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# Exploring the efficacy of pulsed electric fields (PEF) in microbial inactivation during food processing: A deep dive into the microbial cellular and molecular mechanisms

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# ABSTRACT

Pulsed electric field (PEF) is a food processing technology based on the phenomenon of electroporation for the inactivation of microorganisms with main advantage the minimal effect on the quality (nutritional, functional, and sensorial) characteristics of the food products. Despite the plethora of research literature on PEF-processed food safety, PEF's industrial application as an alternative of classical pasteurization is limited and mainly at industrial level is focused on high acid-liquid food products. Thus, the thorough assessment of the antimicrobial efficiency of PEF, coupled with the meticulous identification of key microbial resistance mechanisms is scientifically imperative. These efforts are essential for refining the process and exploring potential enhancements through synergistic integration and combination with other methods or/and hurdles. On this basis this manuscript aims to critically review and summarise: a) the antimicrobial mechanism of action, b) the microbial inactivation efficiency, and c) the effect of PEF at a microbial genomic/transcriptomic level. *Industrial application:* Evaluating the effectiveness of inactivation and understanding the underlying resistance

*Industrial application:* Evaluating the effectiveness of inactivation and understanding the underlying resistance mechanisms can help on strategies to optimize PEF-mediated decontamination practices, and thereby enhancing the overall process efficiency.

## 1. Introduction

### 1.1. Mechanism of action; electroporation phenomenon and its effects

The underlying phenomenon to the application of an electric field to biological cells or tissues for the increase of membrane permeability is described as electroporation (or electropermeabilization) (Heinz et al., 2001; Wiktor et al., 2015). In general, the cell membrane is composed by lipids, which exhibit a structural duality with a polar (hydrophilic) head and a non-polar (hydrophobic) tail (Kotnik et al., 2012). These lipids are arranged into bilayer, where nonpolar tails align inward while polar heads face outward, interacting with the surrounding aqueous environment (Kotnik et al., 2012), After application of electric pulses,

electroporation phenomenon is initiated by the aqueous molecules into the lipid bilayer of the membrane (a biological structure formed by amphilic lipids) and leads to reorientation of the lipids with the polar head groups towards these aqueous molecules (Kotnik et al., 2015; Müller et al., 2022). The theory of the mechanism of electroporation is mainly based on the formation of hydrophilic pores, however recent studies have revealed that other factors may contribute to the increased membrane's permeability, such as chemical changes to the lipids and alteration of the membrane's protein functions (Breton & Mir, 2018; Kotnik et al., 2019).

The application of short electric pulses of high voltages for short duration to biological cells and tissues to enhance membrane permeability, is becoming a pertinent method in different applications

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including applications in food technological (Mahnič-Kalamiza et al., 2014), medicinal (Batista Napotnik et al., 2021) biotechnological and environmental processes (Kotnik et al., 2015). However, depending on the research field, those processes/techniques appear in the scientific literature with different terms, namely electroporation, electropermeabilization, electropulsation or Pulsed electric field (PEF) treatment, and are characterized by subtle differences (Kotnik et al., 2019). More specifically, whilst electroporation focuses on the formation of aqueous pores in the lipid bilayer caused by the induced transmembrane voltage, electropermeabilization examines membrane permeability for molecules lacking the physiological mechanisms of transmembrane transport, and electropulsation/PEF generally comprise cell exposure to electric pulses, leading to membrane structural alterations and increased conductivity and/or permeability (Kotnik et al., 2019). The application of an electric field to a biological cell can lead to three different outcomes depending on (i) the electric field strength, (ii) the duration of exposure, and (iii) the membrane recovery rate (Mahnič-Kalamiza & Miklavčič, 2022). In case the electric field strength and the duration of exposure are insufficient to achieve pore formation, electroporation is unachievable, and there is no effect on the cell's permeability and viability (Kotnik et al., 2012; Mahnič-Kalamiza & Miklavčič, 2022). On the condition that the electric field strength exceeds the critical threshold value of the potential difference across a membrane (transmembrane potential), typically between 0.5 and 1.5 V, repulsion between the charge-carrying molecules induces pore formation in the cell membrane (Barba et al., 2015; Weaver & Chizmadzhev, 1996). Depending on the selected parameters of PEF treatment, reversible or irreversible electroporation can occur, with the intensity of treatment determining whether the electroporation can cause temporary or permanent injuries for microbial cells.(Jaeger et al., 2009; Weaver & Chizmadzhev, 1996). When reversible, it causes the cell membrane to discharge (Mohamed & Amer Eissa, 2012) and facilitates microorganism injuries (Yun, Zeng, et al., 2016). In this case and, after a short exposure to an electric field, the membrane resealing and recover, ensuring the viability of the biological cell (Kotnik et al., 2012). Recovery of the cell is an active cellular process involving intricate cellular machinery after reversible electroporation (Batista Napotnik et al., 2021). The occurrence of irreversible pores following appropriate PEF applications leads to microbial cell death as a result of the release of intracellular substances due to the increased permeability of the membrane, structural membrane changes, and osmotic or swelling phenomena (Golberg et al., 2010; Min et al., 2007). For example, Yang et al. (2008) have demonstrated that the peptidoglycan layer of S. epidermis cells experienced changes after exposure to PEF. Additionally, Wang et al. (2016) have shown that in S. aureus (cultivated at 37 °C) cells, following a PEF treatment at an electric field strength of 39.0 kV/cm, a pulse frequency of 1.0 kHz, for a 1.6 ms treatment time, and a maximum thermal effect of <30 °C with the cells undergoing shape distortions, exhibiting more oval phenotypes.

### 1.2. PEF as pasteurization alternative

The demand for more sustainable food production methods and the growing consumer interest in fresher and more nutritious food products in combination with the advancement of human knowledge and technology progress, have facilitated the development of new food processing technologies for food preservation and safety, in replacement of the more classical food processing technologies like heating (Chacha et al., 2021; Golberg et al., 2010; Nowosad et al., 2021; Ortega-Rivas & Salmerón-Ochoa, 2014). The term, "non-thermal", was coined to describe those alternative-to-temperature-based-pasteurization methods (Chacha et al., 2021; Morales-de la Peña et al., 2019; Ortega-Rivas & Salmerón-Ochoa, 2014; Pereira & Vicente, 2010). "Non-thermal" technologies can utilize ultrasound (US), high hydrostatic pressure (HPP), ultraviolet light, pulsed electric fields (PEF), non-thermal /cold plasma (NTP), and ozone. They can be classified as physical (US), HPP),

UV, and PEF) or chemical (NTP, and ozone) (Chacha et al., 2021; Valdramidis & Koutsoumanis, 2016).

PEF, is described as one of the most promising technologies to inactivate microorganisms and achieve microbial inactivation equivalent with thermal treatments (Barba et al., 2015; Peng et al., 2020) with main advantages as a process being a) the lower treatment temperature, b) the shorter processing time, and c) the potential for its application in continuous flow treatments (Bhat et al., 2019). The PEF process is based on pulse intensities which vary from 0.5 to 1.5 kV/cm for the induction to stress responses and reversible electroporation and from 15 to 40 kV/cm intensities for microbial inactivation, and irreversible electroporation (Raso et al., 2016). Industrially, an electric field strength between (~ 10–20 kV/cm) has been employed as a prerequisite for PEF systems for the microbial inactivation to date (Toepfl, 2012). The exposure of microbial cells to a source of electrical field for a few microseconds is associated with structural changes of the cell membrane, ultimately leading to cell damage (Heinz et al., 2001; Roobab et al., 2018).

A variety of food products, from liquid or semi-liquid to solid, have been researched for microbial inactivation by PEF treatment (Abbas Sved, 2017). Most of the studies related to PEF process for microbial inactivation focus on the application of high voltage pulses to milk and dairy products, juices and a variety of liquids (Abbas Syed, 2017; Tanino et al., 2020). Depending on the type of the food product (liquid, semiliquid and solid), the effectiveness of different PEF systems can be explored, that of the batch or the continuous (Mohamed & Amer Eissa, 2012; Niu et al., 2020; Nowosad et al., 2021). The batch PEF systems are primarily opted for handling static volumes of solid or semi-solid foods (Mohamed & Amer Eissa, 2012), whereas the continuous treatment PEF systems have a potential for industrial processing of liquid and semiliquid foods, as they allow the continuous/steady flow of products (Niu et al., 2020). The first commercialized PEF system for fruit juices (apple, strawberry, and other flavors) preservation was used by Genesis Juices (Oregon, USA) in 2006 (Clark, 2006) while the first commercial PEF line for fruit juice preservation (1500 L/h) was reported in Europe back in 2009 (Siemer et al., 2014). According with Raso et al. (2016). The most common treatment chambers in use for continuous systems have their electrodes with parallel plate or colinear configuration. The parallel plate configuration is characterized by a large electrode surface and low intrinsic electrical resistance, with the main advantage the formation of a uniform electric field, but the limitation of creating electrode corrosion due its high current operation that may trigger undesired electrochemical phenomena. The colinear treatment chamber functions at lower current compared to the parallel plate configuration. It is known to be conducive, minimizing electrode reactions and enabling the parallel connection of multiple co-linear units from an electrical standpoint. Nevertheless, its main drawback lies in the uneven distribution of electric field strength and temperature within the treatment zone during PEF processing (Raso et al., 2016).

### 2. Microbial inactivation by PEF treatments

Food products harbour a variety of different microorganisms, several of which can be used in the food industry to drive fermentation processes. However, other food associated microbes can cause food spoilage and generate public health problems (Mosqueda-Melgar et al., 2008). Common food spoilage microorganisms include *Saccharomyces*, *Lactiplantibacillus, Leuconostoc, Brochothrix thermosphacta, Pseudomonas, Acinetobacter, Moraxella Penicillium, Cladosporium* spp. (Mermelstein, 2017) while common foodborne pathogens include *Salmonella, Campylobacter, Enterohaemorrhagic Escherichia coli, Listeria and Vibrio cholerae* (World Health Organization, 2020). Consequently, for the application of an effective PEF disinfection, and for safeguarding food stability and safety, the identification of PEF-resistant pathogenic and spoilage bacteria becomes pivotal (García, Gómez, Raso, et al., 2005). Over the last two decades, the impact of PEF on enzyme and microorganism inactivation, as well as on energy-saving has been heavily researched (Nowosad et al., 2021). Significant PEF-mediated microbial inactivation have been reported for several pathogenic bacteria including *Staphylococcus aureus*, *Yersinia entercolitica, Escherichia coli, Listeria monocytogenes* and *Salmonella Enteritidis,* as well as for spoilage microorganisms, such as *Acetobacter* spp., *Bacillus subtillis, Lactiplantibacillus plantarum*, and *Saccharomyces cerevisiae* (as shown in Table 1) (García, Gómez, Mañas, et al., 2005; Katiyo et al., 2017; Niu et al., 2019; Wang et al., 2018).

### 2.1. Processing parameters

The efficiency of decontamination by PEF technology is dependent on different factors. These can mainly be grouped under three different categories: processing conditions, characteristics of microbes, and product parameters (Abbas Syed, 2017; Roobab et al., 2018). The main process parameters for PEF treatments are: the electric field strength (E), the treatment time (*t*), the pulse shape, the pulse width ( $\tau$ ), the number of pulses (*n*), the pulse repetition frequency, and the total specific energy input (W) and (Raso et al., 2016). Different treatment conditions (E =12-50 kV/cm, 27-2000 µs) and a variety of food matrices are presented in this review (see Table 1). In general, changes in PEF processing conditions can impact the efficiency of microbial inactivation, with microbial inactivation generally increasing with higher electric field strength or longer treatment times (Wouters et al., 2001). However, an increase in the total specific energy causes an increase of the temperature in the treatment medium due to Joule's heating which is of great importance as heat sensitive compounds could be affected (Schottroff et al., 2019).

### 2.2. Microbial characteristics

The main microbial characteristics that play an important role in microbial inactivation by PEF are: the type of microorganism, the species, the strain and culture conditions (Raso et al., 2016). In a pilot study, Lee et al. (2015) have shown that PEF-treatments of low-fat milk with an electric field strength of 10 kV/cm, total specific energy input of 200 kJ/L and an inlet temperature of 30 °C enabled a 4.4-log10 CFU/mL, a 4.5-log<sub>10</sub> CFU/mL, and a 6.0-log<sub>10</sub> CFU/mL inactivation, for L. brevis, E. coli, and S. cerevisiae, respectively. Additionally, Huang et al. (2014) reported that PEF-treatment (24 kV/cm, 180 µs, inlet temperature of 30  $^{\circ}\text{C}$  and maximum temperature of 38.2  $\pm$  0.8  $^{\circ}\text{C}$ ) of grape juice resulted in a 2.69-log10 CFU/mL, a 3.6-log10 CFU/mL and a 6.01-log10 CFU/mL inactivation, for Staphylococcus aureus, E. coli, and S. cerevisiae, respectively. Consequently, the effectiveness of PEF disinfection is microbial species dependent (Niu et al., 2020) where in general the larger the cells the more susceptible are to the electrical fields (Heinz et al., 2014). Studies have also revealed that even different strains of the same bacterial species exhibit different sensitivities to the same PEF treatment (Raso et al., 2016). For example, Walter et al. (2016) showed that PEF treatment (35 kV/cm, 30 µs treatment time and an average temperature of 40 °C) of UHT whole-milk (4% fat), resulted in a  $> 2 \log_{10}$  CFU/mL for E. coli strains ATCC 11775 and FSAW 1325, whereas strains of O157:H7 Sakai and FSAW 1326 appeared more PEF-resistant (<1.5 log10 inactivation; *p* < 0.05).

