



# Thermophysical characterization of lidocaine:camphor:thymol or l-menthol eutectic mixtures: Experimental and modelling

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## ABSTRACT

Knowing the values of the thermodynamic and transport properties of fluids is essential for their implementation in different fields. In addition, their analysis allows us to understand the intermolecular interactions which is useful in the subsequent design of processes. In this work, two ternary eutectic mixtures composed of lidocaine, camphor, and thymol or l-menthol were studied. Six thermophysical properties were measured at 0.1 MPa and at various temperatures. Density values up to 65 MPa were also determined. From these data, different properties were calculated, such as isobaric expansibility, isentropic and isothermal compressibility, internal pressure, and critical temperature, among others. The mixture with thymol was the most dense, structured, and viscous. The correlations and models used showed small deviations between the experimental and estimated values. The deviations of the density and isobaric molar heat capacity predicted with PC-SAFT equation of state were lower than 1.4 % and 3.1 %, respectively. The interactions between lidocaine and thymol were the strongest. On the other hand, camphor was shown to be a steric hindrance to binary interactions.

## 1. Introduction

Healthcare challenges require innovative, sustainable, effective, and affordable pharmaceutical solutions. Despite major advances in research in this field, two major obstacles remain to be overcome. First, almost 40 % of drugs marketed or in development exhibit reduced solubility. This fact is often offset by higher doses increasing costs and increased risk of side effects [1,2]. Second, the increasing number of approved biological therapies (peptides, proteins, or nucleic acids), brings additional challenges for their stability, storage, and administration, including the advantages of the formulations in liquid phase [3,4]. Recently, the use of deep eutectic solvents (DESs) in pharmacology is being postulated as an alternative with multiple advantages. Briefly, DESs are mixtures of two or more components that show a much lower melting point when combined so that they are in liquid phase at room temperature. Although the term eutectic was introduced in 1884 [5], the work published by Abbott et al. [6] in 2004 is considered as the starting point of this field. Since then, DESs have attracted great attention in very distant scientific areas, ranging from structural biology to energy storage materials, since it is possible to tailor their physicochemical properties,

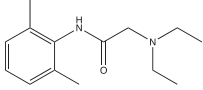
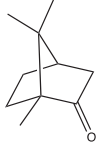
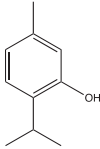
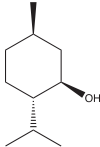
such as hydrophobicity, ionic strength, acid/base character or dielectric constant, among others. A more exhaustive analysis of their definition and typology can be found in several reviews [7–11]. In principle, any compound capable of donating or accepting hydrogen bonds can be component of DES. Most active pharmaceutical ingredients (APIs) meet this requirement and can therefore give rise to mixtures that will also have therapeutic properties. In this case, they are called THEDESs. They have gained relevance in the pharmaceutical context due, among other things, to the synergies detected between the constituent APIs thus enhancing the value of the final product [10,12–14].

Lidocaine (L) is one of the most widely used APIs in the design and preparation of THEDESs due to its anesthetic, antiarrhythmic, and antiepileptic activity [15]. Its combination with prilocaine (known as EMLA®) was the first DES marketed in 1949 [16]. Later, other binary mixtures with nonsteroidal carboxylic acid anti-inflammatories or terpenes were evaluated [17–20]. This work presents the thermophysical characterization of two ternary mixtures of L with camphor (C) and thymol (T) or l-menthol (M). Previously, the structural study of these mixtures was carried out and published by us. This work showed the presence of important intermolecular interactions between lidocaine

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**Table 1**  
Compounds used in this work.

Chemical (Acronym)	CAS No	Purity <sup>a</sup>	<i>M</i> /g·mol <sup>-1</sup>	Structure
Lidocaine (L)	137-58-6	>0.98	234.34	
Camphor (C)	464-49-3	>0.98	152.23	
Thymol (T)	89-83-8	>0.985	150.22	
L-menthol (M)	89-78-1	>0.99	156.27	

<sup>a</sup> As stated by the supplier (mass fraction).

and terpenes [20]. The three compounds enhance transdermal penetration, which is why their use in medicinal and cosmetic applications is widespread. Other benefits such as their activity against microbes or fungi, and their power to stimulate thermoregulatory receptors have been reported [20]. The structures of T and M differ only in that the cycle of the first is of an aromatic type. Nevertheless, this fact can have a great influence on their behavior. The results of this work will allow us to further investigate the intermolecular interactions present in both mixtures based on the differences observed in their properties. In addition, previous studies carried out on the corresponding binary mixtures [19–21] will allow us to analyze the effect of the addition of the third component. For the ternary mixtures, no literature data was found. From an operational point of view, the use of correlations and thermodynamic models that are capable of calculating and predicting the values of thermophysical properties in a wide range of conditions (pressure, temperature, and composition) is very important in the industry. Nevertheless, they must be previously validated. In the following, we obtain the coefficients that allow calculating the value of the properties at any pressure and temperature within the working range of this study. We also show the goodness of correlations such as Taherzadeh et al. [22], Guggenheim [23], Eotvos [24], Papazian [25], Pelofsky and Mukherjee [26], that allow estimating the isobaric molar heat capacity, critical temperature, and surface tension. Finally, we validate the PC-SAFT equation of state [27,28] as a predictive thermodynamic model.

This article will focus on the measurement and evaluation of thermodynamic and transport properties at 0.1 MPa of two ternary lidocaine-based eutectic mixtures. Also, density data up to 65 MPa were determined. The lowest working temperature was 278.15 K in the equipment operating at atmospheric pressure, and 283.15 K in the high-pressure device. The highest temperature was 338.15 K in all cases. From all these values, different derived properties were calculated and several correlations were applied. In addition, the PC-SAFT equation of state was validated for both mixtures in a wide range of pressure and temperature.

**Table 2**  
Summary of the devices used in the thermophysical characterization at *p* = 0.1 MPa.

Property	Devices	<i>u</i> ( <i>T</i> )/K	<i>U<sub>c</sub></i> ( <i>Y</i> ) <sup>a</sup>	<i>MRD</i> ( <i>Y</i> ) <sup>b</sup> /%
Density, $\rho$	Oscillating U-tube density meter, Anton Paar DSA 5000 <sup>c</sup>	0.005	0.05 kg·m <sup>-3</sup>	0.004
Speed of sound, <i>u</i>	Acoustic, time-of-flight method, Anton Paar DSA 5000 <sup>c</sup>	0.005	0.5 m·s <sup>-1</sup>	0.026
Refractive index, <i>n<sub>D</sub></i>	Standard Abbe refractometer, Abbat-HP refractometer Dr. Kernchen <sup>d</sup>	0.01	2·10 <sup>-5</sup>	0.007
Isobaric molar heat capacity, <i>C<sub>p,m</sub></i>	Differential scanning calorimeter, TA Instruments DSC Q2000	0.5	1 %	0.028
Surface tension, $\gamma$	Drop volume tensiometer, Lauda TVT-2 <sup>d</sup>	0.01	1 %	0.21
Kinematic viscosity, $\nu$	Capillary viscosimeter Ubbelohde, Schoot-Geräte AVS-440	0.01	1 %	0.28

<sup>a</sup>*k* = 2 (0.95 level of confidence); <sup>b</sup> $MRD(Y) = \frac{100}{n} \sum_{i=1}^n \left| \frac{Y_{i,lit} - Y_{i,exp}}{Y_{i,exp}} \right|$ ; <sup>c</sup> Calibrated with dry air and water MilliQ ( $\rho = 18.2 \mu \text{S} \cdot \text{cm}^{-1}$ ); <sup>d</sup> Calibrated with water MilliQ ( $\rho = 18.2 \mu \text{S} \cdot \text{cm}^{-1}$ ).

