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Combining ultraviolet light and mild temperatures for the inactivation of *Escherichia coli* in orange juice

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22 ABSTRACT

23	It is difficult to guarantee the effectiveness of UV technology to reach 5 Log ₁₀ cycles of
24	inactivation of <i>Escherichia coli</i> in a large amount of fruit juices with high absorption
25	coefficients and turbidities, such as orange juice. The aim of this work was to overcome
26	this limitation by combining UV light and mild temperatures. UV treatments were
27	carried out in an equipment with eight individual annular thin film flow-through
28	reactors connected sequentially and submerged in a thermostatic water bath. A
29	treatment of 13.55 J/mL reached 0.25±0.04, 0.41±0.13, 0.84±0.32, 0.96±0.12,
30	2.57 \pm 0.05, 5.41 \pm 0.23, and more than 6 Log ₁₀ cycles of inactivation of <i>E. coli</i> STCC
31	4201 suspended in commercial sterilized orange juice at 25.0, 40.0, 50.0, 52.5, 55.0,
32	57.5, and 60.0 °C, respectively. The comparison of UV resistance at 25 °C with heat
33	resistance at mild temperatures demonstrated a synergistic effect of both technologies
34	applied simultaneously. The maximum synergistic lethal effect was reached at 55 ° C
35	(68.03%).
36	A UV light treatment (23.72 J/mL) at 55 °C (3.6 min) of freshly squeezed orange juice
37	allowed reaching more than 5 Log ₁₀ cycles of inactivation of a <i>E. coli</i> cocktail (STCC
38	4201, STCC 471, ATCC 27325, ATCC 25922, and O157:H7 Chapman strain). The
39	selected treatment did not affect the pH, acidity, °Brix, and color, and decreased 16.45%
40	ascorbic acid content and 63.96% the Pectinmethylesterase activity.
41	
42	Keywords: Pasteurization, orange juice, Escherichia coli, ultraviolet, heat treatment
43	
44	

1. Introduction

47	The food industry has been challenged to improve the safety, stability, and convenience
48	of foods and a great effort has been made to develop more appropriate methods for food
49	preservation and sanitation. At present, it can be foreseen that none of the new
50	technologies under study will replace traditional preserving procedures for a wide range
51	of products. However, each one shows particular advantages that may make it the most
52	adequate technology for a certain product or process.
53	Among the nonthermal technologies developed in the last few decades, ultraviolet (UV)
54	light irradiation is one of the most promising because it is easy to use and lethal to most
55	microorganisms (Bintsis et al., 2000), it does not generate chemical residues (Guerrero-
56	Beltrán, 2004), and it is a dry cold process (Bachmann, 1975) that can be effective at
57	low cost in comparison with other preservation methods (Geveke, 2005).
58	The wavelength range for UV light for food processing varies from 100 to 400 nm and
59	is categorized as UV-A (320-400 nm), UV-B (280-320), and UV-C (200-280 nm).
60	Short-wave UV radiation (UV-C) is considered the germicidal region lethal to most
61	types of microorganisms (Bintsis et al., 2000; Sizer and Balasubramaniam, 1999). In
62	this range, the maximum efficacy is best achieved between 250 and 270 nm, and
63	decreases as wavelength increases. UV-C light of 254 nm, generated by low-pressure
64	mercury lamps, is usually used for disinfection purposes.
65	The use of UV light is well established for air and water disinfection, but its use for the
66	pasteurization of liquid foods is still limited. Evidence has demonstrated that UV
67	technology is a promising alternative to thermal pasteurization for a range of liquid
68	foods. In fact, the National Advisory Committee on Microbiological Criteria for Foods
69	of the USDA (NACMCF) revised the definition of "pasteurization" in 2004 and
70	included UV irradiation as an alternative to heat that can be used for pasteurization

71	purposes. However, the bactericidal efficacy of UV light depends on the optical
72	properties of the treatment medium. The penetration of UV radiation depends on the
73	absorptivity of the liquid, which varies with the color of compounds and the amount of
74	soluble and/or suspended solids (Koutchma et al., 2004). The penetration depth also
75	depends on the turbidity of the media. Suspended solids increase the absorptivity but are
76	also responsible for reflection and scattering phenomena (Koutchma et al., 2004;
77	Liltved and Cripps, 1999). As a consequence of these phenomena, UV light only
78	penetrates a very short depth inside the liquid food surface. For example, it has been
79	estimated that 90% of the radiation is absorbed in about 1.1 cm depth of wine, 0.63 cm
80	of beer, 0.67 cm of clear apple juice, and 0.1 cm in orange juice (Koutchma, 2009). This
81	explains the wide range of variation of Log_{10} cycles of bacterial inactivation obtained
82	when microorganisms are suspended in liquid foods. Overall, published data
83	demonstrated that it is difficult to guarantee the effectiveness of UV technology to reach
84	5 Log ₁₀ cycles of bacterial inactivation in a large amount of fruit juices with high
85	absorption coefficients and turbidities.
86	To overcome the limitations of non-thermal methods of food preservation, new
87	processes have been designed by combining several technologies applied at lower
88	intensities, but with equivalent or even higher degrees of stability and safety. Today
89	some combinations with UV light have been explored with pasteurization purposes. It
90	has been demonstrated that UV light followed by pulsed electric fields (PEF) treatments
91	have an additive effect (Gachovska, 2008; Noci et al., 2008). Also Walkling-Ribeiro
92	(2008) found an additive effect when processing apple juice by a hurdle sequence
93	including UV light, pre-heating, and PEF. More promising is the combination of UV,
94	laser, and microwave radiation or conventional heating applied successively, because
95	they act synergistically (Maktabi et al., 2011). The simultaneous application of heat at