Other important factors affecting the PEF treatment efficiency include the bacterial growth environment and growth stage of the cells (Liu et al., 2017). For example, Niu et al. (2019) have shown that ethanol has an effect on the cell membrane properties of *Acetobacter* sp., as under the same PEF treatment (20.0 kV/cm,6.0 ms and maximum temperature < 35 °C) the reduction of the cells cultured with 9% ( $\nu/\nu$ ) ethanol was higher (5.17-log<sub>10</sub>) than those without it (3.22-log<sub>10</sub>). Additionally, Álvarez et al. (2002) have shown that L. *monocytogenes* cells grown at 35 °C were more PEF-resistant than those grown at 4 °C, with PEF resistance increasing during the incubation time and reaching its maximum value at the stationary growth phase of the bacterium. More specifically, after PEF treatment (25 kV/cm800 µs and maximum temperature < 35 °C) for two suspensions (with an initial concentration

of 10<sup>8</sup> cells/mL) grown at 4 °C and 35 °C, their maximal resistance reduced by 2.0 and 1.2 log<sub>10</sub>, respectively (Álvarez et al., 2002). Additionally, Ohshima et al. (2002) have shown that the culture temperature influences the resistance against PEF treatment. More specifically it was identified that in the optimum culture temperature, i.e., 37 °C, E. coli was more resistant under PEF treatment in comparison to culture temperatures of 20 or 42 °C. The sensitivity of E. coli under PEF treatment after cultivation at 20 °C is associated with an increased content of unsaturated fatty acids in phospholipids, which induces cell membrane fragility, whereas cultivation at 42 °C initiates cell destruction cascades, following protein unfolding and activation of bacteria and activates the heat shock proteins (Ohshima et al., 2002). Yun, Liu, et al. (2016) reported that under the same PEF treatment (25 kV/cm,1.2 ms) and initial inactivation temperature of 25 °C, Salmonella Typhimurium cells reaching their stationary phase exhibited 3.30-log<sub>10</sub>, 2.48-log<sub>10</sub>, 1.99-log<sub>10</sub>, 1.86-log<sub>10</sub> and 1.63-log<sub>10</sub> reductions when grown at 10, 20, 30, 37 and 45 °C, respectively. Additionally, Wouters et al. (1999), showed that L. innocua cells grown into stationary phase were more resistant to PEF treatments than cells in their log-growth phase. This phenomenon may be attributed to either the heightened susceptibility of membrane areas involved in cell division, or the larger size of bacterial cells in the exponential phase, leading to decreased resistance to PEF. The resistance of microorganisms grown to their stationary phase may result from alterations in the expression of stress-related genes, instigated by the alternative sigma factor, as well as different metabolic, structural and morphological changes relative to the exponentially grown cells (Somolinos et al., 2008).

### 2.3. Treatment medium properties

Food product parameters that can influence the microbial inactivation efficiency are: the conductivity, and the water activity ( $a_w$ ) and the pH of the product (Abbas Syed, 2017; Chacha et al., 2021; García, Gómez, Raso, et al., 2005). The conductivity of the medium is related to the resistivity of the medium in a treatment chamber and influences current intensity that is needed for the generation of electric fields (Gachovska et al., 2013).

In a range of conductivities that do not influence the distribution of the electric field, lowering the conductivity increases the difference between the ionic concentration of the cytoplasm and the treatment medium and as a consequence leads to an increased flow of ions across the membrane. This phenomenon weakens the membrane and the membrane's resistance to pulses (Jayaram et al., 1993). Different studies have shown that the highest microbial inactivation was achieved at the lowest conductivity (Sensoy et al., 1997; Wouters et al., 1999). Although conductivity is considered a parameter that influences microbial inactivation, different researches have shown that there was no influence under the same total specific energy used (conductivities between from 0.05 up to 0.45 S/m) (Álvarez et al., 2003; Timmermans et al., 2019). Reduction of  $a_w$  has shown to increase the PEF resistance of microorganisms (Álvarez et al., 2002; Aronsson et al., 2001). Regarding the effect of the pH, media of pH 7.0 and 4.0 affected differently L. monocytogenes, with higher inactivation levels achieved at pH 4.0, suggesting that for specific microorganisms an acidic environment can be a hurdle (Saldaña et al., 2009). On the contrary, the opposite behavior was observed for PEF-treated E. coli with higher resistance at pH 4.0 than pH 7.0, indicating that different strategies need to be applied depending on the target microorganism (Saldaña et al., 2009). In another study, Jaeger et al. (2009) reported that the microbial inactivation of Lactiplantibacillus rhamnosus was influenced by increasing the protein content. However, this effect was not observed in L. innocua with increasing protein content under neutral pH condition (Schottroff et al., 2019), Thus, further research on a plethora of microorganisms related to the microbiota of each food matrix and the PEF equipment is important for optimization of the process with a final aim at achieving a 5-log microbial reduction minimum.

### Table 1

Summary of processing parameters and decontamination efficiency of different PEF treatments.

Microorganism	Product	Treatment conditions	Reduction	Reference
Gram-negative bacteria Escherichia coli	Green tea beverage	E: 38.4 kV/cm	5.6 log <sub>10</sub>	(Zhao et al., 2008)
(ATCC 8739)	pH: 6.0 at 20 °C	t: 160 µs		
	Conductivity:	τ: 2 μs		
	0.1 S/m at 20 °C	n: NS f: 667 pps		
		Energy input: $236 \times 10^3$ J/L		
		Inlet temperature: 20 °C		
		Maximum temperature: * NS		
		Pulse type: bipolar / square		
Escherichia coli	Soymilk	E: 40 kV/cm	5.2 log <sub>10</sub>	(Li et al., 2013)
(ATCC 8739)	pH: 7.22 $\pm$ 0.16 at 20 °C	t: 547 µs		
	Conductivity: $0.21 \pm 0.02$ S/m at 20 °C	$\tau: 2 \ \mu s$		
	$0.21 \pm 0.02$ 3/ in at 20 °C	f: 400 Hz		
		Energy input: * NS		
		Flow rate: 1 mL/s		
		Inlet temperature: 25 °C		
		Maximum temperature: $< 35$ °C		
		(in process)		
Eccharichia coli (ATCC26)	Mallyzing buffer solution	Pulse type: Dipolar / square	2.25 log	(Potoro et al. 2014)
Escherichild toli (ATGG20)	nH: 3.8 at 25 °C	t: * NS	2.25 10g10	(Fatalo et al., 2014)
	Conductivity:	τ: 4 μs		
	2 mS/cm at 25 °C	n: * NS		
		f: <sup>*</sup> NS		
		Energy input:40 J/mL		
		Flow rate:15 mL/min		
		Inlet temperature: $25 ^{\circ}\text{C}$		
		Pulse type: monopolar/square		
Escherichia coli	Commercial low-fat milk	E: 10 kV/cm	4.5 log <sub>10</sub>	(Lee et al., 2015)
(ATCC 8739)	pH: * NS	t: * NS		
	Conductivity: * NS	τ: 30 μs		
		n: NS		
		I: NS Energy input: 200 k I/kg		
		Flow rate:30 L/h		
		Inlet temperature: <b>30</b> °C		
		Maximum temperature: * NS		
		Pulse type: bipolar/square		
Escherichia coli	UHT whole milk with	E: 35 kV/cm	4.8 log <sub>10</sub>	(Walter et al., 2016)
(AICC 11/75)	4.0% Iat ( $W/W$ )	$t: 124 \ \mu s$		
	Conductivity: * NS	n: * NS		
		f: * NS		
		Energy input: * NS		
		Flow rate: 120 mL/min		
		Inlet temperature: NS		
		on average (in process)		
		Pulse type: * NS $/$ * NS		
Escherichia coli K12	Orange Juice	E: 20 kV/cm	5.06 log10	(Gurtler et al., 2010)
Escherichia coli (35218)	pH: 3.4 $\pm$ 0.1 at * NS°C	t: 70 μs	2.02 log10	
	Conductivity: NS	τ: 2.6 μs		
		n: * NS		
		Energy input: * NS		
		Flow rate: 120 mL/min		
		Inlet temperature: * NS		
		Maximum temperature: 55 °C (outlet)		
		Pulse type: bipolar / square	0.061	
Escnericnia coli DH5α (CGMCC 1 2170)	Grape Juice Soluble solid content:	E: 24 KV/CM t:180 us	3.06 log <sub>10</sub>	(Huang et al., 2014)
(COMCC 1.2170)	$15.8 \pm 0.2^{\circ}$ Brix at * NS°C	τ. 3 μς		
	pH: 5.98 $\pm$ 0.02 at * NS°C	n: * NS		
	Conductivity:	f: 120 Hz		
	$0.086\pm0.002$ S/m at 20 $^\circ\text{C}$	Energy input: * NS		
	& 0.098 $\pm$ 0.002 S/m at 30 $^\circ\text{C}$	Flow rate: 7.6 mL/min		
		Inlet temperature: 30 $^{\circ}$ C Maximum temperature: 32 2 $\pm$ 0.8 $^{\circ}$ C		
		Pulse type: monopolar / square		
Escherichia coli 1.107	Melon Juice		3.91 log10	(Mosqueda-Melgar et al.,
	Soluble solid content:	E: 35 kV/cm		2007)
				(continued on next page)

