xGn SSPCM and energy storage behaviors of envelopes integrated with
580 enhanced heat storage composites for energy efficient buildings, *Energy and Buildings* 70 (2014)
581 472-479.
- 582 [14] M. Kheradmand, J. Castro-Gomes, M. Azenha, P. D. Silva, J. L. B. Aguiar, S. E. Zoorob,
583 Assessing the feasibility of impregnating phase change materials in lightweight aggregate for
584 development of thermal energy storage systems, *Construction and Building Materials* 89 (2015) 48-
585 59.
- 586 [15] N. P. Sharifi, A. Sakulich, Application of phase change materials to improve the thermal
587 performance of cementitious material, *Energy and Buildings* 103 (2015) 83-85.
- 588 [16] M. A. Izquierdo-Barrientos, C. Sobrino, J. A. Almedros-Ibáñez, C. Barreneche, N. Ellis, L. F.
589 Cabeza, Characterization of granular phase change materials for thermal energy storage applications
590 in fluidized beds, *Applied Energy* 181 (2016) 310-321.

- 591 [17] M. Rady, Study of phase changing characteristics of granular composites using differential
592 scanning calorimetry, *Energy Conversion and Management* 50 (5) (2009) 1210-1217.
- 593 [18] M. Rady, E. Arquis, A comparative study of phase changing characteristics of granular phase
594 change materials using DSC and T-history methods, *Fluid Dynamics & Materials Processing* 6 (2)
595 (2010) 137-152.
- 596 [19] D. Zhang, J. Zhou, K. Wu, Z. Li, Granular phase changing composites for thermal energy
597 storage, *Solar Energy* 78 (3) (2005) 471-480.
- 598 [20] D. Zhang, S. Tian, D. Xiao, Experimental study on the phase change behavior of phase change
599 material confined in pores, *Solar Energy* 81 (5) (2007) 653-660.
- 600 [21] X. Li, J. G. Sanjayan, J. L. Wilson, Fabrication and stability of form-stable diatomite/paraffin
601 phase change material composites, *Energy and Buildings* 76 (2014) 284-294.
- 602 [22] X. Li, H. Chen, L. Liu, Z. Lu, J. G. Sanjayan, W. H. Duan, Development of granular expanded
603 perlite/paraffin phase change material composites and prevention of leakage, *Solar Energy* 137
604 (2016) 179-188.
- 605 [23] Y. Zhang, Y. Jiang, Y. Jiang, A simple method, the T-history method, of determining the heat
606 of fusion, specific heat and thermal conductivity of phase-change materials, *Measurement Science
607 and Technology* 10 (1999) 201-205.
- 608 [24] J. Mazo, M. Delgado, A. Lázaro, P. Dolado, C. Peñalosa, J.M. Marín, B. Zalba, A theoretical
609 study on the accuracy of the T-history method for enthalpy-temperature curve measurement:
610 analysis of the influence of thermal gradients inside T-history samples, *Measurement Science and
611 Technology* 26 (12) (2015) 125001.

- 612 [25] M. A. Rady, E. Arquis, C. Le Bot, Characterization of granular phase changing composites for
613 energy storage using the T-history method, *International Journal of Energy Research* 34 (4) (2010)
614 333-344.
- 615 [26] RUBITHERM GmbH, www.rubitherm.de, (accessed 8.3.17)
- 616 [27] J. M. Marín, B. Zalba, L. F. Cabeza, H. Mehling, Determination of enthalpy-temperature
617 curves of phase change materials with the temperature-history method: improvement to temperature
618 dependent properties, *Measurements Science and Technology* 14 (2003) 184-189.
- 619 [28] B. Zalba, J.M. Marín, L.F. Cabeza, H. Mehling, Free-cooling of buildings with phase change
620 materials, *International Journal of Refrigeration* 27 (8) (2004) 839-849.
- 621 [29] E. Günther, S. Hiebler, H. Mehling, Determination of the heat storage capacity of PCM and
622 PCM-objects as a function of temperature, *Proceedings of ECOSTOCK*, Stockton (USA) (2006).
- 623 [30] H.K. Christenson, Confinement effects on freezing and melting, *Journal of Physics: Condensed*
624 *Matter* 13 (2001) 95-133.
- 625 [31] D. Zhang, K. Wu, Z. Li, Tuning effect of porous media's structure on the phase changing
626 behavior of organic phase changing matters, *Journal of Tongji University* 32 (2014) 1163-1167.
- 627 [32] Z. Fu, L. Su, M. Liu, J. Li, Z. Zhang, B. Li, Confinement effect of silica mesopores on thermal
628 behaviour of phase change materials, *Journal of Sol-Gel Science Technology* 50 (2016) 180-188.
- 629 [33] E. Günther, S. Hiebler, H. Mehling, R. Redlich, Enthalpy of phase change materials as a function
630 of temperature: required accuracy and suitable measurement methods, *International Journal of*
631 *Thermophysics* 30 (2009) 1257-1269.
- 632 [34] M.S. Toas, D.G. Ober, M.P. Ellis, Loose fill insulation product having phase change material
633 therein (2006) EP1628110A1.