96	sublethal temperatures and non-thermal technologies, such as high hydrostatic
97	pressures, ultrasounds, and PEF have been thoroughly investigated (Raso and Barbosa-
98	Canovas, 2003). Surprisingly there are very scarce data in literature about the lethal
99	effect of UV light at midrange temperatures. Previously, Geveke et al. (2008) indicated
100	the improvement of UV lethal effect at mid-temperatures (40-50 °C) in liquid egg white.
101	Ukuku and Geveke (2010) investigated a combined treatment of UV light and radio
102	frequency electric field for the inactivation of E. coli in apple juice. From their results it
103	could be deduced that the inactivating effect of UV light increased with temperature in
104	the range of 20 to 40 °C. More recently, Gayán et al. (2011) demonstrated that the
105	temperature barely changed the UV resistance of <i>E. coli</i> up to 50.0 °C. Above this
106	threshold value inactivation rates due to the combined process synergistically increased
107	up to 60.0 °C. This data, obtained in laboratory media, suggested the possibility of
108	design-combined processes for the pasteurization of fruit juices with high absorption
109	coefficients.
110	The objective of this investigation was 1) to determinate the lethal effect of UV-C
111	treatments at mild temperatures on the UV-C resistant E. coli STCC 4201 strain
112	suspended in sterilized orange juice; 2) to establish the optimum temperature for the
113	combined process; and 3) to evaluate the effect of the optimized treatments on a cocktail
114	of five strains of <i>E. coli</i> on fresh squeezed orange juice and on the quality of the juice.
115	Orange juice was selected as treatment media because of its high absorption coefficient.
116	
117	2. Materials and methods
118	2.1. Bacterial culture and media

The strains of *E. coli* STCC 4201 and STCC 471 were provided by the Spanish Type
Culture Collection (STCC). The strain of *E. coli* ATCC 25922 and ATCC 27325 was

- 121 provided by the American Type Culture Collection (ATCC). The strain *E. coli* O157:H7
- used in this investigation is a VTEC- (Phage type 34) isolated by Dr. Chapman
- 123 (Chapman et al., 1993). The bacterial cultures were frozen at -80 °C in cryovials.
- 124 Stationary-phase cultures were prepared by inoculating 10 mL of tryptone soy broth
- 125 (Biolife, Milan, Italy) supplemented with 0.6% (w/v) yeast extract (Biolife) (TSBYE)
- 126 with a loopful of growth from tryptone soy agar (Biolife) supplemented with 0.6%
- 127 (w/v) yeast extract (TSAYE). The precultures were incubated at 35 °C for 6 h, in a
- shaking incubator. 50 μ L of the precultures were inoculated into 50 mL of fresh TSBYE
- and incubated for 24 h under the same conditions, which resulted in stationary-phase
- 130 cultures containing approximately 2×10^9 CFU/mL.

131 **2.2. Treatment media**

- 132 To determinate the lethal effect of UV-C treatments at mild temperatures on *E. coli*
- 133 STCC 4201, and to establish the optimum temperature for the combined process,
- 134 commercial sterilized orange juice was used as treatment media. The effect of the
- optimized treatments on a cocktail of five strains of *E. coli* and on the quality of the
- 136 juice was evaluated with fresh squeezed orange juice.
- 137 Sterilized orange juice (García Carrion S.A., Spain) was purchased from a local market.
- 138 It showed an absorption coefficient of 81.10 cm^{-1} , and a turbidity of 4,460 nefelometric
- 139 turbidity units (NTU). Fresh squeezed orange juice was prepared by squeezing (Zumex,
- 140 versatile 230 V, Valencia, Spain) Valencia variety orange fruits, and filtering the juice
- 141 through a stainless filter with net square holes of 1 mm². The filtered juice showed an
- absorption coefficient of 51.52 cm^{-1} and a turbidity of 3,075 NTU)
- 143
- 144
- 145