## 2. Experimental section

### 2.1. Materials

The characteristics and structures of the pure compounds used in this work are listed in Table 1. All of them were provided by Sigma–Aldrich and no purification processes were applied. The mixtures were made by weighing (PB210S Sartorius balance) the appropriate mass of each compound to obtain the chosen molar fraction. The standard uncertainty in the weight was of  $u(m) = 1 \cdot 10^{-4}$  g. Stirring and heating at 323 K were then applied simultaneously until a homogeneous liquid was obtained. The water content was measured with an automatic titrator Crison KF 1S-2B and the value was less than 300 ppm in all cases. Finally, the eutectic mixtures were kept at 298 K until used. The studied mixtures were lidocaine:camphor:l-menthol (1:1:2, molar ratio) and lidocaine:camphor:thymol (1:1:1, molar ratio) and are called through the manuscript as LCM2 and LCT, respectively. The molar masses (*M*) were estimated from the molar mass of each compound (*M<sub>i</sub>*) and its molar fraction (*x<sub>i</sub>*) as  $M = \sum_i x_i M_i$ . The values were  $M(\text{LCM2}) = 174.78 \text{ g} \cdot \text{mol}^{-1}$ , and  $M(\text{LCT}) = 178.93 \text{ g} \cdot \text{mol}^{-1}$ .

### 2.2. Apparatus

The thermophysical characterization at *p* = 0.1 MPa was carried out with widely known devices. Table 2 reports the type of apparatus, the standard uncertainty in the temperature (*u*(*T*)), the combined expanded uncertainties for each property (*U<sub>c</sub>*(*Y*)), and the mean relative deviations (*MRD*(*Y*)) obtained from checking it with benzene. For all properties, each tabulated data was the average of two replicates with a coefficient of variation less than the experimental uncertainty. Furthermore, for each replicate of the surface tension, 6 cycles of 6 drops per cycle were averaged. Dynamic viscosity ( $\eta$ ) was calculated from density and kinematic viscosity data,  $\eta = \rho \nu$ .

The measurement of density under pressure was performed with a

thermostatted oscillating U-tube density meter (Anton Paar DMA HP 5000). A hand pump 750.1100 (Sitec) was used to achieve the working pressure that was measured with a transducer US181 (Measuring Specialties). The device was calibrated with dry air, hexane, water MilliQ ( $\rho = 18.2 \mu \text{ S cm}^{-1}$ ), and dichloromethane. Later, it was verified with toluene. The values of the standard uncertainties in the temperature and pressure, combined expanded uncertainty ( $k = 2$  (0.95 level of confidence) in the density, and mean relative deviation in the checking were  $u(T) = \pm 0.01 \text{ K}$ ,  $u(p) = \pm 0.05 \text{ MPa}$ ,  $U_c(\rho) = \pm 0.01 \text{ kg} \cdot \text{m}^{-3}$ , and  $\text{MRD}(\rho) = 0.01 \%$ .

### 3. Model and correlations

#### 3.1. PC-SAFT EoS

This model, developed by Gross and Sadowski [27,28] is widely used in the literature for all types of fluids. It is based on the considering the Helmholtz energy ( $\tilde{a}$ ) as the sum of an ideal gas contribution ( $\tilde{a}^{\text{id}}$ ) and a residual ( $\tilde{a}^{\text{res}}$ ). A repulsive term described using the hard-chain reference system ( $\tilde{a}^{\text{hc}}$ ), and several attractive ones as the dispersive ( $\tilde{a}^{\text{dis}}$ ) and association ( $\tilde{a}^{\text{assoc}}$ ) contribute to the residual term.

$$\tilde{a}^{\text{res}} = \tilde{a}^{\text{hc}} + \tilde{a}^{\text{dis}} + \tilde{a}^{\text{assoc}} \quad (1)$$

The equations of the three summands are [29–31]:

$$\tilde{a}^{\text{hc}} = m\tilde{a}^{\text{hs}} - (m-1) \ln g^{\text{hs}} \quad (2)$$

$$\begin{aligned} \tilde{a}^{\text{dis}} = & -2\pi\rho m^2 \left(\frac{\varepsilon}{kT}\right) \sigma^3 \sum_{i=0}^6 \left[ a_{0i} + \frac{m-1}{m} a_{1i} + \frac{m-1}{m} \frac{m-2}{m} a_{2i} \right] \eta^i \\ & - \pi\rho m k T \left(\frac{\partial \rho}{\partial p}\right)_{\text{hc}} m^2 \left(\frac{\varepsilon}{kT}\right)^2 \sigma^3 \sum_{i=0}^6 \left[ b_{0i} + \frac{m-1}{m} b_{1i} + \frac{m-1}{m} \frac{m-2}{m} b_{2i} \right] \eta^i \end{aligned} \quad (3)$$

$$\tilde{a}^{\text{assoc}} = \sum_A \left[ \ln(1 + \rho X^A \Delta)^{-1} - \frac{(1 + \rho X^A \Delta)^{-1}}{2} \right] + \frac{1}{2} S \quad (4)$$

$$\Delta = \kappa^{A_i B_i} \sigma^3 g^{\text{hs}} \left[ \exp\left(\frac{\varepsilon^{A_i B_i}}{kT}\right) - 1 \right] \quad (5)$$

where  $m$  is the chain segment number,  $g^{\text{hs}}$  is the radial pair distribution function of the segments,  $\tilde{a}^{\text{hs}}$  is the Helmholtz energy of the hard sphere,  $\rho$  is the density,  $p$  is the pressure,  $T$  is the temperature,  $\sigma$  is the segment diameter,  $\varepsilon$  is the segment energy,  $\eta$  is the packing fraction,  $X^A$  is the fraction of unbonded monomers,  $\Delta$  is the tendency to form  $n$ -mers,  $\kappa^{A_i B_i}$  is the association volume,  $\varepsilon^{A_i B_i}$  is the association energy, and  $S$  is the number of associated sites of the compound. The parameters  $a_{0i}$ ,  $a_{1i}$ ,  $a_{2i}$ ,  $b_{0i}$ ,  $b_{1i}$ , and  $b_{2i}$  are called *universal constants* and were obtained from the optimization of the thermodynamic properties of  $n$ -alkanes.

In summary, three geometrical parameters ( $m$ ,  $\sigma$  and  $\varepsilon$ ) are needed to characterize each pure compound in this model. Also, two additional ( $\kappa^{A_i B_i}$  and  $\varepsilon^{A_i B_i}$ ) parameters and an association scheme must be provided for substances able to associate. In the case of mixtures, mixing rules are needed and we have used the following:

$$\sigma_{ij} = (\sigma_i + \sigma_j)/2 \quad (6)$$

$$\varepsilon_{ij} = \sqrt{\varepsilon_i \varepsilon_j} (1 - k_{ij}) \quad (7)$$

$$\kappa^{A_i B_j} = \sqrt{\kappa^{A_i B_i} \kappa^{A_j B_j}} \quad (8)$$

$$\varepsilon^{A_i B_j} = (\varepsilon^{A_i B_i} + \varepsilon^{A_j B_j})/2 \quad (9)$$

where the subscripts  $i$  and  $j$  refer to each of the compounds present in the

mixture. A no-null binary interaction parameter ( $k_{ij}$ ) can be estimated from the thermodynamic properties of the mixture. In this way, the model loses the predictive character and becomes a correlation.