Exchanded off 1.1370     Ubiograph A af a SVC pit R, AA C + 04 af a SVC conductivity 3.33 = 0.03 m/cm af NSC     1.1350 pp m r r NSC     1.1350 pp m r r NSC     1.1350 pp m r r NSC       Exchanded off 1.1377     Watermetion info: status and content off 3.54 = 0.01 m/cm aft set perspectar r sNS content NV set perspectar r sNS con	Microorganism	Product	Treatment conditions	Reduction	Reference
pile 5.24 ± 0.00 m/m m m m m m m m m m m m m m m m m m		11.1°Brix at <sup>*</sup> NS°C	t: 1250 μs		
Exclusion of USON at Normal		pH: 5.82 $\pm$ 0.04 at $^{*}$ NS°C	τ: 4 μs		
Exclementia offiling     5.25 ± 0.05 mb/cm at 1NS C     E 580 Has 7762.23 JACa <sup>2</sup> How prace 100 m/cm in How prace 100 m/cm in Solutions     4.01 log <sub>26</sub> Compared-Molgar et al., 2007       Exclementia coli 1.107     Watermenton jate: Solution in Solutions     Watermenton jate: Solution in Solutions     1.01 log <sub>26</sub> 4.01 log <sub>26</sub> Compared-Molgar et al., 2007       Exclementia coli 1.107     Watermenton jate: Solution in Solution i		Conductivity:	n: * NS		
Extension of 1.107         Watermedian information of 1.107         Note that respectator: 'NS         Maximum temperator: 'NS         Maximum		$5.23 \pm 0.03$ mS/cm at NS°C	f: 250 Hz		
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Ruberbain cold 1.102       Warenels interaction of the cold of content interpolate int			Inlet temperature: * NS		
Backenoles cell 1.107         Naterenet in joint Stable sell conserver.         Points type: Higher / sparse Points type			Maximum temperature: 39.1 $\pm$ 0.1 $^\circ$ C		
Exclandada 1.107       Venenadada Julea       Polic type: bip36/r square       4.01 log in       (Decayada Medgar et al., 2007)         Ex 35 X/Vin       E 25 N Vin       1.52 N Vin       2007)         Selferia at NS C       in YS       1.52 N Vin       2007)         Selferia at NS C       in YS       1.52 N Vin       2007)         Selferia at NS C       in YS       1.52 N Vin       2.53 N/Vin       2.53 N/Vin         Exclorer/da col       1.52 N Vin       1.52 N Vin       5.53 log in       0.10 N Vin         Exclorer/da col       1.53 N/Vin       1.52 N Vin       5.53 log in       0.10 N Vin         V/UCC 11777)       Exclorer/da vin/vin       1.52 N Vin       1.53 N Vin       5.53 log in       0.10 N Vin         V/UCC 11777)       Exclorer/da vin/vin       1.53 N Vin       1.53 N Vin       5.53 log in       0.10 N Vin         V/UCC 11777)       Exclorer/da vin/vin       1.53 N Vin       1.53 N Vin       5.53 log in       0.53 log in       0.10 N Vin         Selferida col       0.01 A N SC nt N SC C       In SS N Vin       1.53 N Vin       5.53 log in       0.53 log in       0.50 log in       0.53 log in       0.55 log in       0.53 log in			(outlet)		
Bederichte ofil 1,107     Weternelen juleer     E. 35 W/cm     4.0 log.a     (Monnele-Meiger et al., 2007)       Bederichte ofil 1,107     Statue al 108° C     The paper (1.200 paper)     Conductive (2.200 paper)     2007)       Bederichte ofil (ATCC 11775)     Strawberry Julee (Moncelle solution)     E. 25 W/cm     5.53 log.a     (Monnele-Meiger et al., 2007)       Bederichte ofil (ATCC 11775)     Strawberry Julee (Moncelle solution)     E. 25 W/cm     5.53 log.a     (Monnele-Meiger et al., 2007)       Bederichte ofil (ATCC 11775)     Strawberry Julee (Moncelle solution)     E. 25 W/cm     5.53 log.a     (Monnele-Meiger et al., 2007)       Bederichte ofil (ATCC 11775)     Strawberry Julee (Moncelle solution)     E. 25 W/cm     5.53 log.a     (Monnele-Meiger et al., 2007)       Solube solid contentive: (ATCC 11875)     Strawberry Julee (Moncelle solution)     E. 25 W/cm     5.53 log.a     (Monnele-Meiger et al., 2008)       Solube solid contentive: (ATCC 14894)     Apple cder     E. 25 W/cm     6.38 log.a     (Monnele-Meiger et al., 2009)       Solube solid contentive: (ATCC 14084)     Apple cder     E. 29 W/cm     5.75 log.a     (Monnele-Meiger et al., 2009)       Solube solid contentive: (ATCC 14084)     Apple cder     E. 29 W/cm     5.75 log.a     (Monnele-Meiger et al., 2009)       Solubersolid 1.32 (OTCC 5001     Monnele anteritidi 1.32 (OTCC 5001     Monnele anteritidi 1.32 (OTCC 5001     Monn			Pulse type: bipolar / square		
Solution of Series at "NSC"     r. of p is p is construction of the Secience of the	Escherichia coli 1.107	Watermelon juice	E: 35 kV/cm	4.01 log <sub>10</sub>	(Mosqueda-Melgar et al.,
schemedia energia 1:2       Software       1:5:5:4:1:0:1:3       1:5:5:1:0:0:0:0:0:0:0:0:0:0:0:0:0:0:0:0:		6.5°Brix at * NS°C	τ:4 us		2007)
Solution offer control is 1,52 CVC2530 bit Description 74,11,8 / cm² Provints 1,93 / cm²1530 bit Provints 1,93 / cm² Provints 1,93 / cm²1530 bit Provints 1,93 / cm²1530 b		pH: 5.46 $\pm$ 0.11 at * NS°C	n: * NS		
3.05 + 0.05 mS/cm at "NS C       Programmer 27541.18 J/cm <sup>2</sup> Flow rate: 100 J/cmin       Plow rate: 100 J/cmin         Idea solution coll       Renovery Julee         (ATCC 11775)       Subble solid content         7.9 - 0.28 Piter at "NS C       Provide solution coll         (ATCC 11775)       Subble solid content       T 2 µ is         7.9 - 0.28 Piter at "NS C       Provide solution coll       T 2 µ is         3.00 - 10.17 Piter       Piter solution coll       T 2 µ is         3.00 - 10.17 Piter       Solution coll       T 2 µ is         3.01 - 10.17 Piter       Solution coll       T 2 µ is         3.01 - 11 + 10 Piter       Piter solution piter       Piter solution piter       Piter solution piter         3.01 + 10.17 Piter       Apple rider       Piter solution piter       Piter solution piter       Piter solution piter         3.01 + 10.17 Piter       Apple rider       Piter solution piter       Solution piter       Piter solution piter       Solution piter         3.01 + 10.28 Piter at "NS C       Piter solution piter       Piter solution piter       Solution piter       Piter solution piter       Solution piter         3.01 + 10.28 Piter at "NS C       Piter solution piter       Piter solution piter       Piter solution piter       Piter         3.00 + 10.28 Piter		Conductivity:	f: 250 Hz		
Excherichic coli       Strawberry Julee       Strawberry Julee       ESS MYCRA       5.53 logs       (Vidit et al., 2019)         Excherichic coli       Ododet olutica)       12 7 ja       5.53 logs       (Vidit et al., 2019)         Excherichic coli       Strawberry Julee       ESS MYCRA       12 7 ja       5.53 logs       (Vidit et al., 2019)         Excherichic coli       12 7 ja       12 7 ja       12 7 ja       5.53 logs       (Vidit et al., 2019)         Soliabile colid content:       12 7 ja         Conductivity:       Conductivity:       13 80 + 0.4 w/s, m al 'NYC       Plow rate: 50 mL/nin       6.38 logs       3.8 logs       (Usedes Olivein et al., 2019)         Conductivity:       12 5 Pitx al 'NYC       Plow rate: 50 mL/nin       6.38 logs       (Usequeta) Molecular et al., 2019)         Solumendio contentis of Contentiste of Conductivity:       12 5 Pitx al 'NYC       15 folgs       3.8 logs       (Usequeta) Molecular et al., 2019)         Solumendio contentia 1.82 (NCTC       Merion .nice       Experimentation 2.55 °C (na portation 0.10, nin late temperature: 4.0, 10 °C (nation		$3.66 \pm 0.05$ mS/cm at <sup>*</sup> NS°C	Energy input: 7541.18 J/cm <sup>3</sup>		
Excherichia cell (VTCC 11775)Strawberry, JuiceIC </td <td></td> <td></td> <td>Flow rate: 100 mL/min</td> <td></td> <td></td>			Flow rate: 100 mL/min		
Exhemichle coll (ATCC 11775)Strawberry Juice (Mode solution) Soluble solid content: 90.048 with content: 10.048 with content: 90.028 with a 'NS'C (Bit 3:30 + 0.01 at 'NS'C (Bit 1:30 + 0.01			Inlet temperature: NS Maximum temperature:		
Echebrichia coli (ATCC 11775)Strawberry Auto: (Model solid content: 7.9 ± 0.28 Brix at "NS"C 2.9 ± 0.28 Brix at "NS"C Conductivity: 1.25 Brix at "NS"C Conductivity: 1.25 Brix at "NS"C Display Display D			$30.3 \pm 0.2$ °C (outlet)		
Bachenolise off (ATCC 11775)Strawberry, hireE: 35 W/rm5.53 log(Vidio et al., 2019)(ATCC 11775)(Adde Jakuion)t: 2 jst: 3 jst:			Pulse type: bipolar / square		
(NTCC 11775)(Model solution)t=27 µs t=7.9 = 0.28 Prix at "NSC t=155 hr t=0.25 Prix at "NSC t=155 hr t=0.25 Prix at "NSC t=155 hr t=0.25 Prix at "NSC t=155 hr t=0.25 Prix at "NSC t=0.25 Prix at "NS	Escherichia coli	Strawberry Juice	E: 35 kV/cm	5.53 log10	(Yildiz et al., 2019)
Soluble solid content:     t: 2 µs       Pit 3.9 = 0.28 Pit x at "NS"C     r: 1 NS       Pit 3.9 = 0.01 at "NS"C     f: 155 Hz       Excherichia call     Apple cider       (ATCC 43894)     Apple cider       Pit 3.8 = 1.00 Tat "NS"C     r: NS       O157:17     Soluble solid content:     r: NS       Solubie solid content:     r: NS C     r: NS C       Pit Solution:     r: NS C     r: NS C       Solution:     r: Solution:     r: Solution:       Solution:     r: Solution:     r: Solution:       Solution:     r: Solution:     r: Solution:       Solution:     r: Solution:	(ATCC 11775)	(Model solution)	t: 27 μs		
Salmonella enerritátis 1.82 (NCTC       Pá 5.02 bit Nartí NSC       ft 1.55 Hz       ft 1.55 Hz       ft 1.55 Hz         Secherichia coli       Solde Sold content:       ft 1.55 Hz       <		Soluble solid content: $7.0 \pm 0.20^{\circ}$ Prime t <sup>*</sup> NG <sup>o</sup> C	τ: 2 μs		
Salmonella entertida 1.82 (NCT 9001) Salmonella entertida 1.82 (NCT Salmonella entertida 1.82 (NCT Solub e solid content: 1.11 effer entertida 1.82 (NCT Solub e solid content: 1.12 forts at "NS"C 1.12 forts at "N		$7.9 \pm 0.28$ BTIX at NS C pH: 3.39 + 0.01 at * NS °C	n: NS f: 155 Hz		
3.00 ± 0.14 mS/cm at 'NS'CFlow rate: S50 mL/min harimum temperature: 46.0 °C Public type: monopolar / sparse E. 30 KV/cm6.38 log.9(Mendes-Oliveira et al., 2020)2157:H2Apple ciderE. 30 KV/cm6.38 log.9(Mendes-Oliveira et al., 2020)(ATCC 48994)12.5 'Brit at 'NS'C Conductivity: B288 JS'Cm at 'NS'Ctr 'NS Conductivity: B288 JS'Cm at 'NS'Cstr 'NS Conductivity: B288 JS'Cm at 'NS'Cstr 'NS'C Conductivity: B288 JS'Cmstr		Conductivity:	Energy input: * NS		
Escherichia coli O157:H7Apple ciderBischerichia coli Cadasci pictorApple ciderBischerichia coli Cadasci pictorApple ciderBischerichia coli Cadasci pictorApple ciderBischerichia coli Cadasci pictorCherica coli PictorCherica coli PictorDistor PictorDisto		$3.90 \pm 0.14$ mS/cm at $^*$ NS°C	Flow rate: 350 mL/min		
Eacharichia coli 0157:17Apple cider Solubile solid content: 12.5 Bits at 'NS'C Conductivity: 2288 µS/cm at 'NS'C Conductivity: 2388 µS/cm at 'NS'CG.38 log:a 2.300)(Mendes-Oliveina et al., 2.020)Salmonella emeritadia 1.82 (NCTC 9001)Melan JuiceE: 30 KV/cm 1.11: "Bits at 'NS'C E: 30 KV/cm E: 30 KV/cm5.7C log:a 1.12: Spin at 'NS'CMelan Juice3.75 log:a 2.75 log:a(Mosqueda-Melgar et al., 2.007)Salmonella emeritadia 1.82 (NCTC 9001)Melan Juice 1.11: "Bits at 'NS'CE: 35 KV/cm 1.12: Spin at 'NS'C3.75 log:a 1.12: Spin at 'NS'C(Mosqueda-Melgar et al., 2.007)Salmonella emeritadia 1.82 (NCTC 9001)Melan Juice 1.52: 3 ± 0.03 mS/cm at 'NS'CE: 35 KV/cm 1.12: Spin at 'NS'C3.75 log:a 1.12: Spin at 'NS'C(Mosqueda-Melgar et al., 2.007)Salmonella emeritadia 1.82 (NCTC 9001)Melan Juice 1.52: 3 ± 0.03 mS/cm at 'NS'Cit 1.250 µS3.75 log:a 1.12: Spin at 'NS'C(Mosqueda-Melgar et al., 2.007)Salmonella emeritadia 1.82 (NCTC 9001)Melan Juice 1.52: 3 ± 0.03 mS/cm at 'NS'Cit 2.950 µS4.27 log:a 2.007)(Mosqueda-Melgar et al., 2.007)Salmonella orginitari 1.52 (NCTC 9001)Maternelon Juice Soluble solid content: 5.23 ± 0.03 mS/cm at 'NS'Cit 3.55 log:a 1.00 Hz4.27 log:a 2.007)Salmonella orginitari 1.52 (NCTC 9001)Maternelon Juice 3.66 ± 0.05 mS/cm at 'NS'C 1.00 Hzit 3.66 ± 0.05 mS/cm at 'NS'C 2.007)it 3.65 ± 0.05 mS/cm at 'NS'C 2.007)it 3.65 ± 0.05 mS/cm at 'NS'C 2.007)Salmonella Typhimurinm (MTC 1.4028)Apple cider 2			Inlet temperature: 22.7 $\pm$ 0.07 $^\circ\text{C}$		
Excherichia coli O157:H7       Apple cider       E:30 kV/cm       6.38 log:n       (Mendes-Oliveira et al., 2020)         (ATOC 43894)       12.5 'Brix at 'NS'C       t 'NS       t 'NS'       a' 'NS'         (ATOC 43894)       12.5 'Brix at 'NS'C       t 'NS'       a' 'NS'         2088 ja/cm at 'NS'C       a' 'NS'       Energy input:/08.0 /ILI       Flow rate: 60 nL/min         Inter temperature       Maximum temperature       3.75 log:n       (Mongueda-Melgar et al., 2007)         Salmonella entertidis 1.82 (NCTC       Melon Juice       ± 35 KV/cm       3.75 log:n       (Mongueda-Melgar et al., 2007)         9001)       Salmonella entertidis 1.82 (NCTC       Melon Juice       ± 35 KV/cm       3.75 log:n       (Mongueda-Melgar et al., 2007)         9001)       Salmonella entertidis 1.82 (NCTC       Melon Juice       ± 35 KV/cm       3.75 log:n       (Mongueda-Melgar et al., 2007)         9001)       Salmonella entertidis 1.82 (NCTC       Meton Juice       ± 35 KV/cm       3.75 log:n       (Mongueda-Melgar et al., 2007)         9001)       Materime inplore       ± 35 KV/cm       3.75 log:n       (Mongueda-Melgar et al., 2007)         Salmonella entertidis 1.82 (NCTC       Materime inplore       ± 35 KV/cm       4.27 log:n       (Mongueda-Melgar et al., 2007)         Salmonella functidis 1.82 (NCTC			Maximum temperature: 46.0 °C		
Excitation colu     Apple Close     E. 50. V/Cli     C.S5 log:10     Use and Solide solid content:     1: N       (ATCC 43894)     12.5 Bits at 'NS C     r: 'NS     r: 'NS     2020)       (ATCC 43894)     12.5 Bits at 'NS C     r: 'NS     2020)       Salmonella enteritidis 1.82 (NCTC     Melon Juice     E. 35 W/Cm     3.75 log:10       Solido esidi content:     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     11.1 Bits at 'NS C     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     11.1 Bits at 'NS C     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     Soluble solid content:     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     Soluble solid content:     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     Soluble solid content:     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     Soluble solid content:     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     Soluble solid content:     t: 1250 µs     3.75 log:10     (Mosqueda-Melgar et al., 2007)       9001)     Soluble solid content:     t: 1250 µs     2.27 log:10     (Mosqueda-Melgar et al., 2007)       1.61 temperature: NS	Feeborichia coli	Apple eider	Pulse type: monopolar / square	6.29 100	(Mondos Olivoiro et al
(ATCC 43894)       12.5 "Britra at "NS"C       r. "NS         pH 38.0 at "NS"C       n. "NS"         Conductivity:       2058 pS/cm at "NS"C       Encryptique 408 J/mL         Flow rate: 60 mL/min       Inlet temperature:       Association of the second of the sec	0157:H7	Soluble solid content:	t: * NS	0.38 l0g10	(Weldes-Oliveira et al., 2020)
salanonella emeritidis 1.82 (NCTC)       Pris 3.83 a', "NS"C       n.", "NS       f. 1500pm2         Salmonella emeritidis 1.82 (NCTC)       Melon Juice       E: 35 M/Cm       3.75 log10       QMosqueda-Melgar et al., 2007)         9001)       Soluble solid content:       11.1"Birx at "NS"C       E: 35 M/Cm       3.75 log10       QMosqueda-Melgar et al., 2007)         9001)       Soluble solid content:       11.1"Birx at "NS"C       tr. 'NS"C       T. 'S B'         Salmonella emeritidis 1.82 (NCTC)       Soluble solid content:       tr. 'NS"C       tr. 'NS"C       QMosqueda-Melgar et al., 2007)         Salmonella emeritidis 1.82 (NCTC)       Soluble solid content:       tr. 'NS"C       tr. 'NS"C       QMosqueda-Melgar et al., 2007)         Salmonella emeritidis 1.82 (NCTC)       Watermelon juice       E: 35 M/Cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Soluble solid content:       11.1"Birx at "NS"C       tr. 'NS"C       T. 'NS"C       Augure         soluble solid content:       1.2000 js       3.07" (outlet)       2007)       2007)         Soluble solid content:       tr. 'NS"C       tr. 'NS"C       tr. 'NS"C       2007)         soluble solid content:       tr. 'NS"C       tr. 'NS"C       2007)         Soluble solid content:       tr. 'NS"C       tr. 'NS"C       2007)	(ATCC 43894)	12.5°Brix at <sup>*</sup> NS°C	τ: * NS		,
Salmonella enteritidis 1.82 (NCTC 9001)Melon Juice NS*CEnergy input-408 J/mL How rate: 60 mL/min Indet temperature: <55 °C (in process) Pulse type: bipOar / square E :35 KVcm3.75 log10(Mosqueda-Melgar et al., 2007)Salmonella enteritidis 1.82 (NCTC 9001)Melon Juice State in NS*C11.15 Krist 11.15 Kr		pH: 3.83 at <sup>*</sup> NS°C	n: * NS		
Salmonella enteritäds 1.82 (NCTC 9001)       Meion Juice       Energy input:408 J.vnl. Flow rate: 55 °C (in process)       (Mosqueda-Melgar et al., 2007)         Salmonella enteritäds 1.82 (NCTC 9001)       Meion Juice       E: 35 kV/cm       3.75 log;o       (Mosqueda-Melgar et al., 2007)         Salmonella enteritäds 1.82 (NCTC 9001)       Meion Juice       E: 35 kV/cm       3.75 log;o       (Mosqueda-Melgar et al., 2007)         Salmonella enteritäds 1.82 (NCTC 9001)       Meion Juice       E: 35 kV/cm       4.27 log;o       (Mosqueda-Melgar et al., 2007)         Salmonella enteritäds 1.82 (NCTC 9001)       Watermelon juice       E: 35 kV/cm       4.27 log;o       (Mosqueda-Melgar et al., 2007)         Salmonella enteritäds 1.82 (NCTC 9001)       Watermelon juice       E: 35 kV/cm       4.27 log;o       (Mosqueda-Melgar et al., 2007)         Salmonella enteritäds 1.82 (NCTC 9001)       Watermelon juice       E: 35 kV/cm       4.27 log;o       (Mosqueda-Melgar et al., 2007)         Salmonella enteritäds 1.82 (NCTC 9001)       Watermelon juice       E: 30 kV/cm       6.34 log;o       (Mendes-Oliveira et al., 2007)         Salmonella Typhimurium (ATCC 14028)       Apple cider       E: 30 kV/cm       6.34 log;o       (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium (ATCC 14028)       Apple cider       E: 30 kV/cm       1.62 log;o       (Mendes-Oliveira et al., 2020)		Conductivity:	f: 1500pps		
Salmonella enteritidis 1.82 (NCTC)       Melon Juice       Maximum temperature:       NS C       Maximum te		2088 μS/cm at NS°C	Energy input:408 J/mL		
Salmonella enteritidis 1.82 (NCTC 9001)       Melon Juice       E 35 kV/cm       3.75 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         9001)       Soluble solid content: 11.17 brix at 'NS'C Conductivity:       t 1250 µs       3.75 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         9001)       Soluble solid content: 11.17 brix at 'NS'C Conductivity:       t 125 µs       3.75 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC 9001)       Watermelon juice       E argy input: 766.223 J/cm <sup>3</sup> 4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC 9001)       Watermelon juice       E argy input: 766.23 J/cm <sup>3</sup> 4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC 9001)       Watermelon juice       E argy input: 754.18 J/cm <sup>3</sup> 4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC 9001)       Watermelon juice       E argy input: 754.18 J/cm <sup>3</sup> 4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         Salmonella Typhimurium (ATCC 14028)       Apple cider       E argy input: 754.18 J/cm <sup>3</sup> 6.34 log <sub>10</sub> (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium (ATCC 14028)       Apple cider       t 'NS'C       t 'NS       6.34 log <sub>10</sub> (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium (ATCC 14028)       Apple cider <td></td> <td></td> <td>Flow rate: 60 mL/min</td> <td></td> <td></td>			Flow rate: 60 mL/min		