146 2.3. UV treatments

147	UV treatments were carried out in the equipment previously described (Gayán et al.,
148	2011). The whole system consisted of eight individual annular thin film flow-through
149	reactors connected sequentially. Each reactor included a low pressure UV lamp (TUV
150	8WT5, Philips, U.S.A.) with a length of 282.3 mm and 8 W of total power, emitting
151	90% of energy at a wavelength of 254 nm, fixed at the axis of an outer glass tube (25
152	mm of inner diameter) and enclosed by a quartz tube (20 mm of outer diameter) to
153	prevent direct contact of the lamp with the treatment medium. In the annular gap (2.5
154	mm) a stainless steel coil spring was installed to improve the turbulence of the flow.
155	Outside and inside coil diameters of the spring were 23 and 25 mm, respectively, and its
156	length and pitch were 270 mm and 10 mm, respectively. The equipment also included a
157	feed tank, a peristaltic pump (Ismatec, mod. ISM 10785, Glattbrugg, Switzerland), a
158	heating/cooling coil exchanger and extraction valves at the outlet of each reactor. The
159	circuit and reactors were submerged in a 90 L water bath heated at different
160	temperatures (25, 40, 50, 52.5, 55, 57.5 or 60 °C) by the circulating water of a
161	peripheral thermostatic bath (Huber, mod. Kattebad K12, Offenburg, Germany). Two
162	thermocouples (Almemo, mod. ZA 020-FS, Bernburg, Germany) fitted to the input of
163	the first and the outlet of the last reactor allowed the control of the treatment medium
164	temperature.
165	The applied doses were calculated dividing the radiant power (W) by the flow rate (Q)
166	as it has been previously described (Geveke 2005; Keyser et al. 2008). The flow rate
167	was kept constant at 8.5 L/h. Previous experiments demonstrated that above this value,
168	the efficacy of the treatments was hardly affected by the flow rate (Gayán et al., 2011).

- 169 With this flow rate the mean residence time in the equipment was 3.6 min. When heat
- and UV treatments were compared, the UV treatment times were calculated dividing the

171	mean residence time (3.6 min.) by 8 (number of reactors) and multiplying by the
172	number of reactors that the sample goes through before it was removed. The UV applied
173	dose at the outlet of successive reactors was: 3.4, 6.8, 10.2, 13.5, 16.9, 20.3, 23.7 and
174	27.1 J/mL respectively.
175	The medium to be treated was added with the bacterial suspension to achieve 10^7 - 10^8
176	CFU/mL and pumped through the heat exchanger to the reactors. When the treatment
177	conditions were stabilized, samples were withdrawn through the sampling valves at the
178	outlet of each reactor and 0.1 mL or 1 mL was immediately pour plated in the recovery
179	media.
180	
181	2.4 Heat treatments
182	Heat treatments were carried out in a specially designed resistometer (Condón et al.,
183	1993). The thermoresistometer TR-SC is a mixing method designed for studying heat
184	inactivation kinetics by the multipoint method. Briefly, the instrument consists of a 400
185	mL vessel provided with an electrical heater for thermostation, an agitation device to
186	ensure inocula distribution and temperature homogeneity, and ports for injecting the
187	microbial suspension and for the extraction of samples. 350 mL of orange juice were
188	placed in the vessel of the TR-SC and heating was turned on. Once the juice reached the
189	preset temperature (T±0.05 °C) (56, 58, 60 and 62 °C), it was inoculated with 0.2 mL of
190	an adequately diluted microbial cell suspension. After inoculation, 0.2 mL samples were
191	collected at different heating times and immediately pour plated. Before inoculation
192	bacterial cells were pre-adapted to the heating media by suspending 0.1 mL of grown
193	culture into 0.9 mL of orange juice and incubating for 15 min at 20 °C. Previous

194 experiments demonstrated that longer incubation times did not modify *E. coli* heat

resistance (data not shown). All determinations were performed at least three times onindependent working days.

197

198	2.5 Incubation of treated samples and survival counting
199	Tryptone Soy Agar (Biolife) supplemented with 0.6% of yeast extract (TSAYE) was
200	used as recovery medium. Samples of 0.1 and 1 mL were pour-plated in TSAYE and
201	then incubated for 24 h at 35 °C. Longer incubation times did not change the profile of
202	survival curves. After incubation, colony forming units (CFU) were counted with an
203	improved Image Analyzer Automatic Colony Counter (Protos, Synoptics, Cambridge,
204	UK), as described elsewhere (Condón et al., 1987).
205	
206	2.6 Resistance parameters
207	Survival curves to UV-C treatments were obtained by plotting the logarithm of the
208	survival fraction versus applied doses, expressed in J/mL, and to heat versus treatment
209	times in min.To fit survival curves and to calculate resistance parameters the Geeraerd
210	and Van Impe inactivation model-fitting tool (GInaFiT) was used (Geeraerd et al.,
211	2005). As survival curves obtained in this investigation did not show tails but rather
212	shoulders, the log linear regression plus shoulder model (Geeraerd et al., 2000) was
213	used with the equation:
214	$N(d) = N(0), e^{-ktmaxSI} \cdot \left(\frac{e^{ktmaxSI}}{1 + (e^{-ktmaxSI} - 1)e^{ktmaxSI}}\right) $ (1)
215	Where $N(d)$ represents the number of survivors, $N(0)$ the initial count, d the applied

dose for UV and time for heat treatments, Sl the shoulder leght and K_{max} the first order inactivation constant.