#### 3.2. Correlations

##### 3.2.1. Properties ( $p = 0.1 \text{ MPa}$ ) – Temperature

For a range of temperatures such as the one studied here, the thermodynamic properties at  $p = 0.1 \text{ MPa}$  mostly show a linear correlation, ascending or descending, with  $T$ :

$$Y = A_Y + B_Y T \quad (10)$$

where  $Y$  is  $\rho$ ,  $u$ ,  $n_D$ ,  $\gamma$ ;  $A_Y$  and  $B_Y$ , are the fit parameters.

The effect of the temperature on the transport properties at  $p = 0.1 \text{ MPa}$  is more pronounced at low temperatures so they follow an exponential equation. We have used the VFT expression [32–34]:

$$\eta = A \exp\left(\frac{B}{T-C}\right) \quad (11)$$

where  $A$ ,  $B$ , and  $C$ , are the fit parameters.

##### 3.2.2. To estimate the isobaric molar heat capacity

A method to estimate the  $C_{p,m}$  of eutectic mixtures was proposed by Taherzadeh et al. [22]. The equations are the following:

$$C_{p,m} = A + 132.27T^{1/4} \quad (12)$$

$$A = 3.8 \cdot 10^{-4} \frac{M^3}{p_c^6} + 6.3 \cdot 10^{-5} M^{2\omega} - \frac{24577.4}{M} - 94.9 \quad (13)$$

Where  $T$  is the temperature,  $M$  is the molar mass,  $p_c$  is the critical pressure, and  $\omega$  is the acentric factor. The Lee-Kesler (LK) mixing rules extended to ternary mixtures [35] was used to calculate  $p_c$  and  $\omega$  of both THEDES as follows:

$$p_c(\text{bar}) = (0.2905 - 0.0850\omega) \frac{83.1447T_c}{V_c} \quad (14)$$

$$\omega = \sum_{n=1}^3 x_n \omega_n \quad (15)$$

$$V_c(\text{mL/mol}) = \sum_{n=1}^3 \sum_{m=1}^3 x_n x_m V_{c, mn} \quad (16)$$

$$T_c(\text{K}) = \frac{1}{V_c^{0.25}} \sum_{n=1}^3 \sum_{m=1}^3 x_n x_m V_{c, mn}^{0.25} T_{c, mn} \quad (17)$$

$$V_{c, mn}(\text{mL/mol}) = \frac{1}{8} \left( V_{c, n}^{1/3} + V_{c, m}^{1/3} \right)^3 \quad (18)$$

$$T_{c, mn}(\text{K}) = (T_{c, n} T_{c, m})^{0.5} \quad (19)$$

Where  $T_c$  and  $V_c$  are the critical temperature and critical volume of the THEDES. The subscripts  $n$  and  $m$  represent each component, and  $mn$  is the subscript indicating binary interaction term.

##### 3.2.3. To estimate the critical temperature

The  $T_c$  can be calculated with thermodynamic models as in the previous sections (eq. 1–19). In addition, it can be obtained from data of  $\gamma$  and  $\rho$  at several  $T$  with the Guggenheim [23] and Eötvös [24] equations:

$$\gamma = \gamma_0 (1 - T/T_c)^{11/9} \quad (20)$$

$$\gamma(M/\rho)^{2/3} = K(T_c - T) \quad (21)$$

**Table 3**

Summary of the thermophysical properties at  $T = 298.15$  K and  $p = 0.1$  MPa of the studied mixtures.

Property	lidocaine:camphor:l-menthol (1:1:2)	lidocaine:camphor:thymol (1:1:1)
Density $\rho/\text{kg}\cdot\text{m}^{-3}$	939.69	979.76
Speed of sound $u/\text{m}\cdot\text{s}^{-1}$	1395.69	1431.77
Refraction index $n_D$	1.47930	1.50637
Isobaric molar heat capacity $C_{p,m}/\text{J}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$	338	322
Surface tension $\gamma/\text{mN}\cdot\text{m}^{-1}$	30.29	32.48
Dynamic viscosity $\eta/\text{mPa}\cdot\text{s}$	25.70	54.34
Isobaric expansibility $\alpha_p/\text{K}\cdot\text{K}^{-1}$	0.799	0.778
Isothermal compressibility $\kappa_T/\text{TPa}^{-1}$	660.98	601.75
Internal pressure $\pi_T/\text{TPa}^{-1}$	360.53	385.26
Isentropic compressibility $\kappa_S/\text{TPa}^{-1}$	546.31	497.89
Molar refraction $R_m/\text{cm}^3\cdot\text{mol}^{-1}$	52.77	54.29
Free volume $f_m/\text{cm}^3\cdot\text{mol}^{-1}$	133.22	128.33
Entropy of surface $\Delta S_S/\text{mN}\cdot\text{m}^{-1}\cdot\text{K}^{-1}$	0.0823	0.0860
Enthalpy of surface $\Delta H_S/\text{mN}\cdot\text{m}^{-1}$	54.83	58.12
Activation energy of viscous flow $E_{a,\eta}/\text{kJ}\cdot\text{mol}^{-1}$	47.13	52.66

Standard uncertainties are:  $u(T)=0.005$  K for density and speed of sound and 0.01 K for the rest of properties;  $u(p)=0.5$  kPa. The combined expanded uncertainties (0.95 level of confidence,  $k=2$ ) are  $U_c(\rho) = 0.05$   $\text{kg}\cdot\text{m}^{-3}$ ;  $U_c(u)=0.5$   $\text{m}\cdot\text{s}^{-1}$ ;  $U_c(n_D)=2\cdot 10^{-5}$ ;  $U_c(C_{p,m})=1\%$ ;  $U_c(\gamma)=1\%$ ;  $U_c(\eta)=1\%$ ;  $U_c(\alpha_p)=0.04$   $\text{K}\cdot\text{K}^{-1}$ ;  $U_c(\kappa_T)=0.22$   $\text{TPa}^{-1}$ ;  $U_c(\kappa_S)=0.22$   $\text{TPa}^{-1}$ ;  $U_c(R_m)=0.004$   $\text{cm}^3\cdot\text{mol}^{-1}$ ;  $U_c(f_m)=0.03$   $\text{cm}^3\cdot\text{mol}^{-1}$ ;  $U_c(\Delta S_S)=0.001$   $\text{mN}\cdot\text{m}^{-1}\cdot\text{K}^{-1}$ ;  $U_c(\Delta H_S)=0.06$   $\text{mN}\cdot\text{m}^{-1}$ .

Where  $\gamma_0$  is the surface tension at 0 K.

### 3.2.4. To estimate the surface tension

The equation of Papazian [25] allows obtaining the values of  $\gamma$  from the dielectric constant ( $\epsilon_s$ ) data at similar  $p$  and  $T$ . Except to liquids with strong hydrogen bonds, the Maxwell relation ( $n_D^2 = \epsilon_s$ ) can be used and the correlation equation is:

$$\gamma = A \left( \frac{n_D^2 - 1}{2n_D^2 + 1} \right) + B \quad (22)$$

The equations of Pelofsky and Murkerjee [26] relate  $\gamma$  and  $\eta$  of a fluid at each  $T$ :

$$\ln \gamma = \ln A_1 + \frac{B_1}{\eta} \quad (23)$$

$$\ln \gamma = \ln A_2 + \frac{B_2}{3} \ln \eta \quad (24)$$

Where  $A_1, A_2, B_1$ , and  $B_2$  are the fit coefficients.