Salmonella enteritidis 1.82 (NCTC 9001)Melon Juice Network 1 NS°C pH: 5.82 ± 0.04 at 'NS°C Conductivity: 5.23 ± 0.03 mS/cm at 'NS°C Energy input: 756.23 ± 0.03 mS/cm at 'NS°C Energy input: 756.23 ± 0.01 mS/cm at 'NS°C Energy input: 756.11 mS/cm Energy input: 756.11 mS/cm En			Maximum temperature: <55 °C (in		
Pulse type: bjolar/ square9001)Wolon JuiceSi Sk/CmSi Sk/CmSi Sk/CmSi Sk/CmMongueda-Melgar et al., 2007)9001)11.1 "Brix a" NS" Cr. * µ µ2007)2007)11.1 "Brix a" NS" Cr. * µ µ2007)pH: 5.82 ± 0.04 at " NS "Cr. * NS2007)Conductivity:f. 175 Hz2007)5.23 ± 0.03 mS/cm at "NS"CEnergy input: 7662.23 J/cm <sup>3</sup> Flow rate: 100 mL/ninIdet temperature: NS"Maximum temperature: 39.1 ± 0.1 "C2007)Salmonella enteritidis 1.82 (NCTCWatermelon juiceE. 35 KV/cm4.27 log10(Mosqueda-Melgar et al., 2007)9001)Soluble solid content:t. 2000 µ2007)2007)5.5 Prix at "NS" Cr. * NSr. * NS2007)6.5 Prix at "NS" Cr. * NSr. * NS2007)6.5 Prix at "NS" Cr. * NSr. * NS2007)6.5 Prix at "NS" Cr. * NS2007)2007)6.5 Prix at "NS" Cr. * NS2007)6.5 Prix at "NS" Cr. * NS2007)6.5 Prix at "NS" Cr. * NS2007)9011Apple ciderE. 200 (v cm6.34 log10(ATCC 14028)Apple cidert. * NS" Ca. * NS"Salmonella TyphimuriumApple cidert. * NS" Ct. * NSSalmonella Typhimurium y4065Orange Julcet. * NS" Ct. * NSSalmonella Typhimurium y4065Orange Julcet. * NS" Ct. * NS"Salmonella Typhimurium y4065Orange Julcet. * NS" C1.62 log10 <td></td> <td></td> <td>process)</td> <td></td> <td></td>			process)		
Salmonella enteritidis 1.82 (NCTC       Melon Juice       E. 35 KV/cm       3.75 log10       (Mosqueda-Melgar et al., 2007)         9001)       Soluble solid content:       t. 1250 µs       2007)       2007)         11.1*Brix at "NS*C       tr. 4 µs       2007)       2007)         Salmonella enteritidis 1.82 (NCTC       pH: 5.82 ± 0.04 at "NS*C       Energy input: 766.23 J/cm <sup>3</sup> 2007)         Salmonella enteritidis 1.82 (NCTC       Watermelon juice       Energy input: 766.23 J/cm <sup>3</sup> 2007)         Salmonella enteritidis 1.82 (NCTC       Watermelon juice       E35 kV/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC       Watermelon juice       E35 kV/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC       Watermelon juice       E35 kV/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC       Watermelon juice       E35 kV/cm       4.27 log10       2007)         Salmonella enteritidis 1.82 (NCTC       Watermelon juice       Tr 4 µs       2007)       2007)         Salmonella politicitis 1.82 (NCTC       Watermelon juice       Tr 6 µs       2007)       2007)         Salmonella Typhimurium       Apple cider       Eaerery input: 7541.18 J/cm <sup>3</sup> 1.62 log10 <td></td> <td></td> <td>Pulse type: bipolar / square</td> <td></td> <td></td>			Pulse type: bipolar / square		
9001) Soluble solid content: t 1250 $\mu$ s (2007) 11.1 "BYK at "NS" C $\tau$ 4 $\mu$ s (175 Hz 5.23 $\pm$ 0.03 mS/cm at "NS" C Energy input: 7662.23 J/cm <sup>3</sup> Flow rate: 100 mL/min Indict temperature: 39.1 $\pm$ 0.1 "C (outlet) 9001) Soluble solid content: t 2000 $\mu$ s 4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 9001) Soluble solid content: t 2000 $\mu$ s 4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 9001) Soluble solid content: t 2000 $\mu$ s 2007) 5.5 "Brix at "NS" C $\pi$ : "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.01 at "NS" C $\pi$ : "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "S C Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.11 at "NS" C $\pi$ "NS Conductivity: f 100 Hz 3.66 $\pm$ 0.05 mS/cm at "NS" C $\mu$ s "S C Conductivity: f 12.5" Brix at "NS" C $\pi$ "NS Conductivity: f 1500 pps 2088 $\mu$ S/cm at "NS" C $\pi$ "NS Conductivity: f 1500 pps Salmonella Typhimurium x3985 Salmonella Typhimurium x3985 Salmon	Salmonella enteritidis 1.82 (NCTC	Melon Juice	E: 35 kV/cm	3.75 log <sub>10</sub>	(Mosqueda-Melgar et al.,
Salmonella Typhimurium       Apple cider       E. 36 kV/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Soluble solid content:       E. 35 kV/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         9001)       Soluble solid content:       E. 35 kV/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         9001)       Soluble solid content:       E. 35 kV/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Salmonella Typhimurium       Soluble solid content:       E. 35 kV/cm       6.34 log10       2007)         Salmonella Typhimurium       Apple cider       E. 30 kV/cm       6.34 log10       (Mendes-Oliveira et al., 2010)         Salmonella Typhimurium       Apple cider       E. 30 kV/cm       6.34 log10       (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium       Apple cider       E. 30 kV/cm       6.34 log10       (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium       Apple cider       E. 30 kV/cm       6.34 log10       (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium       Soluble solid content:       1 NS C       m.* NS       Conductivity:         12.5* Brix at *NS*C       m.* NS       m.* NS       Conductivity:       2020)       2020)         Salmonella Typhimurium x3985       Soluble solid content:       1.	9001)	Soluble solid content:	t: 1250 μs		2007)
Conductivity:f: 175 Hz5.23 ± 0.03 mS/cm at * NS*CEnergy input: 7662.23 J/cm3Flow rate: 100 mL/min Inlet temperature: 39.1 ± 0.1 *C (outlet)Flow rate: 100 mL/min Inlet temperature: 39.1 ± 0.1 *C (outlet)Salmonella entertiidis 1.82 (NCTCWatermelon juiceSa Sk V/cm4.27 log10Soluble solid content:t: 2000 µs2007)Soluble solid content:t: 200 µb2007)Jace 2 C (outlet)Pulse type: bipolar / square5.34 ± 0,1 xt *Ns°CPulse type: bipolar / squaret: 30.8 ± 0,2 °C (outlet)2020)Pulse type: bipolar / squaret: 30.8 ± 0,2 °C (outlet)2020)Pulse type: bipolar / squaret: 3.8 at *Ns°Ct: *Ns(ATCC 14028)Soluble solid content:t: *Ns2020)Soluble solid content:t: *Nst: *Ns12.5 Brix at *Ns°Ct: *Nst: *NsConductivity:t: S0 kV/cm6.34 log10(ATCC 14028)Soluble solid content:t: *Ns12.5 Brix at *Ns°Ct: *Nst: *NsPulse type: bipolar / squareE: 20 kV/cm1.62 log10Soluble solid content:t: *Ns2.36 log10 <td></td> <td>pH: 5.82 <math>\pm</math> 0.04 at * NS °C</td> <td>n: * NS</td> <td></td> <td></td>		pH: 5.82 $\pm$ 0.04 at * NS °C	n: * NS		
Salmonella enteritidis 1.82 (NCTC)       Watermelon juice       Energy input: 7662.23 /cm <sup>3</sup> Flow rate: 100 mL/min         Salmonella enteritidis 1.82 (NCTC)       Watermelon juice       E35 W/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Salmonella enteritidis 1.82 (NCTC)       Watermelon juice       E35 W/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         Soluble solid content:       E35 W/cm       E35 W/cm       4.27 log10       (Mosqueda-Melgar et al., 2007)         6.5° Brix at *NS°C       r. 4 μs       2007)       2007)       2007)         6.5° Brix at *NS°C       r. 4 μs       2007)       2007)         3.66 ± 0.05 mS/cm at *NS°C       Energy input: 7541.18 J/cm <sup>3</sup> 1.63 log10       (Mendes-Oliveira et al., 2010)         Salmonella Typhimurium       Apple cider       E 30 W/cm       6.34 log10       (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium       Apple cider       E 30 W/cm       6.34 log10       (Mendes-Oliveira et al., 2020)         Solube solid content:       t * NS       maximum temperature: *NS       2020)       2020)       2020)         1.25 Brix at *NS°C       n* NS       Energy input:408 J/mL       Flow rate: 60 mL/min       Maximum temperature: <55 °C (in process)		Conductivity:	f: 175 Hz		
Salmonella enteritidis 1.82 (NCTC       Watermelon juice       E: 35 KV/cm       4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 2007)         9001)       Soluble solid content:       t: 2000 μs       2007)       2007)         6.5° Brix at "NS°C       r: 4 μs       2007)       2007)         901)       Soluble solid content:       t: 2000 μs       2007)         6.5° Brix at "NS°C       r: 4 μs       2007)       2007)         901       Soluble solid content:       t: 000 μs       2007)         5.5° Brix at "NS°C       r: 4 μs       2007)       2007)         901       Soluble solid content:       t: 100 Hz       3.66 ± 0.05 mS/cm at "NS°C       102 tHemperature: "NS         Maximum temperature: "NS       Ja.66 ± 0.05 mS/cm at "NS°C       Energy input: 7541.18 J/cm <sup>3</sup> 114: themperature: "NS         Salmonella Typhimurium       Apple cider       E: 30 KV/cm       6.34 log <sub>10</sub> (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium       Soluble solid content:       t: "NS       2020)       2020)         L2:5° Brix at "NS°C       r: "NS       2020)       2020)       2020)         Soluble solid content:       t: "NS       Energy input:408 J/ml.       2020)       2020)         L2:5° Brix at "NS°C       r: "NS       Con		$5.23\pm0.03$ mS/cm at $^*$ NS°C	Energy input: 7662.23 J/cm <sup>3</sup>		
Salmonella enteritidis 1.82 (NCTC)Watermelon juiceWatermelon juiceBile temperature: 39.1 ± 0.1 °C (outlet)Maximum temperature: 39.1 ± 0.1 °C (outlet)Mosqueda-Melgar et al.,9001)Soluble solid content:t: 2000 µs4.27 log10(Mosqueda-Melgar et al.,9001)Soluble solid content:t: 2000 µs2007)pit: 5.46 ± 0.11 at "NS°Cr. 4 µs2007)pit: 5.46 ± 0.11 at "NS°Cn. "NSConductivity:f. 100 Hz3.66 ± 0.05 mS/cm at "NS°CEnergy input: 7541.18 J/cm³Inlet temperature:30.3 ± 0.2 °C (outlet)Pulse type: bipolar / square6.34 log10(ATCC 14028)Soluble solid content:12.5°Brix at "NS°Cr. "NSpit: 3.83 at "NS°Cr. "NSpit: 3.83 at "NS°Cr. "NSpit: 3.83 at "NS°Cenergy input: 408 J/mLpit: 3.84 ± 0.1 at "NS°CE: 20 K//cmpit: 3.45 ± 0.1 at "NS°Ct: 70 µsSalmonella Typhimurium x4998Orange JuiceSalmonella Typhimurium x4998Orange JuiceSalmonella Typhimurium x4998Orange JuiceSalmonella Typhimurium x4998Orange JuiceSalmonella Typhimuriumpit: 3.4 ± 0.			Flow rate: 100 mL/min		
Salmonella enteritidis 1.82 (NCTC Soluble solid content: t 2000 µs 4.27 log <sub>10</sub> (Mosqueda-Melgar et al., 2007) 9001) Soluble solid content: t 2000 µs 2007) 6.5°Brix at *NS°C r. 4 µs 1.5°C r. 4 µs 2007) 6.5°Brix at *NS°C r. 4 µs 2007) 5.66°± 0.05°MS/cm at *NS°C r. 4 µs 2007) Soluble solid content: t 100 Hz 2007 Soluble solid content: t 100 Hz 2007 12.5°Brix at *NS°C r. 4 µs 2007) 5.2°Brix at *NS°C r. 4 µs 2007) 5.2°Brix at *NS°C r. 4 µs 2007) 5.2°Brix at *NS°C r. 4 µs 2007 5.2°C (outlet) Pulse type: bipolar / square E: 20 kV/cm 6.34 log <sub>10</sub> (Mendes-Oliveira et al., 2020) 12.5°Brix at *NS°C r. 4 µS 2020) 12.5°Brix at *NS°C r. 4 µS 2020) 5.2°Brit at *NS°C r. 4 µS 2020) 5.2°Brit at *NS°C r. 4 µS 2020) 5.2°Brit at *NS°C r. 4 µS 2020) 5.2°C (in process) Pulse type: bipolar / square E: 20 kV/cm 1.62 log <sub>10</sub> (Gurtler et al., 2010) Pit : 3.4 ± 0.1 at *NS°C t 70 µs 2.36 log <sub>10</sub> 5.2°C (onductivity: *NS t 2.6 µs 2.36 log <sub>10</sub>			Inlet temperature: NS*		
Salmonella enteritidis 1.82 (NCTCWatermelon juice Soluble solid content: 6.5° Brix at *NS°C 0, 5° Brix at *NS°C 100 Hz 1, 506 ± 0.05 mS/cm at *NS°C 104 Energy input: 7541.18 J/cm³ 1 Inlet temperature: *NS Maximum temperature: *NS 104 Bright and temperature: *NS 104 Bright and temperature: *NS 104 Bright and temperature: *NS 104 Bright and temperature: *NS 12.5° Brix at *NS°C 12.5° Brix at *NS°C 13.			(outlet) (outlet)		
Salmonella enteritidis 1.82 (NCTC       Watermelon juice       E: 35 kV/cm <sup>1</sup> 4.27 log10       (Mosqueda-Melgar et al., 2007)         9001)       6.5° Brix at *NS°C       r: 4 μs       2007)       2007)         91       6.5° Brix at *NS°C       r: 4 μs       2007)       2007)         91       5.46 ± 0.11 at *NS°C       r: 4 μs       2007)       2007)         91       5.46 ± 0.11 at *NS°C       r: 4 μs       2007)       2007)         92       3.66 ± 0.05 mS/cm at *NS°C       Energy input: 7541.18 J/cm <sup>3</sup> 1       1         92       3.66 ± 0.05 mS/cm at *NS°C       Energy input: 7541.18 J/cm <sup>3</sup> 1       1			Pulse type: bipolar / square		
9001) Soluble solid content: t 2000 μs 2007) 6.5° Brix at * NS°C τ : 4 μs 15: 5.46 ± 0.11 at * NS°C n-11 at * NS°C r : 4 μs Salmonella Typhimurium χ3985 Salmonella Typhimurium χ4096 Salmonella Typhimurium χ406 Salmonella Typhimurium X406 Salmonella Typhimurium X406 Salmonella Typhimurium X406 Salmonella Typhimurium X4	Salmonella enteritidis 1.82 (NCTC	Watermelon juice	E: 35 kV/cm	4.27 log10	(Mosqueda-Melgar et al.,
	9001)	Soluble solid content:	t: 2000 μs		2007)
$Salmonella Typhimurium \chi 3985$ Salmonella Typhimurium $\chi 3985$ Salmonella Typhimurium $\chi 4096$ Salmonella Typhimurium $\chi 5006$ Salmonella Typhimurium $\chi 506$ Salmonella		$6.5^{\circ}$ Brix at $^{\circ}$ NS $^{\circ}$ C	τ: 4 μs		
Salmonella Typhimurium χ3985 Salmonella Typhimurium χ4096 Salmonella Typhimurium χ4096 Salmonella Typhimurium       Apple cider       Energy input: 7541.18 J/cm <sup>3</sup> Inlet temperature: *NS Maximum temperature: 30.3 ± 0.2 °C (outlet) Pulse type: bipolar / square         Salmonella Typhimurium       Apple cider       E: 30 kV/cm       6.34 log10       (Mendes-Oliveira et al., 2020)         Salmonella Typhimurium       Soluble solid content:       t * NS       2020)       2020)         12.5° Brix at * NS°C       r. * NS       2020)       2020)         12.5° Brix at * NS°C       r. * NS       2020)         2088 μS/cm at * NS°C       f: 1500pps       2088 μS/cm at * NS°C       Energy input: 408 J/mL         Flow rate: 60 mL/min       Maximum temperature: <55 °C (in process)		pH: 5.46 $\pm$ 0.11 at NS <sup>*</sup> C Conductivity:	n: NS f: 100 Hz		
Salmonella Typhimurium X3985 Salmonella Typhimurium X4096 Salmonella Typhimurium X4096 Salmonella Typhimurium X4096Apple cider Apple cider Soluble solid content: 12.5°Brix at *NS°C PH: 3.83 at *NS°C Conductivity: *NS6.34 log10 (Mendes-Oliveira et al., 2020)Salmonella Typhimurium X4096 Salmonella Typhimurium X4096 Salmonella Typhimurium X4096Orange Juice pH: 3.4 ± 0.1 at *NS°C Conductivity: *NSE: 20 kV/cm1.62 log10 2.36 log10(Gurtler et al., 2010) (Gurtler et al., 2010)Salmonella Typhimurium X4096 Salmonella Typhimurium X4096Orange Juice pH: 3.4 ± 0.1 at *NS°C Conductivity: *NSE: 20 kV/cm1.62 log10 2.36 log10(Gurtler et al., 2010) (Gurtler et al., 2010)		$3.66 \pm 0.05$ mS/cm at <sup>*</sup> NS°C	Energy input: 7541.18 J/cm <sup>3</sup>		
Salmonella Typhimurium χ3985 Salmonella Typhimurium χ3985 Salmonella Typhimurium χ49965 Salmonella Typhimurium χ4965 Salmonella Typhimurium χ4965 <td></td> <td></td> <td>Inlet temperature: * NS</td> <td></td> <td></td>			Inlet temperature: * NS		
$\begin{array}{cccccccccccccccccccccccccccccccccccc$			Maximum temperature:		
Salmonella Typhimurium       Apple cider       E: 30 kV/cm       6.34 log10       (Mendes-Oliveira et al., 2020)         (ATCC 14028)       Soluble solid content:       t * NS       2020)       2020)         12.5°Brix at *NS°C       r: * NS       2020)         pH: 3.83 at *NS°C       n: * NS       2020)         Conductivity:       f 1500pps       2088 μS/cm at * NS°C       Energy input:408 J/mL         Flow rate:       60 mL/min       Maximum temperature: <55 °C (in process)			$30.3 \pm 0.2$ °C (outlet)		
Solutionated TyphinuriumApple CreftE. Solvy/Chi0.04 $\log_{10}$ (interdescription at et al., 2020)(ATCC 14028)Soluble solid content: 12.5°Brix at *NS°C pH: 3.83 at *NS°Ct. *NS t. *NS conductivity: 2088 $\mu$ S/cm at *NS°Cn. *NS f. 1500pps 2088 $\mu$ S/cm at *NS°C2020)2088 $\mu$ S/cm at *NS°Cf. 1500pps Energy input:408 J/mL Flow rate: 60 mL/min Maximum temperature: <55 °C (in process) 	Salmonella Typhimurium	Apple cider	Figure Sector Figure Fi	6.34 log	(Mendes Oliveira et al
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	(ATCC 14028)	Soluble solid content:	t: * NS	0.54 10g10	2020)
$ \begin{array}{cccc} pH: 3.83 at {}^{\circ}NS^{\circ}C & n: {}^{\circ}NS \\ Conductivity: & f: 1500pps \\ 2088 \ \mu S/cm at {}^{\circ}NS^{\circ}C & Energy input:408 \ J/mL \\ Flow rate: 60 \ mL/min \\ Maximum temperature: <55 {}^{\circ}C (in \\ process) \\ Pulse type: bipolar \ / square \\ Salmonella \ Typhimurium \ \chi 4096 \\ Salmonella \ Typhimurium \ \chi 4096 \\ Salmonella \ Typhimurium \ \chi 4096 \\ Conductivity: {}^{\circ}NS & t: 2.6 \ \mu S \end{array} $		12.5°Brix at <sup>*</sup> NS°C	τ: <sup>*</sup> NS		
Conductivity:       f: 1500pps         2088 μS/cm at * NS°C       Energy input:408 J/mL         Flow rate: 60 mL/min       Maximum temperature: <55 °C (in process)		pH: 3.83 at <sup>*</sup> NS°C	n: <sup>*</sup> NS		
2088 μS/cm at NS°C       Energy input:408 J/mL         Flow rate: 60 mL/min       Maximum temperature: <55 °C (in process)		Conductivity:	f: 1500pps		
Filew Fall: Boo InL/Initi       Maximum temperature: <55 °C (in process)		2088 µS/cm at NS°C	Energy input:408 J/mL		
Salmonella Typhimurium χ3985       Orange Juice       E: 20 kV/cm       1.62 log10       (Gurtler et al., 2010)         Salmonella Typhimurium χ4096       pH: 3.4 ± 0.1 at *NS°C       t: 70 μs       2.36 log10         Salmonella Typhimurium       Conductivity: *NS       t: 20 μs       (continued on next page)			Flow rate: of IIIL/IIIIn Maximum temperature: <55 °C (in		
Salmonella Typhimurium χ3985       Orange Juice       Pulse type: bipolar / square         Salmonella Typhimurium χ4096       pH: 3.4 ± 0.1 at *NS°C       E: 20 kV/cm       1.62 log10       (Gurtler et al., 2010)         Salmonella Typhimurium       pH: 3.4 ± 0.1 at *NS°C       t: 70 μs       2.36 log10         Salmonella Typhimurium       Conductivity: *NS       t: 2.6 μs       (continued on next page)			process)		
Salmonella Typhimurium $\chi 3985$ Orange JuiceE: 20 kV/cm1.62 log_{10}(Gurtler et al., 2010)Salmonella Typhimurium $\chi 4096$ pH: 3.4 $\pm$ 0.1 at $^{\circ}$ NS°Ct: 70 $\mu$ s2.36 log_{10}Salmonella TyphimuriumConductivity: $^{\circ}$ NS $\tau$ : 2.6 $\mu$ s(continued on pext page)			Pulse type: bipolar / square		
Salmonella Typhimurium χ4096       pH: 3.4 ± 0.1 at NS°C       t: 70 μs       2.36 log <sub>10</sub> Salmonella Typhimurium       Conductivity: <sup>*</sup> NS       τ: 2.6 μs	Salmonella Typhimurium $\chi 3985$	Orange Juice	E: 20 kV/cm	1.62 log10	(Gurtler et al., 2010)
ounnoneur ryphanad aan Conductivity. No Continued on next none)	Salmonella Typhimurium χ4096	pH: $3.4 \pm 0.1$ at NS°C Conductivity: * NS	t: 70 μs τ: 2.6 μs	2.36 log <sub>10</sub>	
	samonana rypniminium	Conductivity. 195	ι. 2.0 μο		(continued on next name)