This model describes the survival curves through two parameters: the shoulder length (Sl) or dose before the exponential inactivation begins and the inactivation rate (K_{max}) ,

220	defined as the slope of the exponential portion of the survival curve. Therefore, the
221	traditional decimal reduction time value (D) can be calculated from the K_{max} parameter
222	by the equation: $D=2.303/K_{max}$. Thermal death time curves were obtained by plotting
223	the Log ₁₀ 4D values vs treatment temperatures, and z values(°C increase to 4D values
224	decrease ten times) were calculated from the slope of the regression line. Statistical
225	analyses (ANOVA and Student's t-tests) were carried out with the GraphPad PRISM®
226	software (GraphPad Software, Inc., San Diego, Calif., U.S.A.). Error bars in figures
227	correspond to the mean standard deviation.
228	2.7 Analytical measurements
229	2.7.1 Absorption coefficient, turbidity, pH, and °Brix
230	Absorbance of orange juice was measured at 254 nm using a Unicam UV500
231	spectrophotometer (Unicam Limited, Cambridge, UK). Sample solutions were diluted
232	and evaluated using quartz cuvettes (Hellma, Müllheim, Germany) with path lengths of
233	1, 2, and 10 mm. The absorption coefficient of the sample solution was determined by
234	the slope of the absorbance vs. path length correcting the dilution factor.
235	Turbidity was measured using a HI 83749 nephelometer (Hanna Instrument, Szeged,
236	Hungary). The instrument automatically provides the nephelometric turbidity units
237	(NTU) from lectures of scattered (90°) and transmitted light (180°) detectors with a
238	sample of 10 mL. Measurements were carried out following manufacturer's
239	instructions.
240	The pH measurements of orange juice $(20 \pm 1 \text{ °C})$ were performed with a pH meter
241	(Basic 20 pH meter; Crison Instrument, Barcelona, Spain) with a glass electrode
242	(Crison) and calibrated before measurement at pH 4 and 7.
243	The °Brix of centrifuged samples of orange juice (10 min at 360*g) was measured by a
244	digital hand-held refractometer at 20 ± 1 °C (PR-101, Atago, Tokyo, Japan).

245	
246	2.7.2 Color measurement
247	Color measurements were carried out as described by Martínez Verdú (2001). For
248	image acquisition, an HP G 4010 Scanjet scanner was used and the images were
249	processed using Matrox Inspector 8.0 [®] software (Stuttgart, Germany). Color calibration
250	was carried out with the HP scanner/Matrox combination, using the 300 Natural Color
251	System (NCS), which make up the Spanish Color Norm (UNE 48-103-94), and CIE
252	1976 (L^* , a^* , b^*) color space (CIELAB) was performed. The redness (a^*), yellowness
253	(<i>b</i> *) and lightness (<i>L</i> *) were measured in triplicate. Color difference (ΔE) was
254	calculated from L^* , a^* , b^* parameters, using Hunter-Scotfield's equation:
255	$\Delta E_{ab} = \sqrt[4]{(\Delta L)^2 + (\Delta a)^2 + (\Delta b)^2} $ ⁽²⁾
256	Where $a=a-a_0$, $b=b-b_0$ and $L=L-L_0$. The subscript ' ₀ ' indicates initial color, and the y-
257	intercept of linear regression models was taken for this number. Depending on the value
258	of ΔE the development in color difference with treatment could be estimated as not
259	noticeable (0-0.5), slightly noticeable (0.5-1.5), noticeable (1.5-3.0), well visible (3.0-
260	6.0), and greatly different (6.0-12.0) (Walkling-Ribeiro et al.; 2009)
261	
262	2.7.3 Pectinmethylesterase Analysis
263	The Pectinmethylesterase (PME) activity in the orange juice was determined, as
264	described by Kimball (1999), by monitoring the release of acid during pectin hydrolysis
265	as a function of time at pH 7.75 and 20 ± 1 °C. The reaction mixture consisted of 5 mL
266	orange juice sample and 100 mL of a 1% (w/v) citric pectin solution (Sigma-Aldrich,
267	St. Louis, USA) containing 0.15 M NaCl (Panreac, Barcelona, Spain). After mixing

- components, the pH was quickly adjusted to pH 7.75 and the pH was maintained
- constant by addition of 0.01 M NaOH. The enzyme activity was related directly to the

 \leq

- amount of NaOH added per minute. One PME unit (PMEU) was defined as the number
- of mL 0.01 M NaOH needed per minute to maintain constancy of the initial pH (Eq. 3).
- 272 The relative *PME* activity was calculated according Eq. 4 (Kimball, 1999). The PME
- activity of each sample was measured in triplicate.

- 275 Relative PME activity (%) = PMEV of treated juice PMEV of untreated x 1
- 276
- 277 2.7.4 Ascorbic Acid Retention

Ascorbic acid (AA) content was measured using AOAC's official 2, 6-dichloindophenol

titration procedure (AOAC, 1990b). To summarize, 10 mL of orange juice was mixed

with 50 mL of 5% acetic acid (Panreac, Barcelona, Spain) as a stabilizing agent and

diluted to 100 mL. The mixture was titrated with 2, 6-dichloindophenol solution until a

- faint pink color appeared and persisted for 15 s. The AA content of the samples were
- calculated by interpolation in a calibration curve previously obtained with several

solutions of pure AA (AnalaR Normapur, Leuven, Belgium) in 5% acetic acid solution.