### 3.2.5. Pressure – Density – Temperature

The equation of Tait was used to correlate  $p$ ,  $\rho$  and  $T$  [36]. The expressions are:

$$\rho = \frac{\rho_0(T, p_0)}{1 - C \bullet \ln \left( \frac{B(T)+p}{B(T)+p_0} \right)} \quad (25)$$

$$\rho_0(T, p_0) = \sum_{i=0}^n A_i \cdot T^i \quad (26)$$

$$B(T) = \sum_{i=0}^n B_i \cdot T^i \quad (27)$$

where  $p_0$  is the reference pressure (0.1 MPa) and  $\rho_0$  is the density at  $p_0$ . The  $A_i, B_i$ , and  $C$  are the fitted parameters. From  $p\rho T$  data and by deriving of eq. (20), several properties can be obtained. They are the isobaric thermal expansibility ( $\alpha_p$ ), isothermal compressibility ( $\kappa_T$ ), and internal pressure ( $\pi_T$ ):

$$\alpha_p = -\frac{1}{\rho} \left( \frac{\partial \rho}{\partial T} \right)_p \quad (28)$$

$$\kappa_T = \frac{1}{\rho} \left( \frac{\partial \rho}{\partial p} \right)_T \quad (29)$$

$$\pi_T = T \left( \frac{\kappa_T}{\alpha_p} \right)_T - p \quad (30)$$

## 4. Results and Discussion

### 4.1. Thermophysical properties at $p = 0.1$ MPa

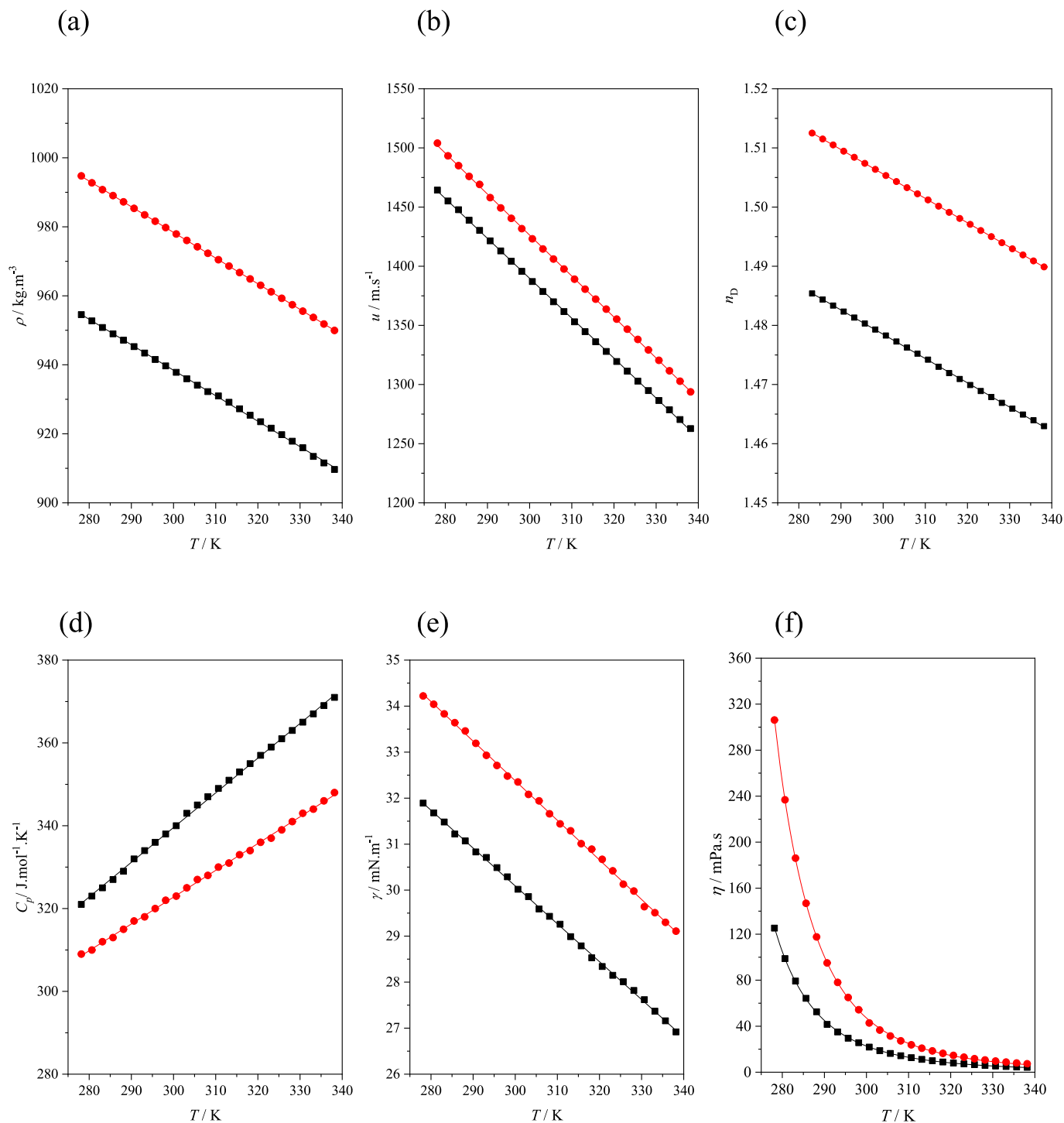
In this section, experimental data of  $\rho$ ,  $u$ ,  $n_D$ ,  $C_{p,m}$ ,  $\gamma$ , and  $\eta$  at pressure of 0.1 MPa and temperatures from 278.15 to 338.15 K are presented, modelled, and discussed. Tables S1 and S2 report all data and Table 3 lists those at 298.15 K.

For both systems, the  $\rho$  measured at 0.1 MPa was lower than that of water. However, only LCM2 could be adequately separated in a liquid–liquid equilibrium with an aqueous phase. The  $\rho$  of the mixture with M ranged from 909.68 to 954.54  $\text{kg}\cdot\text{m}^{-3}$  and LCT was 40  $\text{kg}\cdot\text{m}^{-3}$  denser throughout the  $T$  range. A liquid can be considered as a continuous space that contains holes so that the volumetric behavior of the former will be the result of how different variables affect the latter. The flatter structure of T compared to the cycle of M would justify the need for a larger hole in the LCM2 mixture.

Fig. 1a shows the experimental  $\rho$  values at different  $T$  and those obtained with the linear correlation. The coefficients of the latter are listed in Table 4.

Having validated thermodynamic models that allow predicting property values under any composition, pressure, or temperature condition is a very useful tool. Here, we estimated the  $\rho$  with the PC-SAFT EoS (eq. 1–9) and compared these values with those experimental ones. The parameters of the pure compounds are listed in Table 5 and that of the binary interaction was null ( $k_{ij} = 0$ ). The model predicted this property very well (Fig. S1) with mean relative deviations of 0.54 % for LCM2, and 0.46 % for LCT.