634 [35] A. Lazaro, C. Peñalosa, A. Solé, G. Diarce, T. Haussmann, M. Fois, B. Zalba, S. Gschwander,
635 L.F. Cabeza, Intercomparative tests on phase change materials characterization with differential
636 scanning calorimeter, *Applied Energy* 109 (2013) 415-420.

637 [36] ASTM E1269—11 Standard test method for determining specific heat capacity by differential
638 scanning calorimetry, ASTM International.

639 [37] BIPM, IEC, IFCC, ISO, IUPAC, IUPAP, OIML, Evaluation of measurement data. Guide to the
640 expansion of uncertainty in measurement JCGM 100: 2008, 1st edition, Sèvres (2008) BIPM Joint
641 Committee for Guides in Metrology.

642 [38] S. Rudtsch, Uncertainty of heat capacity measurements with differential scanning calorimeters,
643 *Termochimica Acta*, 382 (2002) 17-25.

644 [39] B. Wilthan, Uncertainty budget for high temperature heat flux DSCs, *Journal of Thermal*
645 *Analysis and Calorimetry*, 118 (2014) 603-611.

646 [40] S. M. Sarge, G. W. H. Höhne, W. Hemminger, *Calorimetry. Fundamentals, instrumentation*
647 *and applications*, Wiley-WCH, Weinheim, Germany, 2014.

648 [41] J. Mazo, Research about the application of thermal energy storage with PCM in thermally
649 activated building elements, Ph.D. Thesis (2016) Zaragoza.

650 [42] E. Palomo del Barrio, J. L. Dauvergne, A non-parametric method for estimating enthalpy-
651 temperature functions of shape-stabilized phase material, *International Journal of Heat and Mass*
652 *Transfer* 54 (2011) 1268-1277.

653 [43] A. Lázaro, *Thermal Energy Storage with Phase Change Materials. Building applications:*
654 *Material behavior characterization and experimental setup for testing air-PCM heat exchangers*,
655 Ph.D. Thesis (2008) Universidad de Zaragoza.

656 [44] H. Hong, C. Kang, J.H. Peck, Measurement methods of latent heat for PCM with low melting
657 temperature in closed tube, *International Journal of Air-Conditioning and Refrigeration* 12 (4)
658 (2004) 206-213.

659 [45] H. Hong, S.K. Kim, Y.S. Kim, Accuracy improvement of T-history method for measuring heat
660 of fusion of various materials, *International Journal of Refrigeration* 27 (4) (2004) 360-366.

661 [46] P. Dolado, I. Miranda, J.S. Urieta, J. Coronas, A. Lázaro, Packed bed zeolite experimental
662 setup to study TCS systems up to 200°C, *Eurosun 2014* (2014), Aix-les Bains, France.

663 [47] Bronkhorst, <http://www.bronkhorst.com/files/downloads/brochures/folder-el-flow.pdf>,
664 (accessed 8.3.17)

665 [48] F. P. Incropera, D. P. DeWitt, T. L. Bergman, A. S. Lavine, *Fundamentals of heat and mass*
666 *transfer*, United States of America (2007) John Wiley & Sons.

667 [49] S.W. Churchill, H.H.S. Chu, Correlating equations for laminar and turbulent free convection
668 from a horizontal cylinder, *International Journal of Heat and Mass Transfer* 18 (9) (1975) 1049-
669 1053.

670 [50] M. A. Izquierdo-Barrientos, *Heat transfer and thermal storage in fixed and fluidized beds of*
671 *phase change material*, PhD Thesis (2014) University of Carlos III, Madrid (Spain).

672 [51] M. A. Izquierdo-Barrientos, C. Sobrino, J. A. Almedros-Ibáñez, Modeling and experiments of
673 energy storage in a packed bed with PCM, *International Journal of Multiphase Flow* 86 (2016) 1-9.

674 [52] N. Wakao, S. Kaguei, T. Funazkri, Effect of fluid dispersion coefficients on particle to fluid
675 heat transfer coefficients in packed beds, *Chemical Engineering Science* 34 (3) (1979) 325-336.

676 [53] S. V. Patankar, *Numerical heat transfer and fluid flow*, New York (1980) McGraw-Hill.