285 *AA* retention of treated samples was calculated using the equation:

286 Relative AA (%) =
$$\frac{(AA \text{ treated sample})}{(AA \text{ untreated sample})} x 100$$
 (5)

287

288 2.7.5 Acidity determination

The acidity (*A%*) of treated and untreated orange juice was determined following the official method described by AOAC (1990a). This is a titration method that use phenolphthalein as indicator. In brief, two mL of orange juice were titrated with 0.1 N NaOH solution until the point when the indicator changed from colorless to pink and

- the change persisted for 15 s. Results were expressed as citric acid concentration in 100
- mL of orange juice, so that 1 mL 0.1 N NaOH is equivalent to 0.0064 g citric acid.

$$295 \qquad A\% = \frac{ml \, NaQH \times 0.0064 \times 100 \, ml \, orange \, juice}{2 \, ml \, sample}$$

(6)

- All analytical assays were performed in triplicate.
- 297

298 **3 Results and discussion**

- In this investigation, the lethal effect of UV radiation, for different times at several
- temperatures, on *E. coli* STCC 4201 suspended in sterilized commercial orange juice
- 301 was determined. For comparison purposes, heat resistance of this strain was also
- 302 performed in the same media. Survival curves of the UV-mild temperatures combined
- process (UV-H) were fitted with Geeraerd et al.'s model to estimate UV resistance
- 304 parameters. From data obtained with the model the process parameters for the
- pasteurization of orange juice was optimized. The effect of this treatment on a pool of
- five strains of *E. coli* as well as on the content of *AA*, *PME* activity, and other
- 307 physicochemical characteristics were evaluated in fresh squeezed orange juice.
- 308

309 **3.1. UV and heat resistance of** *E. coli* **in orange juice**

310 The *E. coli* strain STCC 4201 was used to evaluate the UV, heat and the combined

- treatment (UV-H) in sterilized commercial orange juice since it was the most UV
- 312 resistant strain of the five *E. coli* strains previously studied (Gayán et al., 2011).
- 313 Survival curves were constructed by drawing the survival fractions *versus* the applied
- dose. Traditionally UV dose is expressed as the energy supplied per unit area
- multiplying the irradiance (W/cm^2) by the exposure time. In continuous flow reactors it
- 316 can also be expressed in volume units (J/mL). The latter approach is useful to directly
- compare the energetic efficiency of the process with other technologies (Geveke, 2005;

318	Müller et al., 2011). Figure 1 shows the survival curves of <i>E. coli</i> STCC 4201 treated by
319	UV light at different temperatures. As shown in the figure, some survival curves did not
320	follow a logarithmic order of death. Some authors concluded from their work that the
321	number of survivors of UV light treatment may be an exponential function of time
322	(Franz et al., 2009; Oteiza et al., 2010), but many published survival curves to UV light
323	present shoulder and tails (Quintero-Ramos et al., 2004; Unluturk et al., 2010). In this
324	investigation concave downward survival curves were obtained. Also other authors
325	(Hoyer, 1998; Tran and Farid, 2004) have observed no microbial inactivation at low UV
326	doses followed by a normal log-linear relationship at higher UV doses. These shoulders
327	have been related to damage and repair phenomena (Koutchma, 2009). DNA absorbs
328	UV light photons resulting in cross-linking between the neighboring pyrimidine
329	nucleoside bases (thymine and cytosine) in the same DNA strand and thereby causing
330	delay of reproduction or cell death (Bachmann, 1975; Sizer and Balasubramaniam,
331	1999). However, the damage occurring at the DNA level can be repaired up to a level if
332	the recovery conditions are adequate (Liltved and Landfald, 1996). In a previous work
333	(Gayan et al., 2011), it was demonstrated that the shoulder of survival curves of this
334	strain increased when a photoreactivation step was included previous to culture of
335	survivors.
336	There are several mathematical approaches to describe non-linear inactivation kinetics
337	(Mafart et al., 2002; Peleg and Cole, 1998). In this investigation the Log-linear
338	regression plus shoulder model (Geeraerd et al., 2000) was used because it allowed
339	describing independently the shoulders and the Log-linear section of inactivation. The
340	fitting of the survival curves was carried out with the GInaFiT model-fitting tool
341	(Geeraerd et al., 2005) that automatically provides the resistance parameters as well as
342	the treatment time needed to inactivate 99.99% of the initial cell population (4D