The propagation of sound is favored in more compact materials, so  $u$  is indicative of the structuring of the fluid. For LCT mixture, these data were a 2.5 % higher than those determined for LCM2, in agree with the above volumetric results. The increase in thermal agitation with increasing  $T$  represents a decrease in compaction and, consequently, a decrease in  $u$ . The decrease was linear as shown in Table 4 and Fig. 1b. The capacity of the liquid to compress under isentropic conditions or isentropic compressibility ( $\kappa_S$ ) was calculated from  $\rho$  and  $u$  data at similar  $p$  and  $T$ . Also, an estimation of the free intermolecular length ( $L_f$ ) was made from  $\kappa_S$  and the constant of Jacobson ( $K$ ) [38]. The equations used are:



**Fig. 1.** Thermophysical properties of the studied mixtures as a function of temperature,  $T$ . (a), density,  $\rho$ ; (b), speed of sound,  $u$ ; (c), refraction index,  $n_D$ ; (d), isobaric molar heat capacity,  $C_{p,m}$ ; (e), surface tension,  $\gamma$ ; (f), dynamic viscosity,  $\eta$ . (■), Lidocaine:camphor:l-menthol (1:1:2); (●), lidocaine:camphor:thymol (1:1:1). Points, experimental data; lines, correlated values.

$$\kappa_s = \frac{1}{\rho u^2} \quad (25)$$

$$L_f = K\sqrt{\kappa_s} = (91.368 + 0.3565 T) \cdot 10^{-8} \sqrt{\kappa_s} \quad (26)$$

The  $\kappa_s$  values were higher for the mixture with M and increased with  $T$  due to the increase of the thermal motion (Table 3, Fig. S2a). The temperature coefficients of this property ( $\partial\kappa_s/\partial T$ ) were 3.345 and 3.033  $\text{TPa}^{-1}\text{K}^{-1}$  for LCM2, and LCT, respectively. Moreover,  $L_f$  ranged from 0.421 to 0.556 Å for the mixture with M, and from 0.402 to 0.531 Å for

that with T.

On the other hand, the propagation of light is favored in less compact materials, so  $n_D$  is also indicative of the structuring of the fluid. This property is defined as the ratio between the speed of light in the vacuum to that in the fluid. Then, the less compact fluid, the lower index. The results coincided with the previous ones, with LCT being the most compact mixture. The  $n_D - T$  correlation was also a straight line with a negative slope (Table 4, Fig. 1c). An estimate of polarizability of the fluid, which is related to the hard-core volume, can be made from  $n_D$  and

**Table 4**

Fit parameters ( $A_Y, B_Y, C_Y$ ) and the regression coefficients,  $R^2$ , for the thermo-physical properties at  $p = 0.1$  MPa of the studied mixtures.

Property	Mixture	$A_Y$	$B_Y$	$C_Y$	$R^2$
Density $\rho^a / \text{kg} \cdot \text{m}^{-3}$	lidocaine: camphor:l- menthol (1:1:2)	1160.05	-0.7387		0.99955
	lidocaine: camphor: thymol (1:1:1)	1201.57	-0.7440		0.99999
Speed of sound $u^a / \text{m} \cdot \text{s}^{-1}$	lidocaine: camphor:l- menthol (1:1:2)	2402.28	-3.3750		0.99987
	lidocaine: camphor: thymol (1:1:1)	2465.67	-3.4645		0.99986
Refraction index $n_D^a$	lidocaine: camphor:l- menthol (1:1:2)	1.60164	$-4.10 \cdot 10^{-4}$		0.99988
	lidocaine: camphor: thymol (1:1:1)	1.62930	$-4.12 \cdot 10^{-4}$		0.99999
Isobaric molar heat capacity $C_{p,m}^a / \text{J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$	lidocaine: camphor:l- menthol (1:1:2)	88.028	0.8385		0.99930
	lidocaine: camphor: thymol (1:1:1)	128.64	0.6471		0.99913
Surface tension $\gamma^a / \text{mN} \cdot \text{m}^{-1}$	lidocaine: camphor:l- menthol (1:1:2)	54.78	-0.0823		0.99944
	lidocaine: camphor: thymol (1:1:1)	58.19	-0.0860		0.99927
Dynamic viscosity $\eta^b / \text{mPa} \cdot \text{s}$	lidocaine: camphor:l- menthol (1:1:2)	0.04215	643.86	197.67	0.99984
	lidocaine: camphor: thymol (1:1:1)	0.02184	855.44	188.57	0.99990

$${}^a Y = A_Y + B_Y T; {}^b Y = A_Y \exp\left(\frac{B_Y}{T - C_Y}\right)$$

$\rho$  data calculating the molar refraction ( $R_m$ ) with the equation of Lorentz-Lorentz [39]:

$$R_m = \left(\frac{n_D^2 - 1}{n_D^2 + 2}\right) \frac{M}{\rho} \quad (27)$$

The  $R_m$  values were highest for the mixture with T. At 298.15 K, they are listed in Table 3 and as function of  $T$  are shown in Fig. S2b. The influence of  $T$  on  $R_m$  was small for both systems. The temperature coefficients ( $\partial R_m / \partial T$ ) were  $2.783 \cdot 10^{-3}$  and  $3.787 \cdot 10^{-3} \text{ cm}^3 \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$  for LCM2, and LCT, respectively. From  $R_m$  definition, the size of the holes or free volume ( $f_m$ ) is calculated as the difference between the molar volume and molar refraction. As expected, data of the mixture with M were higher than those of with T and increased with  $T$  (Table 3, Fig. S2c). At 298.15 K, the percentages of unoccupied volume were 71.6 % for LCM2, and 70.3 % for LCT.

On average, the  $C_{p,m}$  of the mixture with M was 5 % higher than that of the mixture with T, and this difference increased with  $T$  (Fig. 1d). The

**Table 5**

PC-SAFT parameters used to model the studied mixtures. The type 2B (one donor and one acceptor site) was considered as association scheme.

Compound	$m$	$\sigma / \text{\AA}$	$\epsilon / \text{K}$	$\kappa^{A_i B_i}$	$\epsilon^{A_i B_i} / \text{K}$
Lidocaine <sup>a</sup>	6.320	3.770	285.85	0.01	2798.5
Camphor <sup>b</sup>	3.583	3.984	283.50	0.01	2662.3
Thymol <sup>c</sup>	4.012	3.816	290.22	0.0616	1660.0
L-menthol <sup>c</sup>	4.152	3.903	262.40	0.0996	1785.6

<sup>a</sup> Ref. [19]; <sup>b</sup> Ref. [21]; <sup>c</sup> Ref. [37].

higher the temperature, the greater the ability of the fluids to accumulate energy. For most of them, the increase follows a linear equation. Table 3 lists the coefficients for our mixtures. Our experimental data were compared with those calculated with the correlation of Taherzadeh et al. (eq. 12–13) whose uncertainty estimated was 4.7 %. For this, the values of  $p_c$  and  $\omega$  of the mixtures were needed and can be estimated with the Lee-Kesler (LK) mixing rules (14–19). For our ternary eutectic mixtures, we used the Excel worksheet provided by Boublia et al. [35]. The model underestimated  $C_{p,m}$  for the mixture with M and slightly overestimated that of the mixture with T. The deviations were 5.5 % and 0.9 % for LCM2 and LCT, respectively. This property was also modeled with PC-SAFT (eq. 1–9). The EoS well predicted  $C_{p,m}$  for both mixtures with deviations of 2.8 % for LCM2 and 3.1 % for LCT. The trends were similar to the above correlation (Fig. S1b).