Microorganism	Product	Treatment conditions	Reduction	Reference
χ3751		n: * NS	4.05 log <sub>10</sub>	
Salmonella Choleraesuis χ8442		f: 740 Hz	5.45 log <sub>10</sub>	
		Energy input: <sup>*</sup> NS		
		Flow rate: 120 mL/min		
		Inlet temperature: NS		
		Pulse type: bipolar / square		
Pseudomonas fluorescens	UHT whole milk with	F: 35 kV/cm	2.4 10910	(Walter et al. 2016)
(ATCC 948)	4.0% fat (w/w)	t: 124 µs	21110810	(mater et all, 2010)
	pH: * NS	τ: 2 μs		
	Conductivity: <sup>*</sup> NS	n: <sup>*</sup> NS		
		f: <sup>*</sup> NS		
		Energy input:		
		Flow rate: 120 mL/min		
		Maximum temperature: 30 °C on average		
		(in process)		
		Pulse type: * NS / * NS		
Cronobacter sakazakii	Infant milk formula	E: 35 kV/cm	$1.1\pm0.03$	(Pina-Pérez et al., 2013)
(29,544 ATCC)	pH: 6.8 at 25 °C	t: 700 µs	$log_{10}$	
	Conductivity:	τ: 2.5 μs		
	0.278 S/m at 25 °C	n: NS		
		f: NS Enorgy input: * NS		
		Ellergy input: NS Flow rate: 30 mL/min		
		Inlet temperature: 4 °C		
		Maximum temperature: $25 \pm 3 ^{\circ}\text{C}$		
		Pulse type: bipolar / square		
Gram-positive bacteria				
Bacillus cereus	Pasteurized skim Milk	E: 35 kV/cm	$\textbf{3.05} \pm \textbf{0.02}$	(Pina-Pérez et al., 2009)
(131)	pH: 6.69 ± 0.03 at 25 °C	t: 200 μs	log <sub>10</sub>	
	Conductivity:	τ: 2.5 μs	$3.03 \pm 0.02$	
	$5.77 \pm 0.10$ mS/cm at 25 °C	n: NS f. * NS	log <sub>10</sub>	
	$e_{\sigma\sigma}$ (80/20 v/v)	Energy input: * NS		
	pH: $6.18 \pm 0.05$ at 25 °C	Flow rate: 30 mL/min		
	Conductivity:	Inlet temperature: * NS		
	$7.23\pm0.03$ mS/cm at 25 $^\circ\text{C}$	Maximum temperature: 20 °C		
		(in process)		
v t t. t	o	Pulse type: NS / NS	0.071	(2, 1, 1, 1, 0010)
Lactiplantibacillus plantarum	Orange Juice	E: 20 kV/cm	3.07 log <sub>10</sub>	(Gurtler et al., 2010)
(49445) Lactiplantibacillus lactis	$p_{\text{H}}$ : 5.4 $\pm$ 0.1 at NS C Conductivity: * NS	τ: 2.6 μs	4.55 l0g <sub>10</sub>	
(114545)	conductivity. No	n: * NS	0.60 log <sub>10</sub>	
Lactiplantibacillus fermentum		f: 740 Hz	010	
(9338)		Energy input: * NS		
Lactiplantibacillus casei 393		Flow rate: 120 mL/min		
		Inlet temperature: * NS		
		Maximum temperature: 55 °C (outlet)		
Lactiniantibacillus bravis	Commercial low fat milk	F: 10 kV/cm	4.4 log	$(I_{ee} et al 2015)$
(ATCC13648)	nH <sup>• *</sup> NS	t: * NS	4.4 l0g10	(Lee et al., 2013)
(110010010)	Conductivity: * NS	τ: 30 μs		
		n: * NS		
		f: <sup>*</sup> NS		
		Energy input: 200 kJ/kg		
		Flow rate:30 L/h		
		Inlet temperature: <b>30</b> °C		
		Pulse type: bipolar/square		
Listeria monocytogenes 1,131	Melon Juice	F: 35 kV/cm	4.27 log10	(Mosqueda-Melgar et al.,
	Soluble solid content:	t: 2000 µs	010	2007)
	11.1°Brix at <sup>*</sup> NS°C	τ: 4 μs		
	pH: 5.82 $\pm$ 0.04 at $^{*}$ NS°C	n: * NS		
	Conductivity:	f: 100 Hz		
	$5.23 \pm 0.03$ mS/cm at NS°C	Energy input: 7662.23 J/cm <sup>3</sup>		
		Flow rate: 100 mL/min		
		Maximum temperature: $39.1 \pm 0.1$ °C		
		(outlet)		
		Pulse type: bipolar / square		
Listeria monocytogenes	Watermelon juice	E: 35 kV/cm	3.77 log <sub>10</sub>	(Mosqueda-Melgar et al.,
1.131	Soluble solid content:	t: 2000 μs		2007)
	6.5°Brix at NS °C	τ: 4 μs		
				(continued on next page)