343	parameter). The use of the Log-linear plus shoulder model allowed to directly compare
344	results with others previously published (Gayán et al., 2011). Table 1 shows the
345	averages and standard deviations of the UV light resistance parameters calculated with
346	Geeraerd et al.'s model for <i>E. coli</i> STCC 4201 suspended in sterilized orange juice and
347	treated at different temperatures. Table 1 includes the coefficient of determination (R^2)
348	and the root mean square error (RMSE) values from the fitting, the rate of the log phase
349	inactivation (K_{max}), the shoulder length (Sl) and, for comparison purposes, the 4D
350	parameter. As observed in Table 1, shoulder lengths of survival curves decreased as
351	increasing treatment temperature. Some authors had correlated the shoulders with the
352	damage repair mechanisms (Koutchma, 2009). Therefore results would indicate that
353	damage repair capability of UV treated cells would be lower as treatment temperature
354	increases, or that DNA damages are greater at higher temperatures. On the contrary, the
355	inaction rate (K_{max}) increased with temperature. In summary, the overall lethal effect of
356	UV light treatments drastically increased with temperature. Whereas the highest UV
357	dose possible to apply with the equipment (27.10 J/mL) hardly decreases 0.64±0.04
358	Log ₁₀ cycles the population of <i>E. coli</i> STCC 4201 at 25.0 °C, the same doses allowed
359	achieving more than 6 Log cycles of inactivation at 55.0 °C (Figure 1). In other words, a
360	treatment of 13.55 J/mL reached 0.25±0.04, 0.41±0.13, 0.84±0.32, 0.96±0.12,
361	2.57 ± 0.05 , 3.41 ± 0.23 and more than 6 Log_{10} cycles of inactivation at 25.0, 40.0, 50.0,
362	52.5, 55.0, 57.5, and 60.0 °C, respectively (Figure 1). There are few data in literature
363	about the microbial UV resistance in orange juice, probably due to its high absorption
364	coefficient. Koutchma et al. (2007) achieved at room temperature 3.1 ± 0.06 Log ₁₀ cycles
365	of <i>E. coli</i> inactivation in a model juice solution with a similar absorption coefficient
366	than orange juice (48 cm ⁻¹) after 3 passes (12.38 J/mL) in a UV coiled tube reactor
367	under turbulent conditions. These results are far from the 5 Log_{10} cycles of inactivation

368 required by the Food and Drug Administration (FDA) juice production regulation

369 (Anonymous, 2001).

370	The improvement of UV lethal effect at mild temperatures has been previously shown
371	by Geveke (2008) in liquid egg white. The population of <i>E. coli</i> in egg white was
372	reduced by $1.63\pm0.10 \text{ Log}_{10}$ cycles at a temperature of 30 °C, whereas 2.32 ± 0.07 and
373	2.48 ± 0.41 Log ₁₀ reductions were achieved when the temperature was raised to 40 and

- 50 °C respectively, with a UV processing energy of 44 J/mL. Ukuku and Geveke (2010)
- developed a combined treatment of UV light and radio frequency electric field (20-40
- ^oC) for the inactivation of *E. coli* in apple juice, showing that UV light treatment
- reached 5.8 Log₁₀ reductions, while the combined treatment allowed to achieve 6.2

 Log_{10} reductions. These results are in agreement with those observations, although the

379 direct comparisons of data are risky because the treatment medium and the equipment

used strongly determine the results (Koutchma et al., 2004).

381 To differentiate the contribution of heat to the whole lethal effect, the thermal resistance

of *E. coli* STCC 4201 in orange juice was also determinate. Survival curves were fitted

with the Geeraerd et al.'s model (2000) and heat resistance parameters were calculated.

Table 2 shows the averages and standard deviation of the inactivation rate (K_{max}), the

shoulder length (*Sl*), and the 4D parameter. In a further step it was compared the

inactivation parameters for UV light and for thermal treatments at different

387 temperatures. Figure 2 shows the relationship between 4D parameter and the treatment

388 temperature for both treatments. For UV-H treatments, a concave downward profile was

- obtained which means that the lethality of UV light hardly changed below 40 °C, and
- above this threshold quickly decreased with temperature. For heat treatments, an
- exponential relationship between 4D values and temperature was found (Log

4D=0.221T-11.52, $R^2=0.995$) as expected. From this thermal death time curve, a z

value of 4.51 ± 0.23 °C was deduced. Therefore, an increase in temperature of	ot 4.5	1 '	Ϋ́C
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was necessary to reduce the 4D value by ten times. Similarly, Mazzotta et al. (2001) 394

395 determined an average z value of 4.8 °C for E. coli O157:H7 in orange juice.

396

417

3.2. Lethal effect of the UV-H combined treatments 397

In order to determine whether lethal effect of the combined UV-H treatments were due 398 399 to an additive (the lethality of the combined process was the sum of the inactivation rates of heat and UV light treatments acting simultaneously but individually) or to a 400 401 synergistic effect (the lethality of the combined process was higher than the sum of 402 lethality of individual treatments), survival curves to UV at room temperature, to heat 403 and to the UV-H treatments at the same temperature were compared (Figure 3). As it is shown, while UV at room temperature and thermal inactivation at 50.0 °C, 52.5 °C, and 404 55.0 °C for 3.6 min was negligible (0.05, 0.08, and 0.61 Log₁₀ cycles, respectively), the 405 UV-H at the same temperatures, reduced 2.16, 3.01, and more than 6 Log₁₀ cycles, 406 respectively. This demonstrated a synergistic effect of both technologies acting 407 simultaneously. Above 55.0 °C, the lethality of thermal treatments exponentially 408 increased with temperature and differences among survival curves to heat and the 409 combined process tended to disappear. This phenomenon can be clearly observed in 410 Figure 2. From these results, it was concluded that the lethality of the combined process 411 was the result of a synergistic effect which magnitude was thermodependant among 412 413 50.0-60.0 °C. Therefore, it was necessary to optimise the treatment temperature to take 414 full advantage of the combined process. 415 For the optimization of the combined treatment, percent synergism for each temperature 416 was calculated comparing the experimental and the theoretical 4D values, with the equation:

- 419 Theoretical 4D values were calculated, by assuming an additive effect, with the
- 420 equation proposed by Raso et al. (1998):

421 Theorical
$$4D_{UV-H} = \frac{(4D_H \times 4D_{UV})}{(4D_H + 4D_{UV})}$$

422 where $4D_{H}$, and $4D_{UV}$ values were obtained from the fit of the inactivation curves for

423 the thermal and UV light treatments, respectively.