The movement of a molecule from the bulk of the liquid to the air-liquid interface implies an energy contribution, which is higher at higher cohesion between the molecules. The  $\gamma$  is a property indicative of this molecular cohesion. In a similar way to what was found with the properties previously studied, the measured  $\gamma$  data indicated that the interactions in the LCT mixture were stronger than in LCM2. For the later,  $\gamma$  was 7.7 % lower than for first. A linear decrease with  $T$  was also observed because increasing thermal agitation decreases the ability to establish interactions (Table 5, Fig. 1e). From this relationship, the entropy of surface ( $\Delta S_s$ ) and the enthalpy of surface ( $\Delta H_s$ ) were calculated:

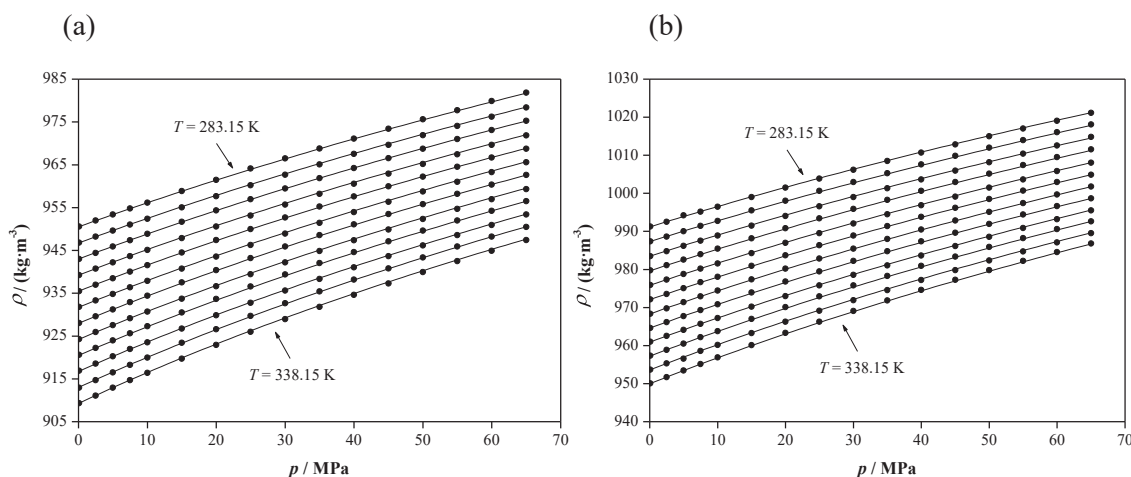
$$\Delta S_s = - \left( \frac{\partial \gamma}{\partial T} \right)_p \quad (27)$$

$$\Delta H_s = \gamma - T \left( \frac{\partial \gamma}{\partial T} \right)_p \quad (28)$$

The greater the cohesive forces in the fluid, the greater the values of the surface properties. A higher structuration was observed in the LCT mixture (Table 3). The  $T_c$  is a very interesting thermodynamic property in the study of fluids but difficult to determine experimentally. Failing that, previously validated EoS, group contribution methods, and  $\gamma - T_c$  correlations can be used. Table S3 reports  $T_c$  values estimated from the PC-SAFT EoS (eq. 1–9), LK mixing rules (eq. 14–19), and Guggenheim and Eötvös correlations (eq. 20–21). For both mixtures, the values calculated with LK and Guggenheim equations were the highest. By averaging the values estimated with the other methods,  $T_c(\text{LCM2}) = 745$

$\pm 5$  K, and  $T_c(\text{LCT}) = 764 \pm 3$  K. In Table S3,  $p_c$  values from PC-SAFT and LK are also included. The differences between estimated data were higher than 1 MPa. Molecules become polarized as they move from the interior of the fluid to the interface as their force field changes. Then,  $\gamma - n_D$  relationship could be expected. Papazian proposed a linear equation between  $\gamma$  and a function of the  $n_D$  (eq. 22). A very high linearity was found for our mixtures with regression coefficients higher than 0.999. The fitting coefficients are listed in Table S4.

Viscosity is the resistance of any fluid to movement. Mainly, it depends on two factors: steric hindrance due to the geometry of the molecules, and intermolecular interactions. A high value may be beneficial for some applications as lubrication but is a drawback in those in which



**Fig. 2.** Density,  $\rho$ , of the studied mixtures as a function of temperature,  $T$ , and pressure,  $p$ . (a), Lidocaine:camphor:l-menthol (1:1:2); (b), lidocaine:camphor:thymol (1:1:1). Points, experimental data; lines, correlated values (eq. 19–21).

the fluid acts as solvent. The value of 100 mPa·s has been established as the maximum value that ensures the proper operation of the equipment [40]. Our studied mixtures exhibited a  $\eta$  lower than that maximum value at  $T$  greater than 290 K. The LCT system was more viscous than LCM2, from 2.44 times at 278.15 K to 1.74 times at 338.15 K. The  $\eta$  decreased exponentially with increasing  $T$  as Fig. 1f shows. The coefficients of the equation used (eq. 11) are listed in Table 5. At  $T \rightarrow \infty$ , the interactions are completely prevented so the  $A_Y$  coefficient would be indicative of the steric hindrance due to the size and shape of the molecules. Additionally, the activation energy for viscous flow ( $E_{a,\eta}$ ), measure of the strength of intermolecular interactions, is calculated from  $B_Y$  and  $C_Y$  according to the following equation [41]:

$$E_{a,\eta} = R \left( \frac{\partial \ln \eta}{\partial \left( \frac{1}{T} \right)} \right) = R \frac{B}{\left( \frac{C^2}{T^2} - \frac{2C}{T} + 1 \right)} \quad (29)$$

Table 3 lists the  $E_{a,\eta}$  data at 298.15 K and Fig. S2d displays those at different  $T$ . From  $A_Y$  and  $E_{a,\eta}$  data, it can be seen that LCM2 exhibited the highest steric hindrance and LCT showed the strongest interactions. According to the measured  $\eta$  values, the second factor predominated over the first in our systems throughout the  $T$  range. Different authors have proposed a  $\eta - \gamma$  relationship. In this work, we applied the Pelofsky and Murkerjee equations (eq. 23,24). Both correlations showed a good linearity for our mixtures. The coefficients are listed in Table S4.

No data were found in the literature of any of the thermophysical properties measured in this work for the LCM2 and LCT ternary systems. Nevertheless, a comparison with the results obtained previously by us for the LM2, CM2, LT, and CT binary systems can be performed [19–21]. The  $\rho$  and properties related to the compaction of the system were similar for the LM2 and LCM2 mixtures, and these values were higher than for CM2. The results showed that the influence of L on CM2 was greater than C on LM2. Also,  $\eta$  and  $E_{a,\eta}$  were similar for CM2 and LCM2 and much lower than those of LM2. This fact could indicate that C hindered the interactions between L and M. In relation to the systems with T, data of the properties of the ternary mixture were intermediate with respect to those of the corresponding binaries. This result showed that the effect of L on CT compaction was similar to that of C on LT. Furthermore, the decrease of  $\eta$  in the LCT system was less pronounced than in LCM, probably because L interacted more strongly with T than with M. The latter agreed with studies carried out with NMR techniques [20].

**Table 6**

Parameters of the Tait equation (eq. 10–12) and the mean relative deviations of the studied mixtures.

	Lidocaine:camphor:l-menthol (1:1:2)	Lidocaine:camphor:thymol (1:1:1)
$A_0 / \text{kg}\cdot\text{m}^{-3}$	1167.26	1253.35
$A_1 / \text{kg}\cdot\text{m}^{-3}\cdot\text{K}^{-1}$	-0.7785	-1.0736
$A_1 / \text{kg}\cdot\text{m}^{-3}\cdot\text{K}^{-2}$	$4.60\cdot 10^{-5}$	$5.22\cdot 10^{-4}$
$C$	0.0724	0.0727
$B_0 / \text{MPa}$	259.99	400.11
$B_1 / \text{MPa}\cdot\text{K}^{-1}$	-0.4484	-1.2444
$B_2 / \text{MPa}\cdot\text{K}^{-2}$	$-1.90\cdot 10^{-4}$	$1.03\cdot 10^{-3}$
$MRD^a(\rho) / \%$	0.12	0.13

$$^a MRD(\rho) = \frac{100}{n} \sum_{i=1}^n \left| \frac{\rho_{i,cal} - \rho_{i,exp}}{\rho_{i,exp}} \right|$$

#### 4.2. Volumetric properties under pressure

The  $\rho$  of the LCM2 and LCT mixtures at pressures from 0.1 to 65 MPa, and temperatures from 283.15 to 338.15 K were determined. From these values, derived properties as isobaric expansibility ( $\alpha_p$ ), isothermal compressibility ( $\kappa_T$ ), and internal pressure ( $\pi_T$ ), were calculated. All data are reported in Table S5–S8 and those for 0.1 MPa and 298.15 K are included in Table 3. No data for these ternary mixtures were found in the literature. Nevertheless,  $p\rho T$  values of the binary CM2 and CT were published by our group at similar  $p$  and  $T$  ranges. So, a comparison between the volumetric behaviour of both type of systems can be performed.