Microorganism	Product	Treatment conditions	Reduction	Reference
	pH: 5.46 $\pm$ 0.11 at <sup>*</sup> NS°C Conductivity: 3.66 $\pm$ 0.05 mS/cm at <sup>*</sup> NS°C	n: <sup>*</sup> NS f: 250 Hz Energy input: 7541.18 J/cm <sup>3</sup> Flow rate: 100 mL/min		
Staphylococcus aureus (CECT 240)	Homogenized UHT skim-milk pH of $6.68 \pm 0.02$ at $25 \degree C$ Conductivity: $6.03 \pm 0.01$ mS/cm at $25 \degree C$	Inlet temperature: $^{*}$ NS Maximum temperature: $30.3 \pm 0.2$ °C (outlet) Pulse type: bipolar / square E:35 kV/cm t: $^{*}$ NS n: 150 pulses f: 100 Hz Energy input: $^{*}$ NS Inlet temperature: $^{*}$ NS Maximum temperature: 25 °C (in process) Pulse type: bipolar / square E: 35 kV/cm	4.5 log <sub>10</sub> 3.6 log <sub>10</sub>	(Sobrino-López et al., 2006)
Stanbylococcus aureus	Green tes heverage	L: 5 K// Cli t: * NS n: 150 pulses f: 100 Hz Energy input: * NS Inlet temperature: * NS Maximum temperature: 25 °C (in process) Pulse type: monopolar / square F: 38.4 kV/cm	4 9 log.c	(7hao et al. 2008)
(ATCC 6538)	pH: 6.0 at 20 °C Conductivity: 0.1 S/m at 20 °C	2. 50 F W/Cm t: 160 μs τ: 2 μs n: *NS f: 667 pps Energy input: 236 × 10 <sup>3</sup> J/L Inlet temperature: 20 °C Maximum temperature: *NS Pulse type: bipolar / square		(2000)
Staphylococcus aureus (ATCC 6538)	Soymilk pH: 7.22 ± 0.16 at 20 °C Conductivity: 0.21 ± 0.02 S/m at 20 °C	E: 40 kV/cm t: 547 μs τ: 2 μs n: * NS f: 400 Hz Energy input: * NS Flow rate: 1 mL/s Inlet temperature: 25 °C Maximum temperature: < 35 °C (in process) Pulse type: bipolar / square	3.51 log <sub>10</sub>	(Li et al., 2013)
Staphylococcus aureus (CICC 21648)	Grape Juice Soluble solid content: $15.8 \pm 0.2^{\circ}$ Brix at $^{\circ}$ NS°C pH: 5.98 $\pm 0.02$ at $^{\circ}$ NS°C Conductivity: $0.086 \pm 0.002$ S/m at 20 °C & 0.098 $\pm 0.002$ S/m at 30 °C	E: 24 kV/cm t:180 $\mu$ s t: 3 $\mu$ s n: * NS f: 120 Hz Energy input: * NS Flow rate: 7.6 mL/min Inlet temperature: 30 °C Maximum temperature: 38.2 $\pm$ 0.8 °C (outlet) Pulse type: monopolar / square	2.69 log <sub>10</sub>	(Huang et al., 2014)
Yeast Candida stellate (NRRL Y- 1446) Saccharomyces cerevisiae (ATCC 16664)	Sterilized deionized water pH: 5.6 at <sup>*</sup> NS°C Conductivity: 68 μS/cm at <sup>*</sup> NS°C Sterilized deionized water pH: 5.2 at <sup>*</sup> NS°C Conductivity: 15 μS/cm at <sup>*</sup> NS°C	E: 12.5 kV/cm t: NS <sup>*</sup> T: 0.3 ms n: 5 pulses f: *NS Energy input: *NS Inlet temperature: *NS Maximum temperature: < 30 °C Pulse turge: *NS (exponential	$\begin{array}{l} 3.5\pm 0.2 \; log_{10} \\ 3.3\pm 0.6 \; log_{10} \end{array}$	(Geveke & Kozempel, 2003)
Saccharomyces cerevisiae (CICC 1374)	Grape Juice Soluble solid content: $15.8 \pm 0.2^{\circ}$ Brix at <sup>*</sup> NS°C pH: 5.98 $\pm$ 0.02 at <sup>*</sup> NS°C Conductivity:	E: 24 kV/cm t:180 μs τ: 3 μs n: * NS f: 120 Hz	6.01 log <sub>10</sub>	(Huang et al., 2014)