424 The magnitude of the synergism at different temperatures can be observed in Figure 4.

As it is demonstrated by the figure, the synergism increased with temperature up to 55.0

- 426 °C (68.03%) decreasing further away.
- 427

428 3.3. Effect of optimized UV-H treatment in fresh squeezed orange juice

429 Several authors have reported significant differences in UV resistance between *E. coli*

430 strains in water systems (Sommer et al., 2000), laboratory media (Gayán et al., 2011)

and fruit juices (Basaran et al., 2004; Oteiza et al., 2010). Therefore, the use of a single

432 strain for the determination of a specific dose for a given log reduction is risky (Oteiza

433 et al.; 2010). The Scientific Advisory Panel of the Environmental Protection Agency

434 (EPA) specifically recommended the testing of five outbreak-related strains in a cocktail

435 for each pathogen (Anonymous, 1997). Therefore, the lethal effect of UV-H treatment

436 on a cocktail of five *E. coli* strains (*E. coli* STCC 4201, STCC 471, ATCC 27325,

ATCC 25922, and O157:H7) inoculated in fresh squeezed orange juice was performed
to validate the designed combined treatment. Figure 5 shows the survival curves of the
cocktail in fresh squeezed orange juice treated by UV-H at 55.0 °C. Survival curves of *E. coli* STCC 4201 in commercial orange juice have also been included for comparison
purposes. As observed, both curves overlapped each other and no statistically

significant differences (p > 0.05) were found between both Sl (2.4 J/mL) and K_{max} (0.6

18

(8)

mL/J) values. Overall results demonstrated that a UV treatment of 23.72 J/mL at 55.0 443 °C allowed reaching more than 5 Log₁₀ cycles of inactivation of the *E. coli* cocktail in 444 445 fresh squeezed orange juice. The loss of juice quality and nutritional properties during the processing has become an 446 important issue due to the increase consumer's demand for fresh food products. 447 Therefore the impact of UV-H combined treatment at 55.0 °C on physico-chemical 448 449 properties (*pH*, ^oBrix, ^oA, ΔE), AA content, and PME activity of natural orange juice was evaluated. For this purpose, measurements were carried out in untreated samples as 450 451 controls and thermal and UV-H treated fresh squeezed orange juice. Thermal treatments were performed in the same installation tempered at 55.0 °C with off UV lamps. Results 452 453 are included in Table 3. Statistical analysis of the results demonstrated that there were no significant differences 454 (p > 0.05) between pH, "Brix, and %A values of the three samples. The total color 455 differences (ΔE) of treated samples with the control were 0.23 and 0.07, which were 456 considered to be "not noticeable" changes according to Walkling-Ribeiro et al. (2009). 457 Regarding AA loss, the results showed that AA was degraded $16.45\pm0.77\%$ with the UV-458 H treatment. This loss is believed to be mainly due to UV light because no AA 459 destruction was reported in the heat treatment (Table 3). Furthermore the effect of air 460 oxidation of AA was measured passing orange juice through the installation at 25.0 $^{\circ}$ C 461 with off UV light lamps and it was observed that the AA destruction due to air oxidation 462 463 was negligible (data not shown). UV light is known to generate free radicals through a 464 wide variety of photochemical reactions, which can damage vitamins (Koutchma, 465 2009a). Overall, the percentage of degradation by the combined process was similar to 466 those observed by other authors after UV light at room temperature treatments (Torkamani and Niakousari, 2011; Tran and Farid, 2004). 467

468	The percentage of <i>PME</i> inactivation by the combined and the thermal treatment were
469	63.96±5.07% and 47.84±9.15%, respectively. These values suggested that enzyme
470	inactivation was mainly due to heat. There are few studies about the effect of UV
471	radiation on <i>PME</i> enzyme. Tran et al. (2004) obtained an inactivation of 5% when juice
472	was treated with 73.8 mJ/cm ² , and Torkamani and Niakousari (2011) an inactivation of
473	the 8% with the same UV dose. The loss of <i>PME</i> activity by the proposed UV-H
474	process was lower than if reached by the traditional thermal sterilization processes (90
475	°C for 60 sec), that usually pursue the 99.9% loss of PME activity (Eagerman, 1976),
476	but it is similar to industrial conditions for heat pasteurization of premium juices (70 °C
477	for 2 sec) which reduced by 70 % the enzyme activity (Tran and Farid, 2004).
478	Timmermans et al. (2011) demonstrated that thermal treatments at 72 °C for 20 sec,
479	ultrahigh pressure treatments at 600 MPa for 1 min and high electric field pulses of 76
480	J/mL at 23 kV/cm reached PME inactivation levels in freshly squeezed orange juice of
481	85%, 92% and 34% respectively. Therefore the combined process of UV light at mild
482	temperatures could be a realistic alternative to traditional thermal and proposed non-
483	thermal methods for pasteurization of orange juice.
484	