The mixture with thymol was  $40 \text{ kg}\cdot\text{m}^{-3}$  denser than that of l-menthol for any  $p$  and  $T$ . The higher  $\rho$  would be related to the planar configuration of the aromatic ring of thymol, and with stronger L-T interactions. Comparing with the corresponding binary mixtures, the incorporation of L into the system increased the  $\rho$  value. On average,  $\rho$  of LCM2 was 2.83 % greater than that of CM2, and  $\rho$  of LCT was 1.22 % greater than that of CT. The effect of L on  $\rho$  was smaller with increasing  $p$ . Again, the density was predicted with PC-SAFT EoS (eq. 1–9) and compared to measurements in similar way that above. The values provided by the model were slightly greater than the experimental ones and the relative mean deviations were  $MRD(\rho) = 1.34 \%$  and  $1.10 \%$  for LCM2, and LCT, respectively. No trends in the deviations with  $T$  were observed but they increased with  $p$  (fig. S1a). Despite that, the low  $MRD(\rho)$  values do not justify a non-null  $k_{ij}$ . Fig. 2 shows the experimental

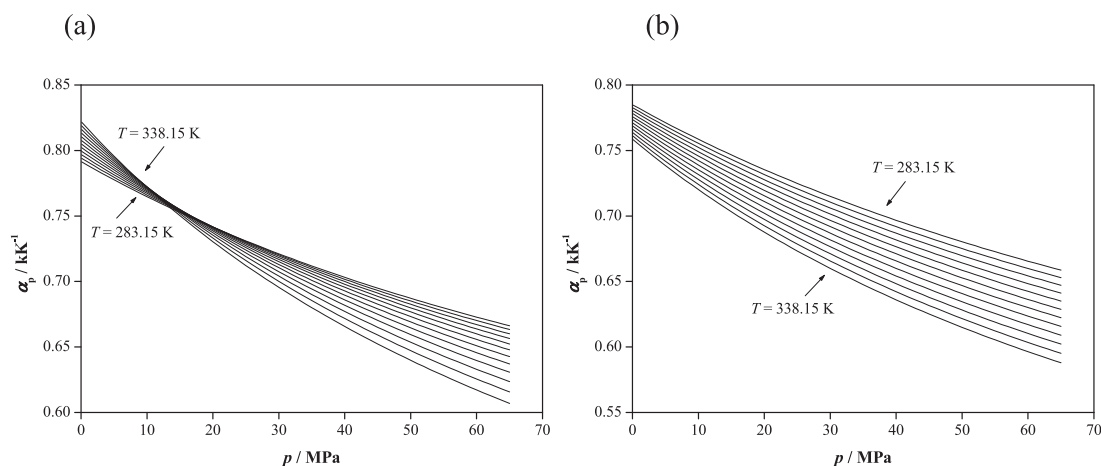


Fig. 3. Isobaric expansibility,  $\alpha_p$ , of the studied mixtures as a function of temperature,  $T$ , and pressure,  $p$ . (a), Lidocaine:camphor:l-menthol (1:1:2); (b), lidocaine:camphor:thymol (1:1:1). Points, experimental data; lines, correlated values (eq. 28).

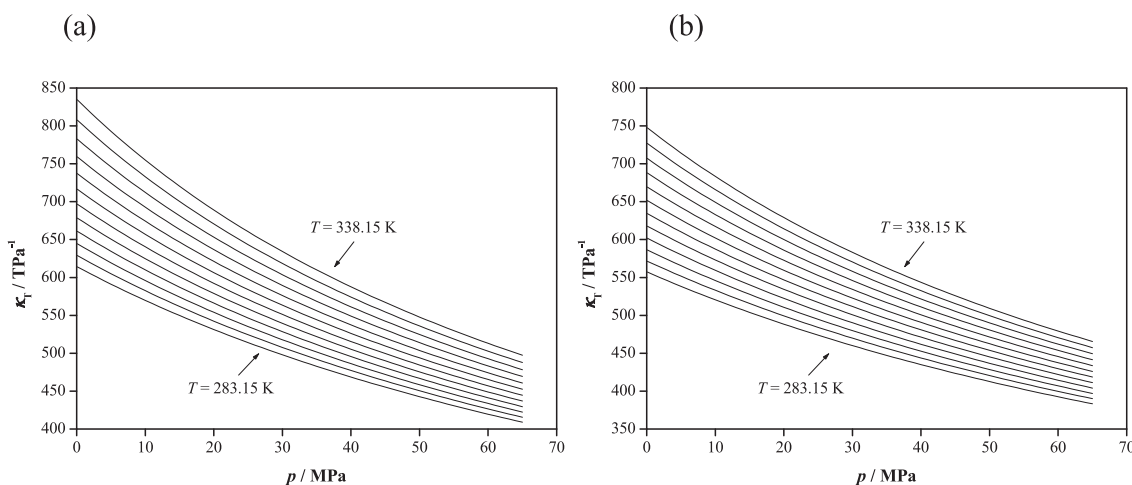


Fig. 4. Isothermal compressibility,  $\kappa_T$ , of the studied mixtures as a function of temperature,  $T$ , and pressure,  $p$ . (a), Lidocaine:camphor:l-menthol (1:1:2); (b), lidocaine:camphor:thymol (1:1:1). Points, experimental data; lines, correlated values (eq. 29).