(continued on next page)

Microorganism	Product	Treatment conditions	Reduction	Reference
	$0.086\pm0.002$ S/m at 20 °C & 0.098 $\pm$ 0.002 S/m at 30 °C	Energy input: <sup>°</sup> NS Flow rate: 7.6 mL/min Inlet temperature: 30 °C Maximum temperature: 38.2 ± 0.8 °C (outlet)		
Saccharomyces cerevisiae (ATCC 26603)	Commercial low-fat milk pH: * NS Conductivity: * NS	Puise type: monopolar / square E: 10 kV/cm t: * NS r: 30 μs n: * NS f: * NS Energy input: 200 kJ/kg Flow rate:30 L/h Inlet temperature: <b>30</b> °C Maximum temperature: * NS Pulse type: bipolar/square	6.0 log <sub>10</sub>	(Lee et al., 2015)
Saccharomyces cerevisiae ascospores (DSMZ 1848)	Lager Beer ≤0.05% alc/vol Conductivity: 2.20 mS/cm at 23 °C Dark Ale beer 5.0% alc/vol Conductivity: 1.97 mS/cm at 23 °C Ale beer 7.0% alc/vol Conductivity: 2.76 mS/cm at 23 °C	E: 45 kV/cm t: 70 µs t: 1.5 µs n: 46.3 pulses f: 700 Hz Energy input: <sup>*</sup> NS Flow rate: 4.34 mL/s Inlet temperature: <sup>*</sup> NS Maximum temperature: < 43 °C Pulse type: bipolar/square	0.2 log <sub>10</sub> 0.7 log <sub>10</sub> 2.2 log <sub>10</sub>	(Milani et al., 2015)
Brettanomyces bruxellensis (AWRI 1608)	Red Wine (Cabernet Sauvignon) 13.5% alc/vol pH: <sup>*</sup> NS Conductivity: 0.789 mS/cm at 5 °C	E: 50 kV/cm t: 42 $\mu$ s t: 1.7 $\mu$ s n: * NS f: 100 Hz Energy input: 119.3 $\pm$ 3.5 kJ/kg Flow rate: 0.23 mL/s Inlet temperature: 4.0 $\pm$ 0.2 °C Maximum temperature: 31.8 $\pm$ 0.7 °C (outlet temperature) Pulse type: bipolar / square	0.9 log <sub>10</sub>	(van Wyk et al., 2018)
Brettanomyces bruxellensis (AWRI 1499)	Red Wine (Cabernet Sauvignon) 13.5% alc/vol pH: * NS Conductivity: 0.789 mS/cm at 5 °C	E 50 kV/cm t: 42 $\mu$ s t: 1.7 $\mu$ s t: 1.7 $\mu$ s t: 100 Hz Energy input: 117.5 $\pm$ 1.4 kJ/kg Flow rate: 0.23 mL/s Inlet temperature: 3.8 $\pm$ 0.1 °C Maximum temperature: 31.1 $\pm$ 0.5 °C (outlet temperature) Pulse type: bioplar / square	3.0 log <sub>10</sub>	(van Wyk et al., 2018)
Brettanomyces bruxellensis (AWRI 1613)	Red Wine (Cabernet Sauvignon) 13.5% alc/vol pH: <sup>*</sup> NS Conductivity: 0.789 mS/cm at 5 °C	E: 50 kV/cm t: 42 μs $\tau$ : 1.7 μs n: *NS f: 100 Hz Energy input: 120.8 ± 3.7 kJ/kg Flow rate: 0.23 mL/s Inlet temperature: 3.4 ± 0.1 °C Maximum temperature: 31.3 ± 0.6 °C (outlet temperature) Pulse type: bipolar / square	3.7 log <sub>10</sub>	(van Wyk et al., 2018)

E: electric field strength; t: is total treatment time;  $\tau$ : is pulse width; n: number of pulses; f: pulse repetition rate. \* NS: non-specified.

# 3. Effect of PEF processing treatment on food-borne microorganisms

PEF treatments, similar to most of the environmental stresses do not lead to a "all or nothing "effect to a microbial population (Wang et al., 2015). Numerous studies have demonstrated that the electroporation phenomena observed in microbial cells after PEF application are not proportionally linked to cell death and there is a clear difference between electroporated and dead cells (Golberg et al., 2010). Consequently, insufficient PEF treatments can generate sub-lethally injured cells that raise food safety and security challenges (Jaeger et al., 2009). The occurrence of reversible pores after PEF treatment supports microbial membrane re-sealing, to a greater or lesser extent, enabling cell survival (Fig. 1) (García, Gómez, Mañas, et al., 2005; Golberg et al., 2010).For example, 45% of sublethally injured cells of *C. sakazakii* resealed their cytoplasmic membranes immediately after PEF treatment (Arroyo et al., 2010). However, Zhao et al. (2011) have demonstrated that PEF applications of >25 kV/cm field electric strength



Fig. 1. Sublethal damaged microorganisms after PEF application.

lead to permanent membrane damage to *E. coli* cells due to irreversible permeabilization, whilst at lower field strengths reversible electroporation manifested up to 20% and 10% of the cells, respectively. Chueca et al. (2015) have also shown that a PEF treatment of 50 pulses at 20 kV/cm lead to 40% inactivation and 40% injured *E. coli* cells. Furthermore, Zand et al. (2022) showed that under PEF treatments of 8 kV/cm and 18 kV/cm, 38% and 63% of the initial *E. coli* population were in intermediate cellular states, respectively, whereas PEF treatment of 25 kV/cm irreversibly injured 93  $\pm$  1% of *E. coli* cells.

In general, under environmental stresses, including temperature and osmotic changes, potential alterations in the organization and structure of the membrane lipids can lead to consecutive modulation of cellular activities (Los & Murata, 2004). Zhao et al. (2014a) noted that S. cerevisiae PEF treatments at 20 kV/cm for 100, 200, 300, 400 and 500 µs achieved lower microbial reductions in the presence of non-selective media  $(0.8, 1.2, 1.9, 2.5 \text{ and } 3.1 \log_{10})$  than in the presence of selective media  $(2.1, 3.0, 3.8 \text{ and } 4.1 \log_{10})$ , indicating that the salt composition of the selective media sensitised a large cell fraction to membrane damage. Additionally, Aronsson et al. (2005) showed that exposure of S. cerevisiae cells to a PEF treatment of 20 kV/cm and 2 µs resulted in a 1.8 log<sub>10</sub> inactivation and a 3.8 log<sub>10</sub> permeabilized cells, while under the same conditions, E. coli cells exhibited a 0.5 log<sub>10</sub> inactivation and a 0.3 log<sub>10</sub> membrane integrity reduction. These results show that cells of S. cerevisiae did not lose their ability to multiply albeit their membranes were permeabilized (Aronsson et al., 2005). Thus, the cytomembrane is a key target for PEF treatment-induced damage and only under favourable conditions sublethal populations can repair their membrane injuries (Zhao et al., 2014b).

Zhao et al. (2014a) have shown that after PEF treatment at 20 kV/cm with a process temperature < 30 °C, S. cerevisiae cells had an increase in their fluorescence anisotropy value (identified by measuring fluorescence anisotropy in intact whole cells by using hydrophobic 1,6diphenyl-1,3,5-hexatriene (DPH) as a probe) indicating a decrease in the cytoplasmatic membrane fluidity. Additionally, Zhao et al. (2014b) following PEF treatment of 20 kV/cm of S. cerevisiae cells for 100, 200, 300, 400, and 500  $\mu$ s with a process temperature < 30 °C have shown that there was an important increase in the membrane's micro-viscosity value n (i.e., 116.7%, 130.0%, 133.3%, 141.3% and 161.3%, respectively to the treatment times), indicating that the longer the PEF treatment the more rigid the cytomembrane was. In general, the response of the cells after environmental stresses is dependent on both the cytoplasmic membrane fluidity and the membrane fatty acid composition (Yun, Zeng, et al., 2016). Yun et al. (2017) have shown that an increase in growth temperature from 10 to 45 °C, increased both the C-C bond

and lamellar packing order of phospholipid chains leading to decreased membrane fluidity. Furthermore, Yun et al. (2017) have demonstrated that the PEF treatment time under the same electric field strength (29.33 kV/cm) for the inactivation of 90% of *S. typhimurium* cells was almost 4 times higher when cells were cultured at 10 °C than at 45 °C which indicates a PEF-efficiency dependence on membrane lipid composition.

Additionally, Wang et al. (2016) have shown that different growth temperatures lead to different percentages of injured S. aureus cells, following PEF treatments. Specifically, they found that S. aureus cells cultivated at 10 and 25 °C prior to a PEF treatment at 52.0 kV/cm, exhibited sublethal injuries to 12.26% and 20.75%, respectively. Those differences were attributed to changes in membrane structural integrity and fluidity, as a result of altered fatty acid membrane composition at different temperatures. S. aureus cells cultivated at 10 °C were more PEF sensitive because of their increased branched chain fatty acid (BCFAs) membrane content (such as anteiso C15:0 and anteiso C17:0) and their resulting membrane fluidity, whereas cells cultivated at 25 °C were more PEF resistant due to their reduced BCFA membrane content, increased straight chain fatty (such as C16:0, C17:0 and C18:0) and their reduced membrane fluidity (Wang et al., 2016). In line with the previous studies, the ratio of unsaturated and saturated fatty acids in the membrane lipids of S. cerevisiae changed after PEF treatment (20 kV/cm and 500 µs,) from 71.14% and 23.6% to 60.56% and 30.27%, respectively, confirming once again the tight relationship between membrane fluidity and effective microbial inactivation (Los & Murata, 2004; Zhao et al., 2014a).

Rivas et al. (2013) demonstrated that after PEF application of 15 kV/ cm, 700 µs and five inlet temperatures (7, 16, 24, 30 and 38 °C) the percentage of sub-lethally damaged E. coli DH5a cells reached a 16% maximum with increasing temperature from 7 to 30 °C, whereas a decrease in sub-lethal damages was observed at 38 °C. Zhao et al. (2022) have shown that depending on different water bath temperatures (4, 15, 35, 55 °C) in combination with a PEF treatment (20 kV/cm for 200  $\mu$ s) different inactivation rates of S. cerevisiae BY4742 were identified (i.e., at 55 °C - 6.1 log<sub>10</sub>, at 4 °C - 4.3 log<sub>10</sub>, at 35 °C - 3.9 log<sub>10</sub> and at 15 °C -3.9 log<sub>10</sub>)). Additionally, after storage at 4 °C for 5 h different sublethal populations were reported at 15 °C and 55 °C. Garcia, et al., (2005) showed that Gram-positive in comparison to Gram- negative bacteria were more resistant to PEF treatments at pH 7.0, whereas Gram-negative bacteria were more resistant in comparison to Gram-positive to PEF treatments at pH 4.0. In harmony with the previous study, Arroyo et al. (2010) found C. sakazakii to sustain sublethal injuries over the 3.5-4.0 pH range, where the strain exhibited its maximum resistance to the

### treatment.

Finally, Zhao et al. (2014a) have shown that injured cells of *S. cerevisiae* BY4742 treated with PEF (20 kV/cm) fully recovered after 70 min of incubation in 20 mmol/L glucose solution at 37 °C, suggesting that the repair mechanism is glucose-energy dependent and the mitochondria are one of the putative PEF treatment targets. Additionally, Garcia et al. (2006) have shown that the sublethally membrane injured population of *E. coli* (NCTC 5934) after PEF treatment was heterogeneous, with a small proportion (<5%) repairing their membranes immediately after PEF treatment and a remaining proportion (95%) requiring energy and lipid synthesis for membrane repair. This suggests that positive responses to the biosynthetic requirements of cytoplasmatic membrane leads to repair of the sub-lethally injured cells (García et al., 2006).

# 4. Effect of PEF treatment at a microbial genomic/ transcriptomic level

Gene expression alterations and differential protein synthesis before and after PEF treatments can reveal useful information for elucidating PEF-microbial inactivation and resistance mechanisms (Table 2)(Chueca

et al., 2015). Recently, Yun, Liu, et al. (2016) reported that following PEF application of 25 kV/cm and 1.2 ms to S. typhimurium cultivated at various temperatures (10, 20, 30, 37 and 45 °C), the transcription levels of the alternative sigma factor genes rpoS, rpoE and rpOH (genes which play an important role in protecting cells from environmental stress and repairing damages) were altered. More specifically: rpoS (RNA polymerase, Sigma S) transcription level was higher for cells cultivated at 10 and 20 °C, whereas the transcription levels for rpoE (RNA polymerase, extracytoplasmic E) and rpoH (RNA polymerase, Sigma H) were higher at 45 °C. Additionally, at higher cultivation temperatures (37,45 °C), the transcription levels of the fatty acid biosynthesis related genes cfa (encoding Cyclopropane-fatty-acyl-phospholipid synthase involved with the formation of cyclopropane fatty acid,(CFA)) and fabD (encoding malonyl CoA:ACP transacylase and associated with the formation of malonyl ACP transformed by malonyl CoA) which may contribute to the alteration of PEF resistance to S. typhimurium, were higher, whereas the transcription level of fatty acid biosynthesis gene, fabA was lower (Yun, Zeng, et al., 2016). Studies by Chueca et al. (2015) showed that after PEF treatment (E:25 kV/cm,  $\tau$ : 2 µs, n:50, <35 °C), targeting almost 90% of E. coli MG1655 cells, 20 genes were up-regulated and 27 were downregulated. Some of the up-regulated genes included: cvtochrome bo

Table 2

Genes/Proteins investigated under PEF treatments and their effect to microorganism's survival.