485 **4.** Conclusions

486 UV light is a promising technology for the pasteurization of liquid foods. However, the 487 high absorption coefficient of some of them can impair its industrial application. The 488 combination of UV light and mild temperatures synergistically increases the efficacy of 489 the treatment for the inactivation of *E. coli* in orange juice. A UV treatment of 27.10 490 J/mL at 55.0 °C allowed reaching more than five Log₁₀ reductions of a cocktail of five 491 strains of *E. coli*. The treatment does not change the physico-chemical properties or the

492	juice colour. The loss of ascorbic acid was similar to juice UV treated at room
493	temperature (16.45%), but the decrease of PME activity was much higher (63.96%).
494	
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Figure 1



















Figure captions

Colin

Figure 1. Survival curves of *E. coli* STCC 4201 in commercial orange juice treated by UV light at different temperatures: 25.0 °C (\bullet), 40.0 °C (\blacksquare), 50.0 °C (\blacktriangle), 52.5 °C (×), 55.0 °C (\bigcirc), 57.5 °C (\square) and 60.0 °C (Δ).

Figure 2. Relationship between temperature and *4D* parameter in commercial orange juice for *E. coli* STCC 4201 inactivation by heat (min) (\blacksquare) and the combined UV-H treatment (J/mL) (\bullet).

Figure 3. Survival curves in commercial orange juice of *E. coli* STCC 4201 treated by UV light at room temperature (\blacksquare), heat (\bullet) and the combined UV-H process (\blacktriangle) at 50.0, 52.5, 55.0, 57.5 and 60.0 °C.

Figure 4. Synergistic effect of the combined UV-H treatments at different temperatures. **Figure 5.** Survival curves of *E. coli* STCC 4201 in commercial orange juice (\bullet) and of a *E. coli* strain cocktail (\blacktriangle) in natural orange juice treated by UV light at 55.0 °C.

Table 1. UV resistance parameters (*Sl, Kmax* and *4D*) at middle temperatures of *E. coli*

 STCC 4201 in commercial orange juice.

				-	
Temperature (°C)	Sl (J/mL)	Kmax (mL/J)	Dose for 4D reductions (I/mL)	R^2	RMSE
25.0	8.24 (2.58)	0.07 (0.01)	-	0.991	0.025
40.0	6.92 (1.29)	0.07 (0.03)	-	0.984	0.036
50.0	3.99 (0.60)	0.21 (0.01)	-	0.991	0.082
52.5	3.69 (0.46)	0.30 (0.03)		0.975	0.187
55.0	2.39 (0.31)	0.61 (0.12)	16.99 (0.25)	0.980	0.401
57.5	1.79 (0.75)	0.91 (0.08)	12.21 (1.06)	0.989	0.194
60.0	0.48 (0.42)	1.72 (0.19)	6.54 (0.22)	0.974	0.374

Table 1

Table 2. Heat resistance parameters (*Sl*, *Kmax* and *4D*) of *E. coli* STCC 4201in commercial orange juice at different temperatures.

T					
Temperature (°C)	Sl (min)	Kmax (min ⁻¹)	Dose for 4D reductions (min)	R^2	RMSE
56.0	0.23 (0.13)	0.94 (0.08)	9.63 (0.63)	0.997	0.019
58.0	0.15 (0.30)	1.43 (0.14)	6.51 (0.86)	0.988	0.035
60.0	0.13 (0.10)	10.61(0.84)	0.97 (0.23)	0.978	0.298
62.0	0.04 (0.07)	20.81 (2.12)	0.48 (0.09)	0.971	0.473

Table 3. Physico-chemical properties -pH, °Brix, acidity (%A), and colour (ΔE)-, ascorbic acid content (AA) and pectin methyl esterase activity (*PMEU*) of untreated (*control*), heat (55.0 °C) and UV-55.0 °C (*UV-H*) treated fresh squeezed orange juice.

	pH	° Brix	%A	ΔΕ	mg AA/100 mL	% AA loss	PMEU	% PME inactivation
Control	2.83 (0.04)	10.1 (0.10)	1.074 (0.051)		52.45 (1.79)		0.124 (0.018)	
Н	2.83 (0.04)	9.86 (0.11)	1.030 (0.037)	0.23	52.84 (0.68)	0	0.035 (0.006)	47.84 (9.15)
UV-H	2.86 (0.03)	9.83 (0.35)	0.975 (0.018)	0.07	43.81 (1.17)	16.45 (0.77)	0.019 (0.083)	63.96 (5.07)

- 656 Our reference: JFOE 7025
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- To be published in: Journal of Food Engineering

- 659 660
- 661 Highlights
- 662
- 663 The lethality of UV on *E. coli* suspended in orange juice increased with temperature.
- The maximum synergistic effect of UV-H treatment was found at 55 °C.
- A UV-H treatment of 23.72 J/mL at. 55.0 °C inactivated more than 5 Log₁₀ cycles.
- 666 The treatment did not affect the pH, acidity, ^oBrix and color of orange juice.
- The UV-H decreased 16.45% ascorbic acid content and 81.27% the PME activity.

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