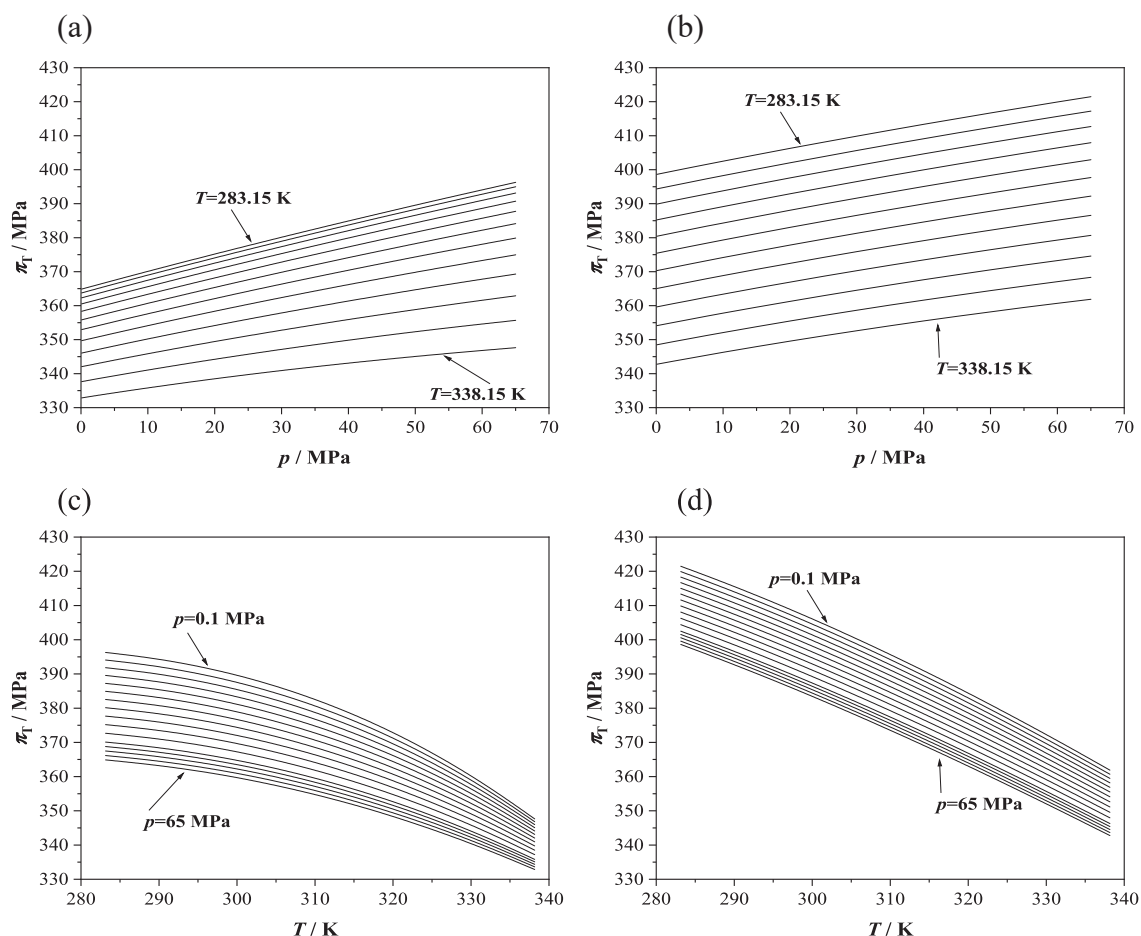
$\rho$  as a function of  $p$  at each  $T$  as well as those values obtained with the Tait equation (eq. 25–27). The coefficients of this correlation for both mixtures are reported in Table 6.

The effect of  $T$  on  $\rho$  was quantified with the  $\alpha_p$  (eq. 28). The calculated values ranged from 0.607 to 0.822  $\text{kK}^{-1}$  for LCM2 and from 0.588 to 0.785  $\text{kK}^{-1}$  for LCT, showing that the first mixture was less compact. As expected, this property decreased with increasing  $p$  due to the decrease in the free volume of the system. On the other hand, an anomalous behavior with  $T$  was observed. For LCM2, the temperature coefficient was positive at pressures below 10 MPa and negative at pressures above 25 MPa (Fig. 3a). For LCT, this coefficient was negative at any  $p$  (Fig. 3b). This decrease in  $\alpha_p$  with an increase in  $T$  has been related to the existence of strong interactions [42] so that the more condensed a fluid is, the lower the pressure value at which this phenomenon appears. It should be noted that in the CM2 and CT binary mixtures, the  $\alpha_p$  increased with  $T$  throughout the  $p$  range. From this, it can be deduced that the presence of lidocaine causes a high structuring in the mixtures. Moreover, the  $\kappa_T$  (eq. 29) allows to estimate the effect of  $p$  on  $\rho$ . Again, the higher values were those of the mixture with M. They were from 408.99 to 834.48  $\text{TPa}^{-1}$  for LCM2, and from 383.25 to 747.60  $\text{TPa}^{-1}$  for LCT. As usual, this property increased with  $T$  and decreased with  $p$  (Fig. 4). An inverse linearity between  $\kappa_T$  and  $p$  was found. For both systems, the  $(1/\kappa_T)-p$  representation was a straight line ( $R^2 = 1$ ) of slope  $m = 12.5$ . This linearity was already found for CM2 and CT

mixtures and was in accordance with that published by Wilhelm [43].

The  $\pi_T$  is a property related to the strength of the interactions present in a fluid and is calculated with the eq. (30). The stronger the interactions, the greater the  $\pi_T$  data. The calculated values ranged from 332.90 to 396.29 MPa for LCM2, and from 342.79 to 421.47 MPa for LCT. They were also greater than the corresponding binary mixtures without L. The  $\pi_T$  increased with  $p$  because intermolecular interactions are favored by decreasing free volume (Fig. 5a, 5b). On the other hand, the  $\pi_T$  decreased monotonically with increasing  $T$  (Fig. 5c, 5d), which indicated a prevalence of hydrogen bonds over van der Waals interactions [44]. From all this, it can be deduced that the presence of L in the system contributed to structuring the fluid and that the L-T interactions were greater than the L-M interactions. These results were in agreement with those previously found by us using NMR techniques [20].

The cohesive energy density (CED) can be estimated from thermodynamical models previously validated as PC-SAFT EoS, and can be written as the sum of two contributions [45,46]. The first ( $\delta_V^2$ ) is related to van der Waals interactions and can be calculated as the square root of the internal pressure. The second ( $\delta_R^2$ ) is related to the interactions of chemical character, and consequently, can be calculated from the difference between CED and  $\pi_T$ . Based on all of the above,  $\delta_R^2$  of LCT was expected to be the highest value. At 298.15 K and 0.1 MPa,  $\delta_R^2 = 47.11$



**Fig. 5.** Internal pressure,  $\pi_T$ , of the studied mixtures as a function of temperature,  $T$ , and pressure,  $p$ . (a,c), Lidocaine:camphor:l-menthol (1:1:2); (b,d), lidocaine:camphor:thymol (1:1:1). Points, experimental data; lines, correlated values (eq. 30).

MPa for LCM2, and  $\delta_R^2 = 60.37$  MPa for LCT. These values were also higher than the corresponding binary mixtures [21].

## 5. Conclusions

In this work, the thermophysical characterization of two hydrophobic eutectic solvents was performed. They were the ternary mixtures lidocaine:camphor:l-menthol (1:1:2) (LCM2), and lidocaine:camphor:thymol (1:1:1) (LCT). For this study, the density, speed of sound, refractive index, isobaric molar heat capacity, surface tension, and dynamic viscosity were measured at 0.1 MPa and from 278.15 to 338.15 K. Furthermore, the volumetric behavior in a pressure range of 0.1 to 65 MPa, and at temperatures from 283.15 to 338.15 K was determined and evaluated. From these data, several derived properties and correlations were presented. Finally, the PC-SAFT equation of state was validated for both systems. The results were analyzed and compared with those previously obtained for the corresponding binary mixtures.

The LCT was the most dense, compact, structured and viscous mixture. Also, its critical temperature estimated from different equations was higher than that of LCM2. The  $C_{p,m}$  values from the Taherzadeh correlation were close to those measured, with deviations of 5.5 % and 0.9 % for LCM2 and LCT, respectively. High linearities were found in the correlations between the surface tension and refractive index, and viscosity. The PC-SAFT model adequately predicted  $\rho$  throughout the range of  $p$  and  $T$  with a mean relative deviation from the experimental values of less than 1.4 %. For  $C_{p,m}$  at 0.1 MPa, the deviation was less than 3.1 %. The interactions between L and T were stronger than those with M. The incorporation of C to the binary mixtures hindered the

interactions of L with both terpenes, especially those between L and M.

## CRedit authorship contribution statement

**Mónica Sancho-Blasco:** Resources, Methodology, Data curation. **Jorge L. Pastor:** Methodology, Data curation. **José Muñoz-Embid:** Writing – original draft, Formal analysis. **Carlos Lafuente:** Writing – original draft, Validation. **Manuela Artal:** Writing – review & editing, Writing – original draft, Supervision.

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.molliq.2024.126655>.

## Data availability

The authors confirm that the data supporting the findings of this study are available within the article and its [supplementary materials](#).

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