Microorganism	PEF parameters & Medium characteristics	Genes/ Proteins	Effect	Reference
Gram negative S. typhimurium	$\frac{\text{PEF parameters}}{\text{(E:25 kV/cm, t:1.2 ms,}}$ t:40 µs,n:50 bipolar square pulses) $\frac{\text{Medium characteristics}}{\text{(pH: 6.9 ± 0.1, 180 ± 1 µS/cm)}}$	<ul> <li>alternative sigma factor S, (<i>rpoS</i>)</li> <li>alternative sigma factor E, (<i>rpoE</i>)</li> <li>alternative sigma factor H, (<i>rpoH</i>)</li> <li>fatty acid biosynthesis, (<i>cfa, fabD, fabA</i>)</li> </ul>	Upregulation dependent on culture temperature (10, 20, 30, 37, 45 °C)	(Yun, Liu, et al., 2016)
<i>E. col</i> i MG1655	PEF parameters         (E:25 kV/cm, $\tau$ : 2 µs, n:50 exponential pulses, maximum temperature         <35 °C)	<ul> <li>cytochrome bo oxidase, (cyoB,cyoC, cyoD)</li> <li>hemeO synthase, (cyoE)</li> <li>transcriptional repressors of bet genes, (betl)</li> <li>succinate dehydrogenase, (sdhC, sdhD, sdhA, sdhB)</li> <li>chromosomal ars operon, (arsR)</li> </ul>	Upregulation	(Chueca et al., 2015)
E. coli DH5α	PEF parameters         (E:15 kV/cm, t: 700 μs, bipolar square pulses         maximum temperature         <25 °C)	<ul> <li>protein of the outer membrane, (OmpA)</li> <li>phosphoheptose isomerase, (gmhA)</li> <li>protein involved in the degradation of unfolded or abnormal proteins, (ClpA)</li> <li>ribosomal protein S6 in the 30S subunit of ribosome, (RS6)</li> <li>enzymedeoxyuridine 5'-triphosphate nucleotidohydrolase, (Dut)</li> <li>ferritine, (FtnA)</li> </ul>	Decreased level (affected by treatment) Increased level after treatment (recovery related)	(Rivas et al., 2013)
Gram positive <i>S. aureus</i> Newman	PEF parameters (E:19–31 kV/cm, exponential pulses, maximum temperature <35 °C) Medium characteristics (nH: 7.0, 2 mS/cm)	• alternative sigma factor B, ( <i>sigB</i> )	Importance for resistance	(Cebrián et al., 2009)
L. monocytogenes EGD-e	PEF parameters (E:30 kV/cm, τ:3 μs, f:1 Hz, square pulses, <35 °C maximum temperature) <u>Medium characteristics</u> (pH: 4.0 and 7.0, 1 mS/cm)	• alternative sigma factor B, ( <i>sigB</i> )	No effect	(Somolinos et al., 2010)
Yeast S. cerevisiae BY4742	PEF parameters (voltage:2 and 4 kV, t: 30 min) Medium characteristics (sterilized distilled water)	<ul> <li>heat-shock-protein encoding gene, (<i>HSP104</i>)</li> <li>genes encoding enzymes for superoxide removal, (<i>SOD1</i>, <i>SOD2</i>)</li> <li>glutathione synthesis genes, (<i>GLR1</i>, <i>GSH1</i>)</li> </ul>	Slightly induced expression Induced expression	(Tanino et al., 2012)
S. cerevisiae BY4742	PEF parameters           (E:20 kV/cm, t: 200 μs, τ:2 μs)           Medium characteristics           (pH: 7.2, *NS mS/cm)	• heat-shock-protein encoding gene, ( <i>HSP104</i> )	Importance for resistance	(Zhao et al., 2022)

E: electric field strength; t: is total treatment time; τ: is pulse width; n: number of pulses; f: pulse repetition rate.

\* NS: non-specified.

<sup>†</sup> ND: not determined.

oxidase (one of the 3 major terminal oxidases in the aerobic respiratory of E.coli) genes (cyoB, cyoC, cyoD) and hemeO synthase (cyoE) which are included in functioning of cytochrome bo oxidase, succinate dehydrogenase (sdhCDAB) operon and transcriptional repressors of bet genes (betI) and chromosomal ars operon (arsR) (Chueca et al., 2015). Cebrián et al. (2009) showed that absence of the alternative Sigma factor (sigB) regulator, in S. aureus (Newman and IK184, an isogenic DrsbUVW-sigB knockout mutant) lowered the resistance against PEF treatments. However, in the study by Somolinos et al. (2010) the SigB gene was dispensable to PEF, as both strains of Listeria monocytogenes (EGD-e and its isogenic deletion mutant *\Delta sigB*) showed the same resistance under the same conditions, independently of the treatment's pH. However, under heat treatment, the genes regulated by SigB appeared to contribute to heat resistance at pH 7.0 (Somolinos et al., 2010). Also, Tanino et al. (2012) showed differences in the transcription level of the heat stress response gene HSP104 and oxidation stress response gene GLR1 after thermal (42 °C for 30 min) and PEF treatments (2 kV and 30 min, 4 kV and 30 min), respectively. Additionally, expression of different stress response genes, such as GSH1 and GLR1 (responsible for glutathione synthesis enzymes) and SOD1 and SOD2 (encoding enzymes for superoxide removal) were induced following only PEF treatments. Interestingly, the same study suggested that glutathione-dependent biological defense mechanisms against oxidation stress appear to be important in the S. cerevisiae resistance against PEF treatments.

Liu et al. (2019a) found 29 out of the 175 differentially expressed proteins of E. coli CGMCC44102 after PEF treatment, were located at the cell membrane, with 16 of the identified proteins playing a role in the transmembrane transport of various small metabolites and macromolecules, including phosphate ions, zinc, glycine betaine, trehalose, as well as short peptides, carbohydrates and lipids. The study of Rivas et al. (2013) identified 7 common proteins differentially produced following PEF treatment of E. coli DH5a (15 kV/cm, for 700 µs at various temperatures (7, 16, 24,and 38 °C). More specifically, outer membrane protein A (ompA), had levels that were lower at 7  $^\circ$ C and 16  $^\circ$ C than the control or even non-existent at 24 °C and 38 °C (Rivas et al., 2013). In contrast, the levels of phosphoheptose isomerase (GmhA; involved in the biosynthesis of cell wall lipopolysaccharide), cytosolic phosphorylase A (ClpA; involved in n the degradation of unfolded or abnormal proteins), ribosomal protein S6 in the 30S ribosomal subunit (RS6;involved in the translation stage of protein biosynthesis), enzyme deoxyuridine 5'triphosphate nucleotidohydrolase (Dut; responsible of the production of dUMP and involved in nucleic acid metabolism) and ferritin A (FtnA; involved in storing iron) were connected with the recovery of the microorganism (Rivas et al., 2013).

Furthermore, Zhao et al. (2014a) reported changes in the activity of cellular enzymes of S. cerevisiae by PEF. More specifically, following a PEF treatment at 20 kV/cm for 500 µs, S. cerevisiae lipase C14, cystine arylamidase, naphthol-AS-BI-phosphohydrolase and a-glucosidase activities were undetectable, whereas esterase (C4), esterase lipase (C8), leucine arylamidase, valine aryl-amidase and phosphatase acid were markedly reduced, indicating a reduced rate of lipolytic processes (Zhao et al., 2014b). Additionally, Zhao et al. (2022) have identified that after a combination of mild heating and PEF treatment there were 8 significantly up regulated proteins (such as cystathionine beta-synthase, intracellular glyceraldehyde-3-phosphate dehydrogenase, phosphopyruvate hydratase ENO2 etc.) and 11 down regulated spots (such as translation machinery-associated protein 17, thioredoxin peroxidase, dihydroorotate dehydrogenase etc.). Among the up regulated proteins, the intracellular glyceraldehyde-3-phosphate dehydrogenase is an enzyme playing an important role in glycolysis and glucogenesis pathways and is important in the cellular energy metabolism. Additionally, due to emerging thermal effects, heat shock proteins, such as heat shock protein 70 (Heat shock protein of Hsp70 family and stress-seventy subfamily A protein) were also upregulated (Zhao et al., 2022). In line with the aforementioned observations, Zhao et al. (2014a) showed compromised recovery from S. cerevisiae sublethal injuries under PEF-

induced mitochondrial damage. Thus, the production of different proteins related to the cell membrane functioning and repair, glycolysis and heat shock can play an important role in the resistance against PEF treatment (Liu et al., 2019b; Zhao et al., 2022).

In conclusion, the investigation into gene expression alterations and differential protein synthesis after PEF treatments have provided valuable insights into microbial inactivation and resistance mechanisms. Studies on S. typhimurium have highlighted temperature-dependent variations in the transcription levels of key genes involved in stress response and damage repair, emphasizing the complexity of microbial responses to PEF. Additionally, research on S. aureus has implicated the regulatory alternative sigma factor B, in determining resistance to PEF treatments. Analysis of protein expression profiles in E. coli and S. cerevisiae, has revealed the involvement of membrane-associated proteins and enzymes related to cellular metabolism in the resistance mechanisms against PEF. Notably, the combination of mild heating and PEF treatment has been shown to induce changes in the expression of key proteins associated with glycolysis, cellular energy metabolism, and heat stress response. These findings collectively underscore the multifaceted nature of microbial responses to PEF and provide a foundation for enhancing our understanding of PEF-based microbial control strategies. Further investigations into the transcriptomics, proteomics, and metabolomics of different microorganisms after PEF treatments it is vital for gaining a more comprehensive understanding of the resistance mechanisms and exploring the potential optimization of PEF, whether applied alone or in combination with other hurdles.

An overview on recent investigations of microbial disinfection of food products following PEF-treatments is presented in the current manuscript. In this review, it was shown that 5-log reduction of microorganisms was achieved in specific experimental conditions. Additionally, it was shown that the PEF-inactivation efficiency (5-log reduction) varies with the nature of the food products, the characteristics of the microorganisms and the PEF system/set parameters employed. For example, the threshold of 5-log reduction was achieved for E. coli and high liquid acid products such as orange juice and strawberry juice. In parallel, this review underlined the different mechanisms that can contribute to the microbial PEF resistance (i.e., alterations in the synthesis profile of proteins involved in cell membrane function/transport, cell membrane repairment, oxidative stress adaptation and cellular energy metabolism). However, further investigations should be conducted in this area of research. A deeper understanding and identification of the underlying mechanisms of microbial PEF resistance can aid in optimizing the technology and potentially integrating it with other hurdles.

# 5. Conclusion

PEF technology is a promising method and has shown its potential to inactivate bacterial vegetative cells, yeasts and moulds, and to achieve the food safety requirements, especially for high acid liquid food products, such as fruit juices. However, the attainment of the goal of food safety is contingent upon the specific targeted microorganism, the nature of the food product, and the applied PEF parameters. In certain instances, achieving high-intensity treatments necessary for the antimicrobial efficacy may pose drawbacks, including increased process costs and potential impacts on the organoleptic and nutritional quality of the food. In parallel, PEF process due to its dependence on specific application parameters, may result in reversible electroporation especially in lower intensity treatments, allowing a partial recovery of the initial population, potentially posing serious food safety concerns. This reversible nature means that PEF's effectiveness is not absolute, and partial recovery could lead to significant food safety issues. Therefore, PEF is a promising technology with limitations on the applicability for microbial inactivation depending on the aforementioned parameters. In conclusion, advancing the industrialization of PEF process for microbial inactivation and enhancing its efficiency can progress along two distinct paths: optimizing the PEF process and integrating the technology with

### additional hurdles.

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### CRediT authorship contribution statement

Fotios Lytras: Conceptualization, Investigation, Visualization, Writing – original draft, Writing – review & editing. Georgios Psakis: Conceptualization, Supervision, Writing – review & editing. Ruben Gatt: Conceptualization, Supervision, Funding acquisition, Writing – review & editing. Guillermo Cebrián: Writing – review & editing. Javier Raso: Writing – review & editing. Vasilis Valdramidis: Conceptualization, Supervision, Resources, Project administration, Funding acquisition, Writing – review & editing.

### Declaration of competing interest

None.

### Data availability

Data will be made available on request